Evaluation of synthetic water-soluble metal-binding polymers with ultrafiltration for selective concentration of americium and plutonium

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Water-soluble metal-binding polymers in combination with ultrafiltration are shown to be an effective method for selectively removing dilute actinide ions from acidic solutions of high ionic strength. The actinide-binding properties of commercially available water-soluble polymers and several polymers which have been reported in the literature were evaluated. The functional groups incorporated in the polymers were pyrrolidone, amine, oxime, and carboxylic, phosphonic, or sulfonic acid. The polymer containing phosphonic acid groups gave the best results with high distribution coefficients and concentration factors for 241 Am(11) and 238 Pu(11)/(IV) at pH 4 to 6 and ionic strengths of 0.1 to 4.

Introduction

Despite the ability of modern instrumentation to analyze increasingly lower concentrations, elements of regulatory concern are still often at levels near or below the detection limit. Analytical radiochemical counting instrumentation readily allows for measurements of 1 to 10 ml volumes, containing 2 disintegrations/minute/ml (2 dpm/ml or 33 Bq/l). Inductively coupled plasma-mass spectrometry (ICP-MS) has a normal working range for routine sample analysis in the parts per billion (ppb) range. Routine counting methods and ICP-MS are unable to directly measure the new United States' Department of Energy (DOE) regulatory level for discharge waters containing alpha-emitting radionuclides of 30 pCi/l (1.1 Bq/l) total alpha or the 0.05 pCi/l $(1.8 \cdot 10^{-3} \text{ Bq/l})$ (~1·10⁻⁶ ppb for ²³⁹Pu) regulatory level for Pu or Am activity required for surface waters at the Rocky Flats site by the State of Colorado. This inability indicates the need to develop rapid, reliable, and robust analytical techniques for measuring actinide metal ions, particularly americium and plutonium.

The analysis can be further complicated by high concentrations of alkaline or alkaline earth salts and other metal ions in the waste water. High salt concentrations limit the usefulness of preconcentration of samples by evaporation. In such cases selective separation and other preconcentration techniques are required.¹ Conventional separation and preconcentration techniques (which include extraction chromatography, ion exchange, solvent extraction, co-precipitation, or sorption) have several disadvantages. These methods require interphase transfer of the metal ion and the slower reaction kinetics may require longer contact times. If aqueous solutions are the preferred media for the analysis, additional steps of selective stripping, backextraction, or desorption are required. Other problems



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arise if the metal ions of interest exist in forms such as colloids, which can require additional treatments. For example, colloidal material can pass through or clog ion-exchange resin columns depending on a variety of factors such as bead size, flow rate, and colloid size.

The use of water-soluble metal-binding polymers in combination with ultrafiltration has the potential to be an effective method for selectively removing metal ions from dilute aqueous solutions on both an analytical and a process scale. This method uses water-soluble metalbinding polymers to selectively retain metal ions of interest, while unbound metal ions and small molecular species are removed with the bulk of the aqueous solution as the permeate or filtrate.² The advantages of this "polymer filtration" technique are: (1) metal-ion complexation takes place under homogeneous conditions that generally result in enhanced kinetics of binding, (2) colloidal material does not interfere with metal-ion retention, (3) no mixed waste is produced, (4) direct analysis of the concentrate occurs, (5) a reduced number of procedual steps are required, and (6) a variety of analytical instruments can be used to make the final measurements. Polymer filtration has been successfully used for the retention of transition and heavy toxic metal ions, but there have been very few reported studies on the separation and preconcentration of actinide metal ions from waste waters. Bayer and co-workers have reported that the retention at pH 6 of the actinide metalions, uranium [U(VI)], plutonium [Pu(IV)], americium [Am(III)], curium [Cm(III)], and californium [Cf(III)] was achieved with poly(ethylenimine) modified with 8groups (8HQ).^{3,4} They hydroxyquinoline were successful in separating Am(III) and Pu(IV) from U(VI) at pH 4 in the presence of a masking agent, using 8HQ in combination with ultrafiltration. However, there have been no reports in the literature on the selective and quantitative retention of transuranic metal ions by

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polymer filtration in aqueous solutions having high salt content as found in some process and waste waters. We present here the results of a study using the polymer filtration technique for the recovery of Am and Pu with both commercially available and synthesized watersoluble metal-binding polymers.

Experimental

Instruments and equipment used included the following: Fisher Accumet pH meter (model 610A), Orion pH/ISE meter (model 710A), Lab-line orbit environ-shaker, Clay Adams Dynac II centrifuge, Burrell wrist action shaker (model 75), Mettler balance (model AE240), Supelco Visi-1 single sample ultrafiltration processor, Supelco HARP syringe-tip hollow fiber membrane (cellulose acetate with 10,000 molecular-MWCO), Amicon Centricon-10 weight cutoff. microconcentrators (10,000 MWCO), Packard liquid scintillation analyzer (model Tri-Carb 2200CA), Beckman scintillation counter (model LS6000), Packard Minaxi auto-gamma counter (Series 5000), and ICP/MS VG-Plasma Quad 2.

8-Hydroxyquinoline (8HQ) and 4-methyl-8hydroxyquinoline (Me-8HQ) polymers

were prepared according to the literature procedure of YERGOZHIN⁵ by reacting chloromethyloxime with a polyamine. The elemental analysis of 8HQ: C = 35.06%, H = 8.58%, and N = 19.47%.

Phosphonic acid polymer (PPO_3H_2)

was prepared according to the method of KOBAYASHI^{6.7} from the reaction of formaldehyde and phosphorous acid with a polyamine. The elemental analysis was: C = 2.46%, H = 5.48%, N = 8.7%, and P = 16.88%. FT-IR: (KBr): 3433 cm⁻¹ (N-H), 2843, 2354 cm⁻¹ (P-OH), and 1058 cm⁻¹ (P=0).

Radioisotope stock solutions

²⁴¹Am and ²³⁸Pu were obtained from Los Alamos radioanalytical supplies. A ²³⁸Pu(IV) spiking solution was prepared from 5 ml of the ²³⁸Pu stock solution, which was placed in a glass vial with 0.2 ml of 1 N hydroxylamine hydrochloride and heated (80 °C) for 10 minutes. The solution was cooled and 0.2 ml of 2M sodium nitrite was added to complete the oxidation state adjustment. The ¹⁵²Eu(III) was obtained from the National Institute of Standards and Technology (NIST). The 5 ml of solution were concentrated by heating to 3 ml. After spiking, all initial samples were at the tracer level of 8,000 to 100,000 counts/minute/ml (cpm/ml). Survey of commercially available polymers, 8HQ and Me-8HQ

Commercially available functionalized polymers were evaluated in dilute nitric acid for their metal-ion retaining capability. Initial filtration surveys used the Supelco single UF fiber system. The HFM filter was prewetted (3 ml of 1:1 absolute methanol (Baker): deionized (DI) water) and rinsed with DI water. The polymer solutions were prepared with DI water and polymer concentrations ranged from 0.03 to 0.1 wt/vol. %. The pH values, 2 and 6, were obtained with dilute HNO3 or NaOH (Baker). The polymer solutions were spiked with aqueous acidic ²⁴¹Am(III) and shaken or stirred for 30 min. The samples were added to the HARP reservoir and passed through the HFM filter. The actinide content of the retentate was determined by counting equal volume samples of the starting material and filtrate (permeate), using gamma spectroscopy and calculating the percent metal retained.

Binding studies of PPO_3H_2 , varying pH, ionic strength and polymer concentration

These studies used PPO₃H₂ with the Amicon Centricon-10 (C-10) filter unit. A stock solution of PPO₃H₂ (0.1%w/v) was prepared with DI water then prefiltered (Nalgene, 0.2 μ) to remove any colloidal material. Various concentrations of PPO₃H₂ (0.001, 0.01, 0.05, 0.1, 0.6%w/v) and NaNO₃ (0.1 and 4.0M) were used at pH ranges of 2 through 6. The working solutions were spiked with ²³⁸Pu(IV) or ²⁴¹Am(III) and titrated with aqueous NaOH and dilute HNO₃ to the desired pH values.

The C-10 unit is comprised of two halves, a retentate (top) and permeate (bottom) portion, with the membrane filter incorporated in the retentate half. Initial weights of the top (retentate) and bottom (permeate) units were obtained. Samples were placed in the top half of the C-10 unit and centrifuged at 2200 rpm for 25 min until approximately 1 ml remained as the retentate and 1 ml filtered as the permeate. Final weights were recorded for each unit. The solutions and their accompanying half units were placed into separate liquid scintillation vials and measured using alpha spectroscopy (Beckman). Measuring the complete units (the two halves) with the sample gave 100% accountability because no samples were transferred, thus, no loss of activity occurred from adhesion to the sides of the transfer apparatus. Quenching studies showed Optifluor AF had very low quench values in the presence of the water-soluble polymer, nitrate salts, and the C-10 filter unit. Blanks containing only DI water or 0.1M NaNO₃ spiked with ²³⁸Pu(IV) or ²⁴¹Am(III), titrated to pH 2 and pH 5 were performed to determine metal retention in the absence of polymer.

The adsorption or binding ability of the polymer for metal ions is expressed as the distribution coefficient (D), which is defined as: [total bound metal/total free metal] \times [phase ratio]. The phase ratio is the initial sample volume(ml)/initial polymer weight (g) used in the experiment. Total bound metal = retentate activity (cpm/g) - unbound activity (cpm/g); and the total unbound metal = permeate activity (cpm/g) + unboundactivity (cpm/g); unbound activity = permeate activity (cpm/g) × retentate mass/permeate mass. This formula is similar to the equation that is commonly used to evaluate ion exchange resins in single contact equilibrium binding studies,⁸ with a correction made for the unbound actinide that is present in the retentate solution. That correction adds the unbound actinide count in the retentate to the permeate actinide count to obtain total unbound actinide activity. During the ultrafiltration the concentration of the polymer increased in the retentate as the volume decreased by a factor of two, however we observed little change in the D value as a function of the permeate volume change for tracer levels of metal ions. Filtration of half of the material was therefore chosen as the procedure. Since D values are conditional constants, the same filtration conditions were used for all the experiments, thus allowing for comparison of the data and the development of a rapid survey technique.

Capacity studies of PPO_3H_2

A capacity study using 35 ppm Eu(III) from $Eu(NO_3)_3$ · $6H_2O$ with various concentrations of polymer (0.00, 0.01, and 0.1% w/v), 1.0M NaNO₃ at pH 4, and C-10 unit, was performed to determine when available binding sites became saturated. The permeate was analyzed for Eu by ICP-MS.

Metal-ion competition studies

The competition for binding sites on the PPO_3H_2 with ²⁴¹Am(III) and Fe(III) was studied. The working solutions contained various concentrations of Fe(NO₃)₃ (100, 500,1000, 1500, 2000, and 2500 ppm) with 0.1% w/v polymer and 1.0M NaNO₃ at pH 4. The solutions were spiked with ²⁴¹Am(III) and separated as described above.

Results and discussion

Our approach was to investigate commercially available polymers to determine if their use in a polymer filtration system could achieve high recoveries and concentration factors required for treatment of process and waste waters and for low-level analysis. We did a series of blank studies to determine if there was retention

of ²⁴¹Am(III) and ²³⁸Pu(IV) by simple ultrafiltration at the tracer level in the absence of polymer. It was observed that ²⁴¹Am(III) was not retained by the ultrafiltration membrane in the absence of polymer at pH 2 and 40% was retained at pH 5 when no ionic strength adjuster was present. When 0.1M NaNO3 was present 25% was retained at the higher pH value. For ²³⁸Pu(IV) a larger amount of metal was retained at both pH values, 35% (31% in 1M NaNO₂) at pH 2 and 55% (73% in 1M NaNO₃) at pH 5. This is not unexpected as ²³⁸Pu(IV) is known to hydrolyze and polymerize at lower pH values than ²⁴¹Am(III). One has to consider these results carefully because the condensation of hydrolyzed metal ions can take a long time to reach equilibrium and the presence of the chelating polymer can influence these reactions in a number of ways. The chelating groups on the polymer can suppress polymerization reactions and even redissolve colloids and precipitates. The polymers can also act as flocculating agents to bring colloidal or precipitated materials together in larger aggregates depending on factors such as the surface charge on the particulates and the polymer at a particular pH.

The commercially available water-soluble polymers tested are listed in Table 1. ²⁴¹Am(III) was chosen for this survey as it represents the trivalent actinides which are normally more difficult to bind than the tetravalent actinides [e.g., Pu(IV)] and it showed the least amount of hydrolysis. Polyacrylic acid had the highest binding of the commercially available polymers at 73%. It was surprising to us that the polyvinylphosphate did not have better binding capability given the good results with the phosphonic acid polymer described below. It is possible that this polymer was not stable under the experimental conditions and or had a wide molecular weight distribution which allowed some smaller material to pass through the membrane. The polyethylenimine polymer also had very low binding of 25% with ²⁴¹Am(III). This implies that the backbone polymer has little influence on the overall binding of some of the polymers presented below. From Table 1, the observation of higher ²⁴¹Am(III) levels in some permeate with polymer present relative to permeates with no polymer present may be explained by the inhibition of aggregation of hydrolyzed metal species by the polymer or by small molecular weight components of the polymer/metal ion complex, which pass through the UF membrane as mentioned above.

When none of the commercially available materials proved particularly promising because their ²⁴¹Am(III) retention was less than 75%, we synthesized several chelating polymers reported in the literature that contain derivatives of 8-hydroxyquinoline (8HQ and Me-8HQ).⁵ BAYER et al. showed that 8HQ readily binds actinides.^{3,4}



Table 1. Polymer (0.1%w/v) survey for ²⁴¹Am retention

Polymers ^a	Retention at pH 2, %	Retention at pH 6, %
Polyethylenimine (BASF)	<2%	25%
Polyvinylphosphate ^b (Poly Sciences)	1%	11%
Polyvinylsulfonic acid ^b (Poly Sciences)	_	9%
Polyvinylpyrrolidone (Aldrich)	_	<2%
Polyacrylic acid (Aldrich)	14%	73%
Me-8HQ	<2%	19%
8HQ	<2%	97%

^a Polymer samples were used as received.

^b Molecular weights not on sample bottle; vendor indicated MW greater than 10,000 MWCO.

The initial survey of the synthesized polymers are also shown in Table 1. Indeed, at pH 6 the 8HQ showed high binding of 241 Am(III) (97%). It is interesting that a methyl group substituted for a hydrogen adjacent to the ring nitrogen reduced metal binding from 97 to 19%. This indicates that some selectivity could be built into these metal-binding polymers based on steric effects.

Though the initial results with 8HQ were promising, more extensive ultrafiltration recovery experiments indicated that it was difficult to obtain high actinide accountability in the absence of the water-soluble polymer at the higher pH values of 5 to 7. Experiments performed at pH 6 found 241 Am(III) activity adhered to the surfaces of the ultrafiltration apparatus. Good accountability was obtained when the pH was lowered to 4 in the absence of the polymers. This indicated that a chelating polymer was needed that functioned well in the pH 4 range, otherwise an analytical method using this approach would have difficulty in maintaining high accountability.

It was thought that a multidentate phosphonic acid polymer might function well at pH 4. We choose polyethylenimine reacted with phosphorous acid/formaldehyde, which gave a polymer functionalized with methylene phosphonic acid groups (PPO_3H_2) .^{6,7} The preliminary experiments in acidic DI water indicated that the phosphonic acid could bind ²⁴¹Am(III) under the more acidic conditions. For example, when the pH was 3.9 and polymer concentration 0.1% w/v, 99% of the ²⁴¹Am was retained. Whereas, 8HQ gave 8.3% retention of ²⁴¹Am(III)and 100% accountability at pH 4.0 and 0.05% concentration. Though the polymer concentrations were different, it was obvious that 8HQ was not a strong enough chelating polymer to perform well at lower pH values.

The PPO_3H_2 was chosen over other experimental polymers for subsequent examination because of its selectivity, ease of synthesis, and ability to bind trivalent actinides at pH 4. Multidentate phosphonic acid chelating groups have high binding constants for

trivalent and tetravalent metal-ions such as the actinides. At low pH values, metal ions have to compete with protons for the donor sites on the polymer. Phosphonic acids are ionized even at low pH values relative to carboxylic acids and oximes.

A systematic study of the binding of ²⁴¹Am(III) and ²³⁸Pu(IV) verses pH and ionic strength was conducted. The results are reported in Table 2. It can be seen that both ²³⁸Pu(IV) and ²⁴¹Am(III) bind well over the pH range 3 to 6 with 238 Pu(IV) having the higher overall D values. Thus, the pH 4 working range for the analytical procedure should be acceptable for both metal ions. An interesting result from this study as shown in Table 2 is that the D values are larger at the higher nitrate concentration. This result can best be seen at the lower pH values where the D values are smaller. The higher ionic strength will effect both the metal-ion binding constant and the physical properties of the polymer.⁹ These polymers are polyelectrolytes and it is known that higher ionic strengths can cause polyelectrolytes to "swell", perhaps providing more accessibility to binding sites.9

It was also noted that at lower polymer concentration PPO_3H_2 performed better giving higher average log *D* values than at the higher polymer concentration as shown in Table 3. Again, this could be a property of the polyelectrolytes as they are known to aggregate above their critical micellular concentration.¹⁰

Since Fe(III), which can compete with the actinides, is common in waste waters, the effect of the presence of high concentrations of iron on the binding of tracer ²⁴¹Am(III) was determined. The polymer solutions were prepared at lower pH values where all the Fe(III) and Am(III) were mixed and soluble. The pH was adjusted to 4 by the addition of dilute NaOH. The solutions were mixed and then centrifuged. The competition of Fe(III) for ²⁴¹Am(III) binding sites on the polymer indicated that 1500 ppm Fe(III) was needed before a decrease in the average D of 241 Am occurred. Up to this level no effect was observed on the D value of 241 Am(III). At the highest Fe(III) concentrations (1500 to 3000 ppm) a reddish precipitate of Fe(OH)₃ was observed even though the ²⁴¹Am retention decreased substantially. These results indicate that even in the presence of high concentrations of Fe(III) ($\approx 10^4$ to 10^6 times the concentration of Am), this polymer still had a high binding ability for ²⁴¹Am(III). One has to wonder if Fe(OH)₃ is acting as a carrier for the ²⁴¹Am(III), as Fe(III) is known to start precipitating even at pH 3. If this was the case, then when large amounts of $Fe(OH)_2$ were observed, we might expect to see an increase in the D value for 241 Am(III). Instead we observed a decrease in the D value. Thus, the $Fe(OH)_3$ does not appear to coprecipitate a substantial amount of the ²⁴¹Am(III) under these conditions.

рН	Average log D, % retained				
	at 0.1M NaNO ₃		at 4M NaNO ₃		
	²⁴¹ Am	²³⁸ Pu	²⁴¹ Am	²³⁸ Pu	
1	2.07(10.64%)	3.35(68.35%)	4.44(96.53%)	4.61(97.60%)	
2	3.94(89.66%)	4.70(98.03%)	4.91(98.79%)	4.69(98.01%)	
3	4.81(98.49%)	4.90(98.74%)	5.06(99.14%)	5.30(99.48%)	
4	4.81(98.49%)	5.48(99.80%)	4.81(98.48%)	4.78(98.37%)	
5	4.85(98.58%)	5.44(99.63%)	4.84(98.54%)	4.83(98.54%)	
6	4.91(98.69%)	6.44(99.97%)	5.12(99.25%)	5.13(99.24%)	

Table 2. Binding study for 241 Am(III) and 238 Pu(IV) with 0.1% w/v PPO₃H₂ as a function of pH and ionic strength

Table 3. Binding study of 241 Am(III) with PPO₃H₂ as a function of pH and polymer concentration

рН	Avg. log D of ²⁴¹ Am at 0.1 wt/vol. % PPO ₃ H ₂	Avg. log D of 241 Am at 0.01 wt/vol. % PPO ₃ H ₂
2	3.94	4.02
3	4.81	5.52
4	4.81	6.06
5	4.85	6.43
6	4.91	6.55

Europium (Eu), a trivalent lanthanide having similar properties to ²⁴¹Am(III), was used to determine the capacity of the polymer at the working pH value. Different concentrations of the polymer were treated with a stock solution of Eu(III) maintained at a constant concentration of 35.5 ppm/pH 4 in 1.0M NaNO₃, and the amount of Eu(III) in the permeate determined by ICP-MS analysis. The capacity study showed that at 0.001% w/v polymer (0.1 mg), 25.21 ppm Eu(II) was seen in the retentate, indicating an excess of Eu(III). This indicates a capacity for Eu(III) of 103 mg Eu/mg polymer (0.68 mmol Eu/mg polymer). The capacity appears to decrease at higher concentrations of polymer with the 0.01% w/v solution giving a capacity of 32.9 mg Eu/mg polymer and 0.1% w/v solution giving 3.5 mg Eu/mg polymer. This behavior has been noted by GECKELER et al.¹¹ and was attributed to aggregation of the polymer at higher concentrations that inhibited accessibility to binding sites.

Conclusions

We have been able to show that water-soluble metalbinding polymers with ultrafiltration can be used to remove very low-levels of actinides from aqueous streams containing both high and low concentrations of nitrate salt. The phosphonic acid polymer gave excellent results over the pH range of 4–6. Metal-ion binding increased at higher nitrate concentrations and decreased at higher polymer concentrations. The polymer could compete for actinide binding even in the presence of high iron concentrations. The use of these polymers for preconcentration of actinides from actual process and waste waters for analysis is under development.

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