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**The MES Code: Chemical-Equilibrium
Detonation-Product States of Condensed Explosives**

by

Wildon Fickett

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los alamos
scientific laboratory
of the University of California
LOS ALAMOS, NEW MEXICO 87545

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Units and Energy Zero

The primary units are centimeters, grams, microseconds, K (pressure in Mbar, specific energy in Mbar - cm³/g), but the mole and the system mass M_0 (specified by the user) are also used as the mass unit. The energy unit kcal, prevalent in the literature at the time the code was made, is used for a few input and output quantities.

Energies are relative to elements in their standard states (as defined by the NBS) at $T = 0$. For elements which are gaseous under ordinary conditions, such as oxygen, the typical standard state is the molecular form (O_2) in the hypothetical ideal gas state at a pressure of one atmosphere. For elements which are solid under ordinary conditions, such as carbon, the typical standard state is the most common crystalline form (graphite) at zero pressure.

Terms

Contour - Locus of constant T , e , v , or s

CJ - Chapman-Jouguet

CS - Conformational-solution mixture rule

EOS - Equation of state

Ideal (part) - Translation plus internal part of the EOS
(Secs. III.B and IV.C)

Imperfection (part) - Configurational part of the EOS (Secs.
III.B and IV.C)

KW - Kistiakowsky-Wilson (EOS)

LJD - Lennard-Jones-Devonshire (EOS)

LH - Longuet-Higgins mixture rule

Lattice (in LJD) - The cold ($T = 0$) state with all molecules
fixed on their lattice sites

NBS - National Bureau of Standards

Pure-Fluid - Pure species (gas EOS)

Unreacted Material - The unreacted (in general metastable,
as in an explosive) material in the
initial state (p_0, T_0)

Symbols

Intensive thermodynamic functions

p, T, μ - pressure, temperature, chemical potential

Extensive thermodynamic functions

$V, E, H, A, F, S, C_p, C_v$ - molar volume, internal energy, enthalpy, Helmholtz free energy, Gibbs free energy, entropy, constant-pressure and constant-volume heat capacities

$v, e, h, a, f, s, c_p, c_v$ - corresponding specific quantities (per unit mass) [equal to (n/M_0) times molar]

Composition

n - total number of moles per M_0 grams of system

n_g - number of moles of gas per M_0 grams of system

n_s - number of moles of solid per M_0 grams of system

n_i - number of moles of species i per M_0 grams of system

x_i - mole fraction of species i in the gas phase = n_i/n_g

x_s - n_s/n

Intermolecular potential

r^*, T^* - minimum-energy radius and well depth

$V^* = (N/\sqrt{2})(r^*)^3$ - molar volume of fcc lattice with molecules at distance r^*

n, m - repulsive and attractive indices

Chemical equilibrium calculation

c - number of elements

s - number of species

Q - empirical-formula coefficients

α - species-formulae coefficients

a - renumberings

\hat{s} - supersaturation index

Other

D - detonation velocity

Δ - ΔH_f (NBS)

Symbols (cont)

Other (cont)

- \tilde{F} - "free energy" for equilibrium constants; solid: $\tilde{F}_s = F_s$;
gas: $F_i = \mu_i - RT \ln x_i$ (Sec. IV.E)
- γ - $(-\partial \ln p / \partial \ln v)_s$ - adiabatic exponent
- Γ - $v(\partial p / \partial e)_v$ - Grüneisen coefficient
- \hat{H} - $[H^0(T) - H_O^0]$ (NBS)
- M_O - system mass
- N - Avogadro's number
- q - heat of reaction, Sec. IV.F
- R - molar gas constant
- ρ - density
- Σ - sum over all species
- Σ_g - sum over gas species
- u - particle velocity
- z - pV/RT

Superscript or over

- i - ideal
- $'$ - imperfection
- $*$ - NBS tabular function (translation plus internal)
- $-$ - average
- \sim - (1) function (as distinguished from a variable) e.g. $\tilde{p}(T,v)$,
used only when needed to make this distinction
(2) decoration, as in \tilde{F}

Subscript or under

- i - species index
- o - unreacted material in the initial state
- g - gas
- s - solid
- ℓ - lattice (cold curve) function for the LJD EOS
- H - Hugoniot
- other subscripts - partial derivative
- \sim - vector
- \sim - matrix

THE MES CODE: CHEMICAL-EQUILIBRIUM
DETONATION-PRODUCT STATES OF CONDENSED EXPLOSIVES

by
Wildon Fickett

ABSTRACT

The MES code calculates states of the reaction products of detonation in gaseous or condensed explosives under the assumption of thermal and chemical equilibrium. The products may consist of any number of gaseous species and one solid species. The condition of equilibrium includes the number of phases: the solid may or may not be present depending on the current state. In addition to the primary calculation of the Chapman-Jouguet state at a specified set of initial densities, the detonation Hugoniot, and contours of constant temperature, density, energy, or entropy, each at a specified set of pressures may be obtained. All of the first derivatives (e.g., sound speed and heat capacity) are calculated at each point.

The solid equation of state is one constructed from a given shock Hugoniot under the assumption of constant Gruneisen coefficient. For the gas, either the ideal gas, the Kistiakowsky-Wilson, or the LJD (Lennard-Jones-Devonshire cell theory) equation of state may be used. Several choices of "mixture rules" for extending the last one, a pure-fluid equation of state, to mixtures are offered. For LJD, the input data are the parameters defining the intermolecular potentials of the species.

I. INTRODUCTION

The MES code, which performs the calculations described in Refs. 1 and 2, was made some years ago, became dormant when the IBM 7094 became obsolete, and has just been reactivated "as is" in response to a request. I make no apology for things I would now do differently. The only significant changes made in the code are: (1) the replacement of the original machine-language equilibrium routine with an equivalent FORTRAN version, (2) the replacement of several relatively small machine-language I/O routines by approximately equivalent FORTRAN versions, and (3) a new scheme of diagnostic printing.

II. INPUT

The data are entered in packs, each pack preceeded by a CON card. The CON cards have 2A6 format; only the first two fields are data; the user may enter comments on the rest of the card. The first two fields, each left justified, are the word CON and the pack name. Each pack consists of one or more strings, numbered sequentially in the write-up; each string consists of one or more cards. Strings are described by listing their fields; alphameric items are underlined. A few strings, such as the table of initial densities for the CJ locus, and initial pressures for the Hugoniot and contours, are of indefinite length; these must be terminated by a zero. Most of the formats are 6E12.7. A few are 12I6 or 12A6; these are marked (I) or (A).

Data for a job (a batch-type submission) are divided into runs. Each run begins with a CON, PAS card and ends with a CON, REND card. The job ends with a CON, JEND card following the last CON, REND. Each run has two parts. Part 1 (preliminary), beginning with CON, PAS, generally enters parameters of the constitutive relations. In Part 2, beginning with the first CON, SAM card, the packs CJ, TED, and PV each specify a complete calculation to be performed immediately after the pack is read; the user may often want to have more than one of these packs within a run, as well as additional SAM packs. With a few obvious exceptions, the packs of either part may be entered in any order.

The input program reads one pack at a time. It expects to find a fixed number of strings in each pack (even though, under some options, not all of them are used). If the first card of a pack is not a CON card (usually because the user has gotten the wrong number of strings in the previous pack), the program reports an error and skips to the next CON, PAS card and begins reading there. In describing the input data, the phrase "not used" means that the data of the field or string in question is not used by the program under the specified conditions. It will, nevertheless, be read by the program; the user may enter anything, but a blank field(s) is suggested. The only exception is that if an entire pack is not used, it may be omitted.

•Remarks

1. Alphameric constants in the input are given in caps, underlined.
2. Except for the equilibrium calculation, which has its own special order, the first slot of all composition arrays is the number of moles of solid.
3. There are no prestored defaults. Many standard values must be supplied by the user under CON, FOB; the standard pack is given in the sample input,

Sec. VI. CON, SWIT, q.v., does have a mechanism for preserving previously entered items when it reappears.

A. Part 1

•CON, PAS, run label - begin Part 1. The run label becomes part of the standard output header.

•CON, blank, comment.

•CON, SWIT - switches.

(I) diff, fix diff, gas, solid, mix, eq, CJ, PV, PVC.

diff	- 0 - no action
	1 - calculate equilibrium-composition derivatives at each point
fix diff	- 0 - no action
	1 - fixed-composition derivatives similarly
gas	- 0 - ideal-gas EOS
	1 - LJD EOS
	9 - KW EOS
solid	- 0 - incompressible
	1 - Grüneisen EOS
mix	- 0 - none (pure fluid); omit <u>XIP</u> pack
	1 - ideal mixing
	2 - LH mixing
	3 - CS (conformal solution) mixing
	4 - One-Fluid mixing
eq	- 0 - fixed composition
	1 - equilibrium composition
CJ	- 0 - equilibrium CJ condition
	1 - frozen CJ condition
PV	- 1, 2, 3, 4 for T, v, s, e constant on contours (see <u>CON</u> , <u>PV</u>)
PVC	- 0 - no action
	1 - under <u>CON</u> , <u>PV</u> , use last T, p from previous calculation instead of input T_c , p_c

Two of the switches are set (or reset) elsewhere: the mix switch under CON, XIP and the PVC switch under CON, PV.

This pack may also be entered one or more times in Part 2 to change switch settings between calculations. A negative item means: "don't store this item" [use currently stored (last previously entered)] value.

•CON, TIP - ideal thermodynamic functions

1. (I) number of species, degree of fit n.
2. T_{\min} , T_{\max} .
3. a_0 , a_1 , a_2 , ..., a_n , d, ΔH_f^0 , $\Delta H_f(T_0)$, $[H_0(T_0) - H_0^0]/RT_0$.

Polynomial fit coefficients for $[H^0(T) - H_0^0]/RT$, enthalpy integration constant d, heats of formation, and enthalpy at T_0 . One such string for each species.

•CON, SEP - solid EOS

1. Γ , C_p/R , α , V_0 , T_0 , E_0/RT_0 .
Grüneisen coefficient, heat capacity, thermal-expansion coefficient (K^{-1}), initial volume ($cm^3/mole$), initial temperature (K), initial energy. For incompressible solid, only V_0 is used.
2. blank, c_0 , c_1 , c_2 , c_3 , c_4 .
Hugoniot fit coefficients: $P_H(v) = \sum_{i=0}^4 c_i (v/v_0)^i$

•CON, GEP - gas EOS (omit pack for ideal gas), LJD EOS

1. (I) potential index (1, 2, 3 for LJ, MCM, MR).
2. n, m, A_n , A_m , r^* , T^* .
repulsive/attractive exponents, multipliers, well radius r^* ($\text{\AA} = 10^{-10}m$), well depth T^* (K); r^* and T^* not used for a mixture.

•KW EOS

1. (I) 9.
2. α , β , θ .

•CON, XIP - Mixture (omit if SWIT mix = 0), LJD EOS

1. (I) number of (gas) species, type.
type - 1, 2, 3, 4 for ideal, LH, CS, One-Fluid;
2. s_r , s_T , r_r^* , T_r^* , n, m.
 s_r , s_T - scale factors: multiply all input r^* by s_r and all input T^* by s_T .
 r_r^* , T_r^* - reference r^* , T^* (LH only).
n, m - potential n and m (One-Fluid only); ordinarily same as n, m in
CON, GEP [omit if SWIT gas = 0 (ideal gas)]
3. χ^* - one for each (gas) species.
4. \mathcal{I}^* - one for each (gas) species.

•KW EOS

1. (I) 9.

2. s_r^* , κ .

3. k .

Here $k_i \equiv [r_i^*/(N/\sqrt{2})]^{1/3}$, where k_i is the usual KW covolume and N is Avogadro's number.

4. blank.

•CON, EQP - equilibrium (omit pack for fixed composition)

1. (I) c, s, p, ϕ , p' .

c - number of elements

s - number of species

p - number of phases minus 1; used only if $\phi = 0$

p' - first guess for p when $\phi = 1$

$\phi = 0$: fixed number of phases (p + 1)

1: equilibrium number of phases (one or two);

2. Q - system empirical-formula coefficients (number of gram-atoms of each element).

3. (A) blank, element symbols, A1, A0.

A print label; all fields right-justified.

4. α - species-formulae coefficients.

This consists of s strings, one for each species, so that each string is a row of α . The first field, format A6, is the right-justified element symbol, and the remaining fields, format I6, are the coefficients. (For example, with elements C, H, O, and N, the string for carbon dioxide is: C02, 1, 0, 2, 0).

5. (I) a^1 - species renumbering for two-phase system ($\phi=1$) or given system ($\phi=0$).

6. (I) a^0 - species renumbering for one-phase system ($\phi=1$); not used for $\phi=0$.

Dimensions are all fixed once c and s are given:

$$Q(c), \alpha(s \times c), a^1(c), a^0(c).$$

In α the species may be listed in any order. The a 's specify renumberings. If k is the number of a species as originally entered in α , then its new number is a_k . The a_k must be chosen so that after renumbering the following conditions are satisfied: the formula coefficients of the first c species must be linearly

independent; the danger of convergence failure will be minimized by choosing for them those species expected to be present in largest amounts. Two special requirements simplify the program: For $\phi=0$, $p=1$ (two phases), the solid species must be number c. For $\phi=1$, the user must supply two possible systems: Two phase (solid present) and one phase (solid absent); the program chooses the correct one at each T and p. For the two-phase system the solid must be number c. For the one-phase system it must be (nominally) present as number s; here the program assigns it a large free energy so that its calculated mole fraction is negligibly small.

For details and examples see Secs. IV.E and VI, and Appendix A.

•CON, FOB - knobs

1. FROOT ϵ 's.
2. FROOT r 's.
3. $1/2 \Delta \ln p$, $1/2 \Delta T$, ϵ_{outer} , ϵ_{inner} .
4. FROOT bounds.

The FROOT items are in the order given in Sec. V.B, Table III; the bounds are in pairs (min, max). The Δ 's are the displacements for the numerical differentiation, Sec. II.B. The ϵ 's in string 3 are for the outer and inner equilibrium iterations, Sec. V.A.

•CON, DEBUG - print store

Do the standard error print (mainly the entire common store) at this point.

B. Part 2

•CON, SAM, material label - initial state and begin Part 2

1. ρ_0 (g/cm), p_0 (Mbar), T_0 (K), M_0 (g), $\Delta H_f(T_0)$ (kcal/mol).
 M_0 - system mass; must agree with empirical formula under CON, EQP.
 $\Delta H_f(T_0)$ - enthalpy of formation of unreacted material at p_0 , T_0 relative to elements in standard states at T_0 .
2. n - number of moles of each species (for system of M_0 grams). First field is for solid. For equilibrium composition, these are guesses for the first iteration.

We have picked T_0 for the heat of formation because $\Delta H_f(T_0)$ is the quantity usually listed for explosives, and because it is needed for the calculation of the heat of reaction q as usually defined (Sec. IV.F). An alternative, which may be more convenient for some cryogenic materials, is to enter in place of $\Delta H_f(T_0)$ the enthalpy of formation at T_0 from elements at $T=0$. If this is done, the CON, TIP input must also be changed by entering ΔH_f^0 in place of $\Delta H_f(T_0)$ and setting

$[H^0(T_0) - H_0^0]/RT_0$ for each species to zero. This has the advantage of making the TIP input simpler and independent of T_0 . The disadvantage is that the value of q printed out will have a small error (which does not affect on any other calculated quantity).

• CON, TED - detonation Hugoniot at given p

p - pressure table.

• CON, PV - contour of constant T , v , s , or e at given p

1. (I) k , PVC.

k - 1, 2, 3, 4 for constant - T , v , s , e

PVC - PVC switch (see CON, SWIT)

2. T_c , p_c - initial point (not used if $PVC \neq 0$).

3. p - pressure table.

First calculate the point (T_c, p_c) , then use the value of T , v , s , or e from this point as the constant value for the locus. Use T and p from last previously calculated point for T_c , p_c instead of input values if $PVC \neq 0$.

• CON, CJ - CJ locus at given ρ_0

ρ_0 - initial-density table.

• CON, REND - end of run

• CON, JEND - end of job

III. OVERVIEW

In this section we give an overview of the problem and program, including the principal equations. Some of these equations are schematic or just serve as definitions; Sec. IV gives the detailed equations implemented by the program. Section V, together with comments in the program, provides a more detailed description of the program itself.

We define the term state point and some related symbols in Sec. A, the main components of the state-point calculation in Sec. B, and the higher level part of the program which uses the state-point calculation in Sec. C. Principal routine names are given in parentheses with some of the section headings.

A. State Point (MES)

A state point is the usual set of thermodynamic variables V , E , H , A , F , S , and some of their derivatives, the chemical potentials μ_i , the mole fractions x_i , and the total number of moles n (per system mass M_0) at given T and p . Recall that we have at most one solid species, and the convention that it is the first listed.

The mole numbers and mole fractions are given by (see symbol sheet)

$$n = \sum n_i = n_s + n_g$$

$$n_g = \sum_g n_i$$

$$x_l \equiv x_s = n_s/n$$

$$x_g = n_g/n$$

$$x_i = n_i/n_g, i>1(\text{gas}) \quad .$$

Note that $x_i, i>1$ is the mole fraction in the gas phase. The composition may be either fixed (specified) or equilibrium (recalculated at each state point).

Because the equations defining the equilibrium state are implicit and complicated, we obtain derivatives by numerical centered differencing over carefully chosen intervals, rather than attempting to use the very lengthy analytic expressions.

Routine MES calculates a state point at given T and p , using the five packages whose generic names are given in the subheadings of the next section. These packages constitute the bulk of the program.

B. Components of the State-Point Calculation

An extensive quantity for the system is the linear mole fraction sum of those for the two phases, e.g.,

$$E = x_s E_s + x_g E_g \quad .$$

It is convenient to separate functions like E_g and E_s into ideal and imperfection parts. The ideal part, superscript i , represents translation plus the internal partition function; the imperfection part, denoted by a prime, represents the configuration integral.

Descriptions of the five main components of the EOS calculation follow.

1. Ideal Thermodynamic Functions (TIM). We use superscript * to denote the portion of the ideal part that represents the internal partition function; most of the work is in getting this number (for the solid it is the whole value). These functions are tabulated by the NBS and others; they are represented to the program by polynomial fits. The tabulations refer each species to itself at $T = 0$. The program adds the heats of formation at $T = 0$ to refer all to the same reference, namely elements in their standard states at $T = 0$. The physical state corresponding to the tabulation is the given T and $p = p^*$ (1 atm for a gas and zero for a solid), with the stipulation that a gaseous species is in the hypothetical ideal-gas state at T and p^* . For the gas phase, we define the ideal part as that for an ideal gas at the same T , p , and x , so that

$$E^i(T, p, x) = \sum_g x_i E_i^*(T) ,$$

$$S^i(T, p, x) = \sum_g x_i S_i^*(T) - R \ln p/p^* + R \sum_g x_i \ln x_i , \text{ and}$$

$$\mu_i^i(T, p, x_i) = F_i^*(T) + RT \ln p/p^* + RT \ln x_i .$$

2. Solid Equation of State (SEM). For the extensive thermodynamic functions we have

$$E(T, p) = E^i(T, p = 0) + E'(T, p) , \text{ etc.}$$

With the equation of state in the often-used form $p(T, V)$, the imperfection quantities may be defined as the integrals along the isotherm:

$$E'(T, p) = \int_{V(T, p=0)}^{V(T, p)} (T p_T - p) dV ,$$

$$S'(T, p) = \int_{V(T, p=0)}^{V(T, p)} p_T dV , \text{ and}$$

$$\mu' (T, p) \equiv F' = E' + pV - TS' .$$

The EOS used takes the form of equations for T and p along an isentrope through an unknown point T_1, V_1 on $p = 0$, and incorporates simple approximations to the ideal functions on $p = 0$. The equations can be put into a form such that for given T and p the point T_1, V_1 at the foot of the isentrope can be eliminated and the complete EOS at T, p can be obtained by iterative solution of one equation in one unknown. After this is done, the approximate ideal part is subtracted to give the imperfection part (with the correct ideal part, calculated by TIM, added later).

3. Gas Equation of State (GEM). Here we have

$$E (T, p, x) = E^i (T, p, x) + E' (T, p, x) , \text{ etc.}$$

For the usual form $p(T, V)$ the imperfection functions are given by the integrals along the constant-composition isotherm

$$E' (T, p, x) = \int_{RT/p^*}^{V(p, T)} (T p_T - p) dV \quad \text{and}$$

$$S' (T, p, x) = \int_{RT/p^*}^{V(p, T)} (p_T - R/V) dV ,$$

in which the term R/V in the second integral subtracts off the ideal gas part. Also

$$H' = E' + (z-1) ,$$

$$A' = E' - T S' , \text{ and}$$

$$F' = H' - T S' ,$$

For the chemical potentials we have

$$\mu_i' = (n F')_{n_i} \Big|_{n=1} ,$$

where the partial derivative is at constant T , p , and n_j , $j \neq i$, of the gas phase.

Both of our imperfect-gas equations of state, the LJD and the KW, have the form $p(T, V, x)$, and are not explicitly invertible to $V(T, p, x)$. At given T , p , x we must then first solve the equation

$$\tilde{p}(T, V, x) = p$$

(where \tilde{p} on the left distinguishes the pressure function from the given value of pressure on the right) for V and then calculate the imperfection functions at the given T and this V .

The KW EOS is a simple one, and includes the composition dependence. The LJD EOS is much more complicated, requiring for its calculation the numerical evaluation of several definite integrals. In its original form it applies to only a single, pure species. Here it is extended to apply to the gas mixture through one of several mixture rules, described next.

4. Mixture (XIM). The program offers several options for describing the gas mixture. The first is the general one of ideal mixing, for which each mixture property is a linear mole-fraction sum of those of the individual species

$$E'(T, p, x) = \sum_g x_i E_i'(T, p) , \text{ etc.}$$

This may, of course, be applied to any (pure-species) EOS.

The other mixture rules assume that the pure-species EOS is based on an intermolecular potential function and express the mixture properties as expansions in the potential functions or potential-function parameters of the individual species. In some cases the outcome of this expansion is that the mixture is represented by a fictitious fluid with a certain mean potential whose parameters depend on the composition.

5. Chemical Equilibrium (EQM). The composition of the system can be expressed in terms of the progress variables of J independent reactions (ordinarily

J is the number of species minus the number of elements). We symbolize these reactions by

$$\sum_i v_{ij} X_i = 0, \quad j = 1, \dots, J,$$

where X_i represents one mole of species i , so that v_{ij} is the (molar) stoichiometric coefficient of species i in reaction j . The equilibrium composition is the solution of

$$\sum_i x_i \alpha_{ik} = Q_k \quad k = 1, \dots, k$$

$$\sum_i v_{ij} \mu_i (T, p, n_j) = 0 \quad j = 1, \dots, J$$

with the α_{ik} , the chemical formula coefficients (number of moles of element k in one mole of species i), and the Q_k , the empirical-formula coefficients of the system (total number of moles of element k in the system; total of k elements). The first set of equations represents mass conservation, one equation for each element; the second represents the usual "equilibrium-constant" relations for the reactions. The second equations are put in the form

$$\sum_i v_{ij} \ln x_i = - \sum_i v_{ij} \tilde{F}_i (T, p, \underline{x})/RT, \quad j = 1, \dots, J$$

with \tilde{F}_i defined as

$$\tilde{F}_i = \mu_i - RT \ln x_i \quad \text{for a gas species and}$$

$$\tilde{F}_i = \mu_i = F_s \quad \text{for the solid.}$$

The advantage of this procedure is that, for the ideal gas, the \tilde{F}_i are independent of x , so the x -dependence is confined to the $\ln x_i$ terms. For the real gas the \tilde{F}_i

do depend on \underline{x} , but this dependence is small enough so that the equations can be solved by a direct iteration method based on a procedure that solves the ideal-gas problem: Guess \underline{x} , calculate \tilde{F}_i for this \underline{x} , find the ideal gas \underline{x} for the \tilde{F}_i fixed at this value, recalculate the \tilde{F}_i from the new \underline{x} , and repeat to convergence.

6. Derivatives (GAMM). The first partial derivatives (for the complete system) are calculated by centered difference from symmetrical displacements in $\ln p$ and T of carefully chosen size. Three derivatives are approximated by centered differences

$$c_p \equiv (\partial h / \partial T)_p = \Delta h / \Delta T ,$$

$$(\partial \ln p / \partial \ln v)_T = \Delta \ln p / \Delta \ln v ,$$

$$(\partial \ln v / \partial T)_p = \Delta \ln v / \Delta T ,$$

where Δ denotes a difference between the two symmetrically displaced points in p or T . The remaining derivatives are then obtained from these

$$c_p / c_v = 1 + (pv / c_p T) (-\partial \ln p / \partial \ln v)_T [T(\partial \ln v / \partial T)_p]^2 ,$$

$$\gamma = (c_p / c_v) (-\partial \ln p / \partial \ln v)_T , \text{ and}$$

$$\Gamma = \gamma (pv / c_p T) T (\partial \ln v / \partial T)_p .$$

C. Controls for Particular Loci

The rest of the program uses the (T, p) state-point routine (MES) to calculate points on various thermodynamic loci. The routines are given in the section titles.

1. Contours of Constant T , v , s , or e (PV, MESC). The locus is specified by a given value of the desired variable. Thus for constant e , for example, it is the solution of

$$\epsilon(T, p) = e_c ,$$

with e_c the given value of e , specified either as the values of T_c and p_c at which the program is to calculate e_c , or taken from a previously calculated point. Under control of PV, the program calculates points on the locus for each of the set of specified values of p , using MESC to calculate each point.

2. Detonation Hugoniot (TED, HUG). This procedure works the same way, with TED the control and HUG the Hugoniot-point calculator. In this case the equation solved is the Hugoniot equation

$$h - h_0 = \frac{1}{2} (p - p_0) (v_0 - v) \quad .$$

3. Chapman-Jouget Locus (CJ). A CJ point is located by iterative solution of a form of the CJ condition

$$u + c = D \quad ,$$

with u and D given by the shock conservation relations, over a set of points on the Hugoniot, with each Hugoniot point calculated by HUG. The CJ points are determined for the specified set of initial densities.

IV. EQUATIONS

In this section we give the remaining equations in essentially the form used by the program.

A. Ideal Thermodynamic Functions (TIM)

The system is defined by a matrix of constants, one row for each species. Each row contains

$$a_0, a_1, \dots, a_h, d, \Delta^0, \Delta(T_0), \hat{H}(T_0)/RT_0 \quad .$$

Here we have defined, in terms of the NBS notation

$$\Delta^0 = \Delta H_f^0 = \Delta H_f(0), \quad \Delta(T_0) = \Delta H_f(T_0) \quad ,$$

$$\hat{H}(T) = H^0(T) - H_0^0 \quad ,$$

where ΔH_f^0 and $\Delta H_f(T)$ are the heats of formation from the elements in their standard states at $T = 0$ and $T = T$. The standard state is defined as the standard form at the temperature of interest and pressure p^* (1 atm for a gas, 0 atm for a solid), with a gaseous form in the hypothetical ideal gas state. For elements carbon, hydrogen, oxygen, and nitrogen (CHON), the standard forms are solid graphite, and gaseous H_2 , O_2 , and N_2 , respectively. The symbol $H^0(T) - H_0^0$ denotes the enthalpy at T relative to that of the same substance at $T = 0$. The constants a_0 through a_n are the coefficients of a polynomial fit of degree n to $\hat{H}(T)/RT$, and d is the integration constant for the entropy. Recalling our convention that the solid always be species 1, we define

$$\delta_{i1} = 0 \quad \text{if } i \neq 1 \text{ and}$$

$$\delta_{i1} = 1 \quad \text{if } i = 1 .$$

With i the row (species) index, and j the column index, we have

$$H_i^*/RT = \sum_{j=0}^n a_{ij} T^j + \Delta_i^0/RT ,$$

$$G_i^*/RT = \sum_{j=0}^n (j + 1) a_{ij} T^j ,$$

$$S_i^*/R = a_{i0} \ln T + \sum_{j=1}^n [(j + 1)/j] a_{ij} T^j + d_i - (\delta_{i1} - 1) \ln p/p^* , \text{ and}$$

$$F_i^*/RT = H_i^*/RT - S_i^*/R .$$

All these quantities are relative to elements at $T = 0^+$ (entropy at this temperature is zero for all species).

The ideal functions for the gas mixture are then

$$H_g^i/RT = \sum_g x_i H_i^*/RT$$

$$S_g^i/R = \sum_g x_i S_i^*/R - \sum_g x_i \ln x_i, \text{ etc.}$$

The mixture heat of formation from elements at T_0 is

$$\Delta_g(T_0) = \sum_g x_i \Delta_i(T_0) .$$

The total free energy of the gas is not needed, but the F_i^* of the individual species are used in calculating those F_i that determine the equilibrium composition.

The program uses the fits only over the range of T_{\min} to T_{\max} from the input. Outside this range, the results are an extrapolation using the assumption that the heat capacity is constant at its boundary value.

B. Solid Equation of State (SEM)

The solid EOS is constructed from a reference curve and the assumption of a constant Grüneisen coefficient to get off the curve. Defining $y = V/V_0$ (with V_0 here the normal volume of the solid at $p = 0$), the reference curve (see Fig. 1) is the shock Hugoniot $p_H(y)$ for $y \leq 1$ and the $p = 0$ line for $y > 1$. We assume a simple form for the ideal functions on $p = 0$, use it to calculate the complete

[†]The Hugoniot calculation uses the enthalpy relative to elements at T ; with this reference state indicated by explicit inclusion of the reference temperature T_0 as a parameter (together with argument T), the quantity supplied by TIM for this calculation is

$$H_i^*(T;T_0)/RT = \sum_{j=0}^n a_{ij} T^j - (T_0/T) [\hat{H}_i(T_0)/RT_0] + \Delta_i(T_0)/RT_0 .$$

Note that for the alternate SAM input (Sec.II.B), this becomes identical to H_i^*/RT above, i.e., the reference temperature becomes zero.

EOS, and then subtract it to get the imperfection part. Using superscript I to denote the isentrope through point y_1 on $p = 0$ and superscript o to denote functions on $p = 0$, we have for this isentrope

$$p^I = p^I(y; y_1) \text{ and}$$

$$T^I = T^I[y; y_1, T^0(y_1)] .$$

On the reference curve $p = 0$ we take

$$T^0 = T^0(y) = (y - 1)/\alpha$$

$$E^0 = E^0(T^0) = C_p (T^0 - T_0)$$

with constant heat capacity C_p and thermal expansion coefficient α . With constant Grüneisen coefficient Γ we find

$$E/V_0 = (y/\Gamma) p + g(y) ,$$

$$g(y) = p_H(y) [1/2(1 - y) - y/\Gamma] + E_0 \quad \text{for } y \leq 1, \text{ and}$$

$$g(y) = \alpha^{-1} C_p (y - 1) \quad \text{for } y > 1 .$$

For p^I and T^I we find

$$p^I(y; y_1) = \Gamma y^{-(\Gamma + 1)} \int_{y_1}^y y^{(\Gamma + 1)} g'(y) dy \quad \text{and}$$

$$T^I(y; y_1) = T^0(y_1) (y_1/y)^\Gamma .$$

If we represent the reference Hugoniot by a power series

$$p_H(y) = \sum_{i=0}^n a_i y^i$$

with coefficients chosen such that

$$p_H(1) = \sum_{i=0}^n a_i = 0$$

(to make the result simpler), the integral can be done analytically and we find

$$p^I = p_1(y) = (C_p/\alpha V_0) \left[\Gamma/(\Gamma-1) \right] \left[(y_1/y)^{\Gamma+1} - 1 \right] \quad \text{for } y > 1 ,$$

$$p^I = p_2(y) + p_1(1) \quad \text{for } y \leq 1 ,$$

$$p_2(y) = - (\Gamma/y)g(y) + (\Gamma^2/y^{\Gamma+1}) [I(y) - I(1)] , \text{ and}$$

$$I(y) = \int y^{\Gamma-1} g(y) dy$$

$$= \sum_{i=0}^n \left[\frac{1}{2} \left(\frac{a_i}{\Gamma+i} \right) (y^{\Gamma+i-1}) - \left(\frac{1}{2} + \frac{1}{\Gamma} \right) \left(\frac{a_i}{\Gamma+i+1} \right) (y^{\Gamma+i+1-1}) \right] .$$

To get the EOS for given p and T , we must eliminate (by iterative solution) y_1 from $p^I = p$ and $T^I = T$.

•Computation

Given p , T , the function defining y is

$$T^I(y)/T - 1 = 0 .$$

$T^I(y)$ is calculated (for $y < 1$) by first calculating $p_2(y)$, then solving $p^I(y) = p$ for y_1 to get

$$y_1 = \left[1 + (p - p_2(y))/A \right]^{1/(\Gamma+1)}, \quad A = (C_p/\alpha V_0) \left[\Gamma/(\Gamma+1) \right]$$

and then calculating T^I from the equation above. When y_1 is close to 1 (the usual case) the RHS is expanded in a binomial expansion

$$y_1 = 1 + k x + \frac{1}{2} k (k-1) x^2 + \dots$$

$$k \equiv 1/(\Gamma+1)$$

$$x \equiv [p - p_2(y)]/A.$$

For $y > 1$, y_1 is

$$y_1 = y (1 + p/A)^{1/(\Gamma+1)},$$

with expansion

$$y_1 = y \left[1 + k x + \frac{1}{2} k (k-1) x^2 + \dots \right]$$

$$x = p/A.$$

C. Gas Equation of State (GES)

1. Ideal Gas. The EOS is

$$V = RT/p,$$

and the imperfection quantities are all zero.

2. LJD (Lennard-Jones-Devonshire Cell Theory). This EOS is based on an intermolecular potential $u(r)$ (see Fig. 2) with well depth kT^* (k is Boltzmann's constant) and radius r^* . We define a reduced temperature and volume

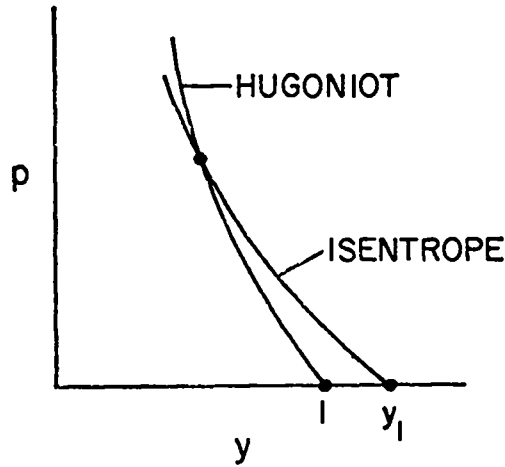


Fig. 1. Solid Hugoniot and isentrope.

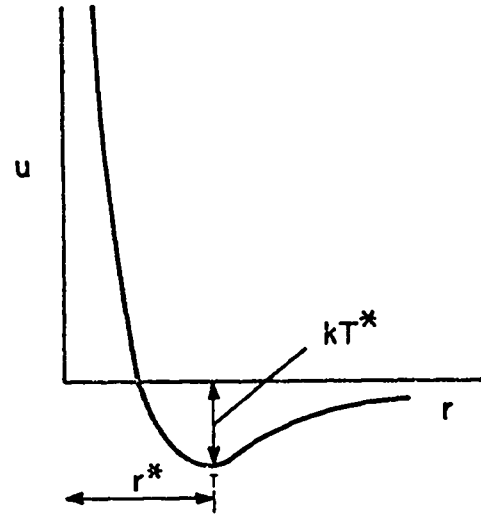


Fig. 2. Intermolecular potential for LJD EOS.

$$\theta = T/T^*, \tau = V/V^*, V^* = 2^{-1/2} N(r^*)^3,$$

with V^* the volume of an fcc lattice with intermolecular separation r^* (N is Avogadro's number). The EOS is a sum of two parts: A lattice ($T = 0$) part, with all molecules fixed on the sites of a regular fcc lattice, and a thermal part, for which the partition function is approximated by a cell integral, in which one molecule moves while all its neighbors remain fixed on their lattice sites.

We first define the lattice and cell-integral functions. We define χ as minus the reduced lattice energy

$$\chi = -\frac{1}{2} Z u(\tau^{1/3} r^*)$$

with Z the coordination number of the lattice for which we use 12, the fcc value. The cell-integral function $G(y)$ is defined as

$$g(y) = \int_0^{b^*} y x^2 e^{-W(\tau, x)/\theta} dx, \quad b^* = 0.55267$$

$$G(y) = g(y)/g(1) \quad .$$

Here the integration variable x is the distance from the cell center in units of the nearest neighbor distance at the given τ , b^* is the distance of the cell boundary from the center, and W is the cell potential relative to its value at the cell center, the potential of a molecule at a given distance from the cell center, in the field of its 12 nearest neighbors smeared into a uniform spherical shell (at the nearest neighbor distance). The cell potential is given by the spherical-smoothing integral

$$W(x, \tau) = \int_{1-x}^{1+x} x' \left[u(\tau^{1/3} r^* x') - u(\tau^{1/3} r^*) \right] dx' .$$

For the two types of potential-function terms we consider (power and exponential) the smoothing integral can be done analytically, but the cell integral cannot.

The cell integrals come from the canonical ensemble, with independent variables T and V . The natural imperfection quantities are thus those relative to ideal gas at the same T and V . Elsewhere, we have used imperfection quantities relative to the ideal gas at the same T and p . The two are the same for all except the entropy and free energies, which are related by

$$S'(T, p)/R = S'(T, V) + \ln z ,$$

$$A'(T, p)/RT = A'(T, V)/RT - \ln z , \text{ and}$$

$$F'(T, p)/RT = F'(T, V)/RT - \ln z ,$$

with the argument p or V denoting imperfection with respect to ideal gas at the same p or V , respectively. In the following, we mark A' with respect to V by argument V (we will refer to it later); all quantities without an argument are with respect to p .

The imperfection thermodynamic functions are

$$z \equiv pV/RT = 1 + \theta^{-1} \left[\tau \chi_{\tau} - G(\tau W_{\tau}) \right] ,$$

$$E'/RT = \theta^{-1} [-\chi + G(W)] ,$$

$$H'/RT = E'/RT + (z-1) ,$$

$$A'(T,V)/RT = 1 - \chi/\theta - \log 2\pi^{1/2} g(1) ,$$

$$A'/RT = A'(T,V)/RT - \ln z ,$$

$$F'/RT = A'/RT + z-1 , \text{ and}$$

$$S'/R = E'/RT - A'/RT .$$

The derivatives, with partials written for $p(T,V)$, $E'(T,V)$ [and $z(\tau,\theta)$, $E'(\tau,\theta)$] are

$$(V/R)p_T = (z\theta)_\theta = 1-\theta^{-2} \left[G(W\tau W_\tau) - G(W) G(\tau W_\tau) \right] ,$$

$$(V^2/RT)p_V = \tau z_\tau - z = \tau(\tau\chi_\tau)_\tau/\theta$$

$$+ \theta^{-2} \left[G^2(\tau W_\tau) g(1) - G^2(\tau W_\tau) - G((\tau W_\tau)_\tau) \right] , \text{ and}$$

$$C'_V/R \equiv R^{-1} E'_T = (E'/RT)_\theta = \theta^{-2} \left[G(W^2) - G^2(W) \right] .$$

The potential functions may be written in the form

$$u(r)/kT^* = (n-m)^{-1} \left[mf(r,n) + nf(r,m) \right]$$

$$f(r,q) = (r^*/r)^q \text{ or } e^{q(1-r/r^*)}, \quad (q = n \text{ or } m) .$$

The three potential forms are

<u>Potential</u>	<u>Repulsive Term</u>	<u>Attractive Term</u>
LJ	power	power
MCM	exponential	exponential
MR	exponential	power

(The symbols α and β have been previously used instead of n and m for the exponential form). To write χ and W , define coefficients a for χ , and b for W for repulsive and attractive terms as follows:

<u>Coefficients</u>		<u>Repulsive</u>	<u>Attractive</u>
a	$=$	$-1/2 A_n Z_n / (n-m)$	$-1/2 A_m Z_m / (n-m)$
b	$=$	$Z_n / (n-m)$	$\delta Z_m / (n-m)$
			$\delta = 0, 1 \text{ for } A_m = 0, A_m \neq 0$

Here the constants A_n and A_m are the Madelung lattice constants for a power-law term and may be regarded as an empirical multiplier for an exponential term. They may also be regarded as switches: $A_n \neq 0, A_m = 0$ gives a one-term (repulsive-only) potential. For a power-law term, the proper value of A_n or A_m takes into exact account the contributions of all neighbors for the lattice contribution; to do this for the exponential form a volume-dependent function would be required. For the b -coefficients, used in the cell integrals, only nearest neighbors are considered, so that the A 's do not appear.

The functions χ and W and their derivatives, are, like the potential, a sum of a repulsive and an attractive term. Using the coefficients a and b defined above, we write the expressions for one term for each of the two forms.

a. Power Form.

$$t \equiv \tau^{1/3}$$

$$\chi = at^{-q}$$

$$\tau\chi_\tau = -(q/3) \chi$$

$$\tau(\tau\chi_\tau)_\tau = (q^2/9)\chi$$

$$W = bt^{-q} \ell(x, q)$$

$$\tau W_\tau = -(q/3) W$$

$$\tau(\tau W_\tau)_\tau = (q^2/9) W$$

$$\ell(x,q) = \left[2(q-2)x\right]^{-1} \left[(1-x)^{-(q-2)} - (1+x)^{-(q-2)}\right]^{-1}$$

$$= \sum_{i=1}^{\infty} c_i x^{2i}$$

$$c_i = (q-2+2i)! / [(q-2)! (2i+1)!]$$

$$c_{i+1} = c_i [(q+2i)(q+2i-1)] / [(2i+3)(2i+2)]$$

The series is used for computation.

b. Exponential Form.

$$s \equiv q\tau^{1/3}$$

$$\chi = a e^{q-s}$$

$$\tau\chi_\tau = -(s/3) \chi$$

$$\tau(\tau\chi_\tau)_\tau = \left[(s^2-s)/9\right] \chi$$

$$W = b e^{q-s} f_1(s,x)$$

$$\tau W_\tau = (b/3) e^{q-s} f_2(s,x)$$

$$\tau(\tau W_\tau)_\tau = (b/9) e^{q-s} f_3(s,x)$$

where the functions f_1 , f_2 , and f_3 all have the form

$$f_i(s,x) = \alpha_i(s) (sx)^{-1} \sinh(sx) + \beta_i(s) sx \sinh(sx) + \gamma_i(s,x) \cosh(sx) + \delta_i(s)$$

with the coefficients α_i , β_i , γ_i , δ_i given in Table I.

• Computation of the g-integral

The 16-point Gauss method is used:

$$\int_0^{b^*} f(x) dx \cong \frac{1}{2} b^* \sum_{i=1}^{16} a_i f(x_i)$$

$$x_i = \frac{1}{2} b^* (1-y_i) ,$$

where the a_i and y_i are the weights and arguments of the method. These are symmetric about the center of the interval $(0, b^*)$

$$y_1 = y_{16} \cong 0.99$$

.

$$y_8 = y_9 \cong 0.1$$

$$a_1 = a_{16} \cong 0.03$$

.

$$a_8 = a_9 \cong 0.19 .$$

TABLE I

COEFFICIENTS FOR THE EXPONENTIAL FORM

i	$\alpha_i(s)$	$\beta_i(s)$	$\gamma_i(s,x)$	$\delta_i(s)$
1	$1+s^{-1}$	0	$-s^{-1}$	-1
2	$-(s+2+2s^{-1})$	-1	$2(1+s^{-1})$	s
3	$s^2+2s+4+4s^{-1}$	$2+3s$	$-(3s+4+4s^{-1}+sx^2)$	$s-s^2$

In the region of interest, the integrands often effectively vanish for x significantly less than b^* . The program allows for this by, in effect, choosing the numerically appropriate upper limit each time, as described in Sec. V.C.

3. KW (Kistiakowsky-Wilson). The KW EOS has its own built-in mixture rule in the form of a linear mole-fraction sum of covolumes k_i

$$k = \kappa \sum_g x_i k_i .$$

Its reduced variable x :

$$x = k/V(T+\theta)^\alpha$$

for $\theta = 0$, would be that corresponding to a repulsive-only potential with

$$k \propto (r^*)^3 (T^*)^\alpha .$$

(actually θ is fixed at 400 K). The equations are

$$z \equiv pV/RT = 1 + xe^{\beta x} ,$$

$$E'/RT = [\alpha T/(T+\theta)](z-1) ,$$

$$F'/RT = (e^{\beta x} - 1)/\beta + z - 1 - \ln z , \text{ and}$$

$$\mu'_i/RT = (e^{\beta x} - 1)/\beta - \ln z + (\kappa k_i/k)(z-1) .$$

The derivatives are, with partials of $p(T,V)$ and $E'(T,V)$

$$(V/R)p_T = z - (1+\beta x)E'/RT ,$$

$$(V^2/RT)p_V = - (1+\beta x)(z-1) - z , \text{ and}$$

$$C'_V/R = \{2 - [1+\alpha(1+\beta x)]T/(T+\theta)\}E'/RT .$$

D. Mixture (XIM)

All the following forms except ideal mixing require the intermolecular potential functions for all binary interactions. To get these from the given potentials for each species, we use the combining rules for r^* and T^*

$$r_{ij}^* = \frac{1}{2} (r_i^* + r_j^*) \text{ and}$$

$$T_{ij}^* = (T_i^* T_j^*)^{1/2} ,$$

and assume the same functional form for all (including common values of the repulsive and attractive exponents n and m).

All of the sums in this section, of course, extend only over the gas species.

1. Ideal Mixing. The properties of the mixture are just linear mole fraction sums of the properties of the components, each calculated as a pure fluid at the given T and p . Thus

$$V(T,p) = \sum x_i V_i(T,p) ,$$

and similarly for the other extensive variables. The chemical potential of each component is just equal to its Gibbs free energy at the given T and p

$$\mu_i(T,p)/RT = F_i(T,p)/RT .$$

2. LH Mixing. This is based on an expansion about the properties of a fixed specified reference fluid (subscript r) in powers of $r_i^* - r_r^*$ and $T_i^* - T_r^*$. All the pure species are assumed to be described by the same reduced EOS $p(\tau_i, \theta_i)$, $\tau_i = V/V_i^*$, $\theta = T/T_i^*$. The partial derivatives are those of the reference-fluid functions with T and V as independent variables: $p(T,V)$, $E'(T,V)$. The equations are

$$f = \sum_{j,k} x_j x_k f_{jk}$$

$$g = \sum_{j,k} x_j x_k g_{jk}$$

$$f_{jk} = r_{jk}^*/r_r^*$$

$$g_{jk} = T_{jk}^*/T_r^*$$

$$z = z_r \left\{ 1 - \left[T/V(-p_T/p_V) + (p/V)/p_V \right] (f-1) + 3 \left[1 + (p/V)/p_V \right] (g-1) \right\}_r$$

$$H'/RT = \left\{ H'/RT + \left[E'/RT - C_V/R - R^{-1} (Tp_T - p)(-p_T/p_V) \right] (f-1) \right\}_r$$

$$F'/RT = \left[F'/RT + (E'/RT)(f-1) + 3(z-1)(g-1) \right]_r$$

$$\begin{aligned} \mu_i'/RT = & \left\{ F'/RT + E'/RT \left[2 \left(\sum_j x_j T_{jk}^*/T_r^* - 1 \right) + (f-1) \right] \right. \\ & \left. + 3(z-1) \left[2 \left(\sum_j x_j r_{jk}^*/r_r^* - 1 \right) + (g-1) \right] \right\}_r, \end{aligned}$$

with all of the thermodynamic functions and their derivatives on the right evaluated for the reference fluid at the given T and V .

3. CS Mixing. This is an improvement over the LH form, with a composition-dependent reference fluid chosen to make $f = g = 1$. The same assumptions apply. The reference fluid is defined by

$$r_r^* = \bar{r}^* = \sum_{i,j} x_i x_j r_{ij}^* \quad \text{and}$$

$$T_r^* = \bar{T}^* = \sum_{i,j} x_i x_j T_{ij}^* .$$

The thermodynamic functions are all just those of this reference fluid except for the chemical potentials, which are the same as those for LH but with r_r^* and T_r^* as defined here and $f = g = 1$:

$$\mu_i^*/RT = \left\{ F'/RT + E'/RT \left[(n/\bar{T}^*) \partial \bar{T}^* / \partial n_i \right] + 3(z-1) \left[(n/\bar{r}^*) \partial \bar{r}^* / \partial n_i \right] \right\}_r ,$$

$$n/\bar{T}^* \partial \bar{T}^* / \partial n_i = 2 \left(\sum_j x_j T_{ij}^* / \bar{T}^* - 1 \right) , \text{ and}$$

$$n/\bar{r}^* \partial \bar{r}^* / \partial n_i = 2 \left(\sum_j x_j r_{ij}^* / \bar{r}^* - 1 \right)$$

These partials are at constant n_j , $j \neq i$.

4. One-Fluid Mixing. This is similar to the CS form, except that the expansion variable is taken to be the potential function itself instead of its parameters r_i^* and T_i^* . It yields a tractable result only for a power-law potential. The reference fluid is defined by the mean parameters

$$s_q = \sum_{i,j} x_i x_j T_{ij}^* (r_{ij}^*)^q, \quad q = n \text{ or } m ,$$

$$\bar{r}^* = (s_n/s_m)^{1/(n-m)} , \text{ and}$$

$$\bar{T}^* = s_m^{n/(n-m)} / s_n^{m/(n-m)} .$$

Again the thermodynamic functions are those of the reference fluid. The chemical potentials are those of the CS form but with

$$(n/\bar{T}^*) \partial \bar{T}^* / \partial n_i = \left[2/(n-m) \right] \left(s_{ni}/s_n - s_{mi}/s_m \right) ,$$

$$(n/\bar{r}^*) \partial \bar{r}^* / \partial n_i = \left[2 + 2/(n-m) \right] \left(m s_{ni}/s_n - n s_{mi}/s_m \right) , \text{ and}$$

$$s_{qi} = \sum_j x_j T_{ij}^* (r_{ij}^*)^q , \quad q = n \text{ or } m .$$

E. Chemical Equilibrium

Recall the definitions given in the input description:

- c = number of independent species
- e = number of elements
- s = total number of species
- $p+1$ = Number of phases ($p=0$: gas only, $p=1$: gas + solid)
- Q_i = empirical-formula coefficients
- α_i = species-formulae coefficients ,

and that, for a complete equilibrium calculation, the user supplies two possible systems: a one-phase system with the solid only nominally present as species number s , and a two-phase system with the solid present as species number c .

Symbols newly defined here are

- q_i = number of moles of each species for a system prepared from independent species only,
- v_k = stoichiometric (chemical reaction) coefficients of the dependent species (independent species have coefficient 1),
- $$v_k = \sum_{j=1}^{c-p} v_{kj} = \text{change in number of moles of gas in reaction } k,$$
- n^s = number of moles of solid,
- n^g = number of moles of gas,
- x_i = (gas) mole fraction n_i/n^g except $x_c = n^s/n^g$ for solid present, and
- K_k = equilibrium constant for reaction k .

We change to superscript s and g here for solid and gas to avoid confusion with indicial subscripts.

1. Initial Calculation. The initial calculation generates constants for the main calculation. Mathematically, it consists of a change of basis from (moles of) elements to (moles of) independent species. In the new basis each dependent species is expressed as a linear combination of independent species, with coefficients that are just the independent-species stoichiometric (chemical reaction) coefficients for the reaction producing one mole of the given dependent species from the independent ones. The system could, of course, be prepared from q_i moles of each independent species i ($i = 1$ to c) instead of Q_i moles of each element.

We now define some index conventions to simplify writing the equations. Divide the α -matrix into independent (c by c) and dependent (s - c by c) parts. Number the complete columns, and the rows of the independent part, with i or j. Number the rows of the dependent part with k. (See Fig. 3.) The ranges are

i and j: 1 to c

k: c+1 to s,

and denote by Σ_i or Σ_j a sum over i or j from 1 to c and by Σ_k a sum over k from c+1 to s. Then α and v are solutions of the linear equations

$$\sum_i \alpha_{ij} q_i = Q_j, \quad j = 1 \text{ to } c \text{ and}$$

$$\sum_i \alpha_{ij} v_{ki} = \alpha_{kj}, \quad j = 1 \text{ to } c, k = c+1 \text{ to } s.$$

The dimensions of v are the same as the dependent part of α and we retain the same usage and range of indices for it. (See Fig. 4.)

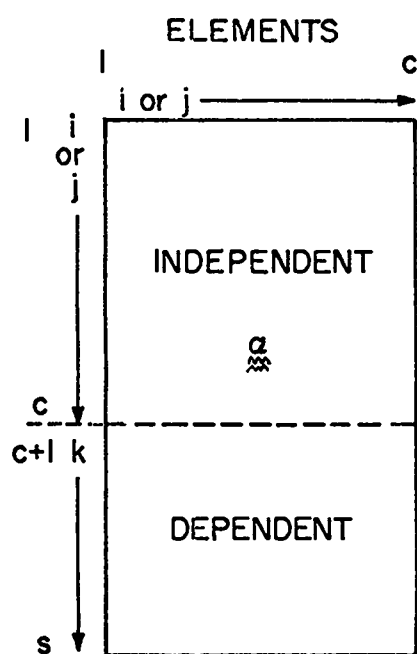


Fig. 3. The α -matrix.

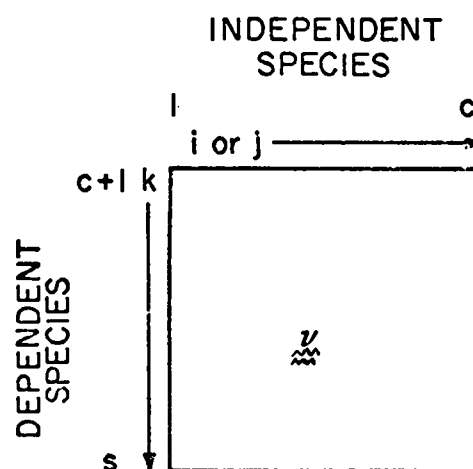


Fig. 4. The v -matrix.

2. Main Calculation. We retain the above index conventions except that now in all sums except that in the definition of K_k the ranges of i and j are

i and j : 1 to $c-p$,

and we use primes to denote sums or products over this range.

The equations can be reduced to a set of $c-p$ equations in $c-p$ unknowns; the remaining mole fractions are determined in the process of solving these or are calculated afterward. The equations are obtained by expressing the dependent species in terms of the independent ones, writing out the first derivatives, and applying the Newton-Raphson method of iteration. Letting superscript (n) number the iteration step, the result is

$$x_i^{(n+1)} = (1 + h_i^{(n)}) x_i^{(n)}, \quad i = 1 \text{ to } c - p$$

(with super (n) understood in the following equations). The increments $h_j^{(n)}$ are the solutions of the linear set

$$\sum_j' A_{ij} h_j = \tilde{F}_i, \quad i = 1 \text{ to } c - p$$

$$A_{ij} = x_i \delta_{ij} + \sum_k x_k v_{kj} G_{ki}$$

$$F_i = -\bar{q}_i + x_i + \sum_k x_k G_{ki}$$

$$G_{ki} = v_{ki} - (v_k - 1) \bar{q}_i$$

$$v_k = \sum_j' v_{kj}$$

$$\bar{q}_i = q_i / \sum_j' q_j$$

$$x_k = K_k \prod_j x_i^{v_{ki}}$$

$$-\ln K_k = \tilde{F}_k - \sum_j v_{kj} \tilde{F}_j .$$

The first equation is a linear system for the h_j . In the second equation δ_{ij} is the Kronecker delta, the x_i 's are the independent-species mole fractions, and the x_k 's are the dependent-species mole fractions, expressed in terms of the mole fractions of the first $c - p$ species through the next-to-the-last equation, which is just the set of equilibrium-constant relations for the reactions. Finally \bar{q}_i is the normalized q_i and v_k the (gas) mole change in reaction k . The K_k and \bar{q}_i are independent of the x 's and are calculated at the beginning.

The x_k 's, $k = c+1$ to s , are found in the process of solving this system. The number of moles of gas is

$$n^g = \left(\sum_j q_j \right) / \left[1 + \sum_k (v_k - 1) x_k \right] .$$

When the solid is present ($p = 1$) the c th equation is decoupled from the first $c - p$ equations because, although each of the first $c - p$ equations contains in general all of the first $c - p$ x_i (by virtue of the presence of the x_i in the equilibrium-constant relations), none contain x_c (by virtue of its absence from the same). Thus, in this case, only the first $c - p$ equations are solved iteratively, and then x_c is determined from the c th equation evaluated for this solution.

As mentioned earlier, in the complete equilibrium case, when a solid may or may not be present, the program carries two possible systems, one with and one without the solid. It begins by solving the case found to be correct on the previous entry, then tests to see if it has the correct one and switches to the other if necessary. If the two-phase system is solved, the test is the sign of the number of moles of solid; if it is positive, the choice was the correct one. If the one-phase system is solved, the test is as follows. Find the first reaction in the two-phase system that involves the solid. Call this the test reaction. In the two-phase system the mole fractions involved in it would have to

satisfy

$$K_k = x_k / \prod_j x_i^{v_{ki}} .$$

(with K and the v 's, of course, from the two-phase system). Define a saturation index \hat{s} for the test reaction as

$$\hat{s} = (x_k / \prod_j x_i^{v_{ki}}) / K_k$$

and evaluate \hat{s} for the x 's (of the species involved) from the one-phase solution. If $\hat{s} < 1$ the system is unsaturated with respect to deposition of solid, and the one-phase choice was the correct one.

F. Miscellaneous

The actual Hugoniot and CJ iteration functions are given in Sec. V.B. (Table III). Note that the Hugoniot function uses enthalpy relative to T_0 and that h_0 is for the unreacted material.[†]

The "heat of reaction" q is defined, for products at given T , p , as the energy released by reaction of the unreacted material in the initial state (T_0 , p_0) to products at the same temperature and pressure (but having the composition calculated at the given T , p)

$$Q = [x_g \Delta_g(T_0) + x_s \Delta_s(T_0)]_{\text{products}} - [\Delta(T_0)]_{\text{unreacted}} - RT_0$$

$$q = (n/M_0)Q .$$

The particle velocity u and detonation velocity D are given by

$$u^2 = (p - p_0)(v_0 - v)$$

[†]If the alternative procedure (heat of formation at $T = 0$ entered under CON, SAM, Sec. II) is followed, then the Hugoniot energies will be relative to $T = 0$. The value of Q will be that at $T = 0$, with the term $(-RT_0)$ incorrectly subtracted.

$$\rho_0^2 D^2 = (p - p_0) / (v_0 - v) \quad .$$

On the isentrope, the particle velocity u , which would require evaluation of the Riemann integral, is not calculated. For the isentrope whose initial point is a CJ point, the quasi-static work done by the explosive in expansion of the products to the given pressure, described in Appendix B,

$$W(p) = e_j - \frac{1}{2} u_j^2 - e_i(p)$$

is printed in the u -slot.

V. PROGRAM

The program listing, Appendix C, contains a list of all routines and common data blocks, with a one-line description of each. It also contains, with each routine, comments giving the routine's specifications. In most cases, the logic is simple enough that suitably placed internal comments suffice to describe it. The exceptions are collected here, in order of decreasing logical level in the program. A detailed list of the contents of all common data blocks is given in Appendix D.

A. Equilibrium Iteration - EQM

To calculate a state point at given T and p , MES calls TIM for the ideal free energies (F_i^i at the given T), and then SEM for the solid free energy $\mu_s' \equiv F_s(T, p)$. It then calls EQM, which calls XIM for the gas mixture EOS in the process of finding the equilibrium composition. Finally it calls TIM for the complete set of ideal functions at the new composition, and then COUT for the complete state.

Because of the multiplicity of EOS and mixture-rule options, EQM and XIM are the most complex routines of the program. EQM is outlined in Table II. Subscript i means all species; for example, $\hat{x}_i \leftarrow x_i$ means save all gas mole fractions. Also, only the most important input and output items of routines XIM and EQMS are indicated. In words, the solid \tilde{F} is calculated once at the start because it depends only on T and p , which are here fixed. First, the mixture routine XIM(1) is called for the imperfection chemical potentials. These are then added to the ideal ones (calculated earlier by TIM) to get the \tilde{F}_i which are the input to the (ideal, i.e., constant- \tilde{F}_i) equilibrium routine EQMS. The current

TABLE II
THE EQUILIBRIUM-EOS ROUTINE EQM

	$\tilde{F}_S \leftarrow F_S^i + F_S'$	solid \tilde{F} , depends on T, p only
α	$\mu_i', r^* \leftarrow \text{XIM}(1)$	gas μ_i' (r^* for LH & One-Fluid only)
β	$\tilde{F}_i \leftarrow F_i^i + \mu_i'$	(F_i^i from TIM earlier)
	$\hat{x}_i \leftarrow x_i$	save old x_i
	$x_i \leftarrow \text{EQMS}(\tilde{F}_i, \tilde{F}_S)$	new x_i at constant F_i
	if $(\sum x_i - \hat{x}_i < \epsilon)$: go to γ	done?
	$x_i \leftarrow 1/2 (x_i + \hat{x}_i)$	next guess: mean of new and old
	$\tilde{F}_i, \bar{r}^* \leftarrow \text{XIM}(2)$; go to β	(CS or One-Fluid only)
γ	if [(CS or One-Fluid) and $(\bar{r}^* - r^* < \epsilon)$]: go to α	outer done?
	(gas state) $\leftarrow \text{XIM}(3)$	final state

composition is saved for later use in the convergence test and in getting the next guess, and then EQMS is called to calculate the composition implied by the current \tilde{F}_i and \tilde{F}_S . If the resulting composition change is small enough, this finishes the iteration for other than the CS or One-Fluid mixture rules (used only with LJD EOS). If not, the next guess for the composition is taken as the mean of the new and old values, new \tilde{F}_i are computed by XIM(2), and the cycle is repeated starting at β . For the CS and One-Fluid mixture rules the completion of the above (inner) iteration is one step of an outer iteration whose convergence test is that the value of \bar{r}^* from XIM(2) after the inner iteration is complete be close enough to its value furnished by XIM(1) at the start at α . This is discussed in more detail below.

We next describe the action of XIM, which is different for the different equations of state and mixture rules. Here GEP is the gas EOS routine, which

gives the ideal-gas, LJD, or KW equations of state (according to the gas switch from CON, SWIT) and XIM chooses the mixture rule from this switch and the mix switch, which we here call k, from CON, SWIT or CON, XIP. For the LH, CS, and One-Fluid mixture rules, XIM calls XIMS for the detailed computations. The notation $XMT \leftarrow GM$ indicates that the pure-fluid state in the GM array is moved to the mixture state in the XMT array. Also, T^* and V^* are to be understood in addition wherever r^* is indicated. The numbers (1), (2), and (3) refer to action taken at the XIM(i) calls, $i = 1, 2, 3$. The options are as follows:

• KW EOS

Recall that GEP calls HKW, which calculates the complete (mixture) EOS.

(1), (2), (3) HKW via GEP supplies the state, including the μ_i .

• k=0: No-mix [normally used only for a pure fluid (single species)]

(1) GEP supplies the pure-fluid EOS for the input r^* . The μ_i are all set to the pure-fluid F_g , and $XMT \leftarrow GM$.

(2) No action.

(3) $XMT \leftarrow GM$.

• k=1: Ideal mix

(1) For each species, set r^* to r_i^* , call GEP for the pure-fluid EOS, and set μ_i to F_g .

(2) No action.

(3) Calculate all mixture imperfection quantities as linear mole-fraction sums of those for the individual species.

• k=2: LH mix

(1) Set r^* to the input reference-fluid value, then call GEP for the pure-fluid EOS, and call XIMS for the μ_i .

(2) Call XIMS for the μ_i .

(3) Call GEP for the final state, then $XMT \leftarrow GM$. (Why any action is needed here is no longer clear to me.)

• k=3: CS mix, and k=4: One-Fluid mix

(1) Call XIMS to get \bar{r}^* , set r^* to \bar{r}^* and call GEP for the EOS, then XIMS for the μ_i . (XIMS calculates both \bar{r}^* and the μ_i , using the reference-fluid state. Here two calls on it are necessary, the first gets r^* , which is needed for the reference-fluid state. There are actually two entries to XIMS that are not distinguished here; the first calculates only \bar{r}^* , the second both \bar{r}^* and the μ_i .)

(2) Call XIMS for the μ_i' and \bar{r}^* .

(3) No action.

The outer iteration described earlier is necessitated by a time-saving device introduced in GEP. A second entry GEP(2) calculates the approximate gas EOS (for LJD) by the quick route of the LH expansion from the reference state currently stored. This time-saving entry is used by XIMS to get the gas state required for the calculation of the μ_i' . Where the mean \bar{r}^* depends on composition as for the CS and One-Fluid mixture rules, the validity of this expansion is ensured by the outer iteration.

B. Iterations

The iterations are tabulated in Table III. All except that for the equilibrium composition described above can be written as a function of a single variable and are controlled by FROOT. Note that the gas and solid EOS iterations, independent and on the same level, must both be completed as part of the equilibrium iteration, which must in turn be completed as part of the calculation of the function for the Hugoniot or constant-v, s, or e iterations. Finally the Hugoniot iteration must be completed as part of the calculation of the function for the CJ iteration. This stacking requires careful adjustment of the convergence criteria for a reliable system. The functions chosen are not too nonlinear and their magnitudes and slopes are reasonable size (the factor of 20 in the Hugoniot function is introduced for this reason). In general there are slots in CON, FOB for several constants for each FROOT iteration: (1) The convergence criterion ϵ , (2) The "guess-constant" r , in most cases the ratio of the second to first guess, and (3) upper and lower bounds for the iteration variable or the related physical quantity. Not all of (2) and (3) are used in every case. Under "Bounds", subscripts min and max denote (3), other bounds are computed as indicated. Finally, we use subscripts 1 and 2 in the "Guesses" column to denote iteration steps 1 and 2. Remarks on some of the iterations follow.

•CJ

For the second guess, a constant- γ isentrope is a sufficiently good approximation to the CJ locus. For the lower bound, we use the constant- γ approximation to the constant-volume detonation pressure. In the function, γ is evaluated for either fixed or equilibrium composition according to the setting of the input switches; thus either a frozen or equilibrium CJ point may be obtained.

TABLE III

Iteration for ^a	FROOT C-array	In Routine	ITERATIONS		Independent Variable x	Function f(x)
			Guesses	Bounds		
Chapman-Jouguet	CC	CJ	$p_1 = \text{previous (0.3)}$ ^b $p_2 = p_1 (v_1/v_2)^{\gamma_1}$ $v_2 = g(p_1)$	$p > \frac{1}{2} (\gamma-1) \rho_0 q \approx p_H(\rho_0)$	p	$j(p) - 1$ $j(p) = \left[\frac{v/v_0}{\gamma(\gamma+1 - p_0/p)} \right]^{-\gamma}$
Hugoniot	CH	HUG	$T_1 = \text{previous (3000)}$ $x_2 = x_1 - f_1/f_1'$ ^c	$T > T_{\min}$ $T < T_{\max}$	T/1000	$20 \left[\frac{h(T; T_0) - h_0(T_0; T_0)}{(p-p_0)v_0} - \frac{1}{2} \left(1 + \frac{v}{v_0} \right) \right]$ ^d
Contour (constant- v, s, or e)	CM	MESC	$T_1 = \text{previous}$ $T_2 = r T_1$	none	T	v: $v-v_c$ s: $e^{s/s_c} - 1$ e: $e-e_c$
Gas EOS	CG	GEP	$x_1 = \text{previous (}\ln 10\text{)}$ $x_2 = x_1 - f_1/f_1'$	$V_g > V_{g \min}$ $V_g < V_{g \max}$	$\ln V_g$	$\ln [p(V_g, T)/p]$
Solid EOS	CS	SEMS	$x_1 = \text{previous (0.8)}$ $x_2 = r x_1$	$x > x_{\min}$ $x < 1 + \alpha(T-T_0)$	V_s/V_{s0}	see Sec. IV
Equilibrium composition	See Sec. V.A.					

^aThe order given is that of the CON, FOB input corresponding to that of the C-arrays in store. Logically, the equilibrium-composition iteration be-
just above that for the gas EOS, and the gas and solid EOS are on the same level as are the Hugoniot and the contour.

^bThe value in parentheses is used on first entry.

^cOn first entry, $f_1' = r$.

^dThe energy zero for h is T_0 ; see Sec. IV.A.

•Hugoniot

The value of f' for the second guess is that calculated by numerical difference on the last step of the iteration for the previous point. On the first time through it is the input guess-constant r .

•Gas

The derivative f'_1 for the second guess is calculated from the derivative $(\partial p / \partial V_g)_T$ furnished by the gas EOS routine GEM.

•Solid

The function, given in Sec. IV.B, is based on the isentrope relation. The quantity α in the upper bound is the thermal-expansion coefficient.

C. LJD Gas EOS Integration (In GES)

As shown in Fig. 5 the problem is to evaluate to prescribed accuracy for any α an integral

$$\int_0^{b^*} f(x; \alpha) dx ,$$

with the integrand depending on α in such a way that for some α it effectively vanishes at some x appreciably less than b^* . We use the 16-point Gauss approximation (Sec. IV.C); its straightforward application to this case would waste those points lying in the region of $f(x) \cong 0$. (Actually all seven integrals are done at the same time; for simplicity the description here is for one.)

The method is to check for the vanishing of the integrand and to perform the integration in segments if necessary. Because α changes little between most of the entries, this turns out to be reasonably efficient. The part of GES that does the integration consists of a control code, which chooses and adds the segments, and a procedure that integrates over a segment and reports how soon the integrand becomes negligible, if at all. All segment lengths are $b^*/2^n$, n integral.

The segment integration procedure $\mathcal{I}(b_1, b_2)$ evaluates $\int_{b_1}^{b_2} f(x; \alpha) dx$ by the 16-point Gauss method and reports three conditions for the size of the integrand near the end of the interval. Let i ($i = 1$ to 16) be the Gauss point at which the integrand first becomes negligibly small. Then \mathcal{I} reports that the upper limit b_2 is

"too small" for no such i ($LD = 1$),

"just right" for $14 \leq i \leq 16$ ($LD = 3$), or

"too large" for $i < 14$ ($LD = 2$),

LD being the Fortran variable that reports the condition. (The actual test is that the condition $|f(x_i)/\sum_{j=1}^i a_j f(x_j)| < \epsilon$ be satisfied for each of the seven integrals). The algorithm which evaluates the complete integral using the segment procedure $\tilde{I}(b_1, b_2)$ is given in Table IV.

D. FROOT-Solve $f(x) = 0$ by Iteration

Number the successive steps in the iteration 1, 2, 3, ..., n, ... with nth (function) argument x^n and function $f^n \equiv f(x^n)$. The complete current state of the iteration is contained in FROOT's argument array c

- c 1 ϵ - convergence: $|f^n| < \epsilon$
- 2 x^n
- 3 f^n
- 4 x^{n-1}
- 5 f^{n-1}
- 6 x^{n-2}
- 7 f^{n-2}
- 8 n - step number
- 9 k - branch index:
 - 1 - finished ($|f^n| < \epsilon$)
 - 2 - continue
 - 3 - error 1: $\tilde{x}^n = x^n$ (see below)
 - 4 - error 2: $f^n = f^{n-1}$.

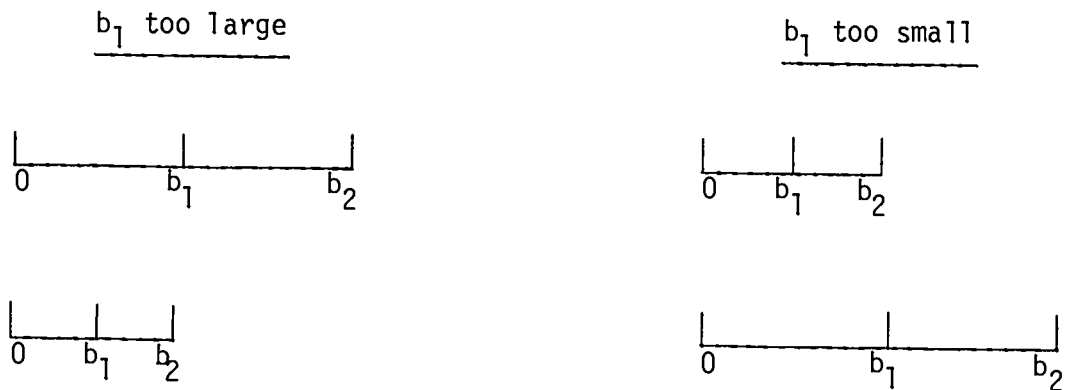
Each time it is called, FROOT bumps n by 1, finds the new x^n and returns to the user, who calculates $f^n = f(x^n)$ and calls FROOT again. The user exits from this loop on convergence via the branch number k. The prototype program is (ϵ pre-stored)

$$n \leftarrow 0, \quad x^n \leftarrow x_g^2, \quad x^{n-1} \leftarrow x_g^1$$

TABLE IV
ALGORITHM FOR THE CELL INTEGRAL

$\alpha \ b_2 \leftarrow b', \ b_1 \leftarrow b'/2$ $I \leftarrow \tilde{I}(0, b_1)$ if (b_1 just right): done if (b_1 too large): $\langle b' \leftarrow b^*/2, \text{ go to } \alpha \rangle$ if (b_1 too small): $\langle \beta \ I \leftarrow I \pm \tilde{I}(b_1, b_2)$ if (b_2 too large or right): done if (b_2 too small): $\langle b' \leftarrow 2b',$ $b_2 \leftarrow b', \ b_1 \leftarrow b'/2, \text{ go to } \beta \rangle$	b' is upper limit from last entry first segment halve and start again add 2nd segment double
---	--

The upper limit b' (not shown is that b' is bounded $\leq b^*$) is saved each time and used as the first guess on the next entry. The successive segments look like



```

α  CALL FROOT
   GO TO (β, γ, δ1, δ2) k

γ  calculate fn ≡ f (xn)
   GO TO α

δ1, δ2  error handling

β  done, proceed

```

Here n , x^n , etc., refer to slots in \underline{c} as indicated above. The user starts the iteration by setting the step index n to zero and supplying x_g and x_g^2 , the first two guesses for x . The iteration then proceeds through the α - γ loop to convergence. Because all the current state is in \underline{c} (and none of it is stored in FROOT), one copy of FROOT can simultaneously control any number of interdependent iterations (i.e., the calculation of $f(x)$ for some iteration may itself require an iterative solution involving FROOT).

The algorithm is the secant method

$$x^1 = x_g^1 ,$$

$$x^2 = x_g^2 ,$$

$$x_n = x^{n-1} - f^{n-1} (x^n - x^{n-1}) / (f^n - f^{n-1}) ,$$

with a refinement wherein \tilde{x}^n is a provisional value of x^n subject to modification. In the normal case it is accepted and the store is stepped down as follows:

$$(x, f)^{n-2} \leftarrow (x, f)^{n-1} ,$$

$$(x, f)^{n-1} \leftarrow (x, f)^n ,$$

$$x^n \leftarrow \tilde{x}^n .$$

The modification replaces \tilde{x}^n if, roughly, it does not lie in the range of previous x 's and if two f 's of opposite sign are on hand. Precisely, if

(1) \tilde{x}^n is not between x^n and x^{n+2} , and

(2) $(\text{sign } f^n = \text{sign } f^{n-1})$ and $(\text{sign } f^n \neq \text{sign } f^{n-2})$

then \tilde{x}^n is recalculated (before the step-down) with point $(n-2)$ instead of $(n-1)$

$$\tilde{x}^n = x^n - f^n (x^n - x^{n-2}) / (f^n - f^{n-2}) .$$

Also, saving of old points is done in such a way that once two f 's of different sign are on hand, the step-down will never result in three f 's of the same sign. Precisely, if condition (2) is satisfied, then the step-down is preceded by

$$(x, f)^{n-1} \leftarrow (x, f)^{n-2} .$$

We remark that, because \underline{c} specifies the state completely, the user, knowing the program's algorithm, may wish to change it in flight. A common case is that a lower bound x^* is known for x , and FROOT at some step supplies $x^n < x^*$. The user might replace x^n by x^* whenever this happens.

As an example (see Fig. 6), we write the code to solve $f(x) = x^{1/2} - A = 0$. The secant recipe can easily give a negative x as the next guess; we prevent this by introducing a fixed lower bound $x = x^*$, x^* small.

```
DATA C(1)/1.0 E-8/
DIMENSION C(9), KC(2)
EQUIVALENCE (KC, C(8))
KC(1) = 0
C(4) = 1.
C(2) = 1.2
α CALL FROOT (C)
GO TO (β, γ, δ, δ) KC(2)
```

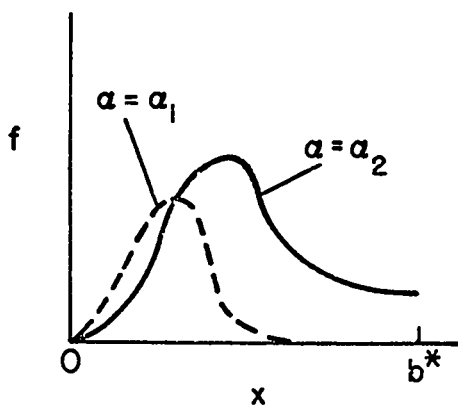


Fig. 5. Integrands for the LJD cell integral.

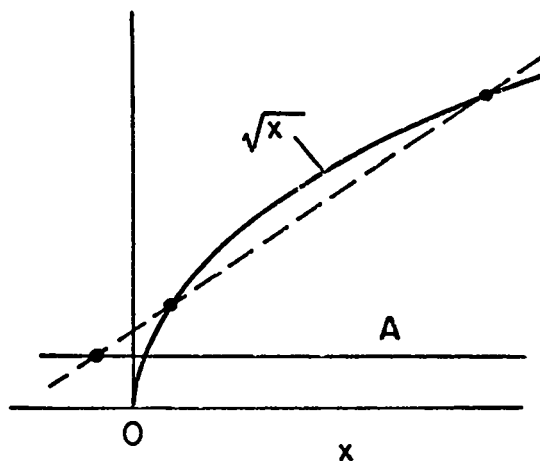


Fig. 6. Iterative solution of $f(x) = x^{1/2} - A = 0$ by FROOT.

```

      IF (C(3) < x*) C(3) = x*
      C(3) = SQRT (C(2)) - A
      GO TO alpha
delta CALL ERR
beta CONTINUE

```

VI. SAMPLE INPUT/OUTPUT AND TEST

Tables V and VI are a key to the output labels and a sample calculation, which also serves as a fairly complete test of the program. The calculation is a chemical equilibrium calculation for the explosive RDX with the LJD EOS and the CS mixture rule. Part 2 of the input defines the following:

- (1) A state point at $T = 2000$, $p = 0.3$.
- (2) Detonation Hugoniot points at $p = 0.3$ and 0.2 .
- (3) CJ points for $\rho_0 = 1.6$ and 1.8 .
- (4) CJ isentrope points at $p = p_{CJ}$, 0.3 , and 0.2 .

A CON, DEBUG print follows item (1). The point printed here is the last slightly displaced one used in the finite-difference calculation of the derivatives.

TABLE V
OUTPUT KEY

Line

1	p	v/v_0	T	u or W	D	ρ_0	q
2	v	e	s	n_g	n_s	n	$(\ln \hat{s} \text{ or } -\hat{n}_s)$
3	V	E/RT	S/R	z	n_1	n_2	n_3
4	V_g	E_g'/RT	S_g'/R	z_g'	n_4	n_5	n_6
5	V_r	E_r'/RT	S_r'/R	z_r'	n_7	n_8	n_9
6	V_s	E_s'/RT	S_s'/R	z_s	n_{10}	n_{11}	n_{12}
7	\bar{r}^*	\bar{T}^*	\bar{V}^*	γ	α	β	c

Notes

1. Lines 1-3 are for the complete system. For lines 4-6 the first four items are for the gas phase, the gas-phase reference fluid, and the solid phase, respectively. The reference fluid differs from the gas phase only for the LH mixing rule (Sec. IV.D.2).
2. The last item in line 2 gives the state of super- or undersaturation of the system with respect to the solid phase; $\ln \hat{s}$ (the saturation index, Sec. IV.E) is printed if a single-phase system was specified and it wants to precipitate solid, and $-\hat{n}_s$ (the number of added moles of solid which would just saturate the system) is printed if a two-phase system was specified and no solid is present.
3. All mole numbers are moles per mole of system (one mole of system = M_0 grams, with M_0 from the SAM input pack).
4. The "u or W" slot in line 1 is the particle velocity for the Hugoniot or CJ point, the quasi-static expansion work (Sec. IV.F and Appendix B) for the CJ isentrope, and meaningless otherwise.
5. All other symbols are defined in the symbol list. Recall that $z \equiv pV/RT$ (and $z' = pV/RT - 1$) and that a prime denotes an imperfection quantity (Secs. III.B.1-3). Molar quantities for the system are per mole of system and for the phases are per mole of phase. All quantities divided by RT are dimensionless.

TABLE VI
SAMPLE CALCULATION

Input Data

```

CON PAS MES1 = SHORT TEST = CJ, HUG, ISENTROPE
CON SWIT DIFF

1
CON F08
5.0 E+05 2.0 E+06 1.2 E+05 7.0 E+07 1.0 E+07 0.0
0.0 1.0 1.1 0.0 9.7 E+01 0.0
1.0 1.01 E+02 1.0 E+05 2.0 E+06 0.0 0.0
1.0 F+03 1.0 E+06 5.0 E+02 8.0 E+03 4.3 E+01 0.0
0.0 0.0 0.0 0.0 0.0 0.0 0.0
CON GEP
2
1.0 E+01 6.0 E+00 1.0 E+00 1.0 E+00 4.4365 E+00 7.54837E+01
CON SEP
1.656 E+01 2.5 8.03 E+06 5.333 2.9816E+02 4.246 E+01
0.0 3.2751 -7.9015 6.6656 -2.0392 0.0
CON TIP
8
1.0 E+03 6.0 E+03
4.8761 E+01 1.4947 E+03 -4.2096E+07 6.2644 E+11 -3.4991E+15 -2.01 E+00
0.0 E+00 0.0 E+00 4.2457 E+01
3.1499 F+00 3.8718 E+24 -1.3665E+07 1.6756 E+11 -8.2278E+16 4.673 E+00
0.0 E+00 0.0 E+00 3.4975 E+00
3.1818 E+00 5.9459 E+04 -1.4065E+07 1.7307 E+11 -8.07 E+16 5.2157 E+00
-2.7222E+01 -2.6416E+01 3.4979 E+00
3.2022E+00 1.18370E+03 -2.1492E+07 2.28400E+11 -1.0874E+15 3.19230E+00
-5.7107E+01 -5.7798E+01 3.99610E+00
3.377 E+00 5.60470E+04 -1.5608E+07 2.04140E+11 -1.0944E+15 5.93 E+00
2.1477 F+01 2.16 E+01 3.7032 E+00
3.2375 E+00 2.3187 E+04 5.0938 E+09 -3.9631E+12 2.931 E+16 -2.8804E+00
0.0 E+00 0.0 E+00 3.4157 E+00
3.7308 E+00 1.9444 E+03 -5.121 E+07 6.8031 E+11 -3.5368E+15 3.4656 E+00
-9.3969E+01 -9.4052E+01 3.7712 E+00
3.4234 E+00 4.55 E+04 -8.0583E+08 9.4557 E+12 -4.8556E+16 4.862 E+00
0.0 E+00 0.0 E+00 3.4934 E+00
CON XIP M2 = BEST MCM SET FROM OTHER SOURCES ,GMX=10=54,P43
7
1.0 E+00 1.0 F+00 3.80012E+00 1.41744E+02 6.0 E+00 1.2 E+01
4.05 E+00 4.05 E+00 3.35 E+00 3.56 E+00 3.34 E+00 4.2 E+00
3.73 E+00
1.2 E+02 1.2 E+02 1.38 E+02 1.31 E+02 3.7 E+01 2.0 E+02
1.32 E+02
CON EQP
4
3.0 8 1 0 1 1 6.0
C H O N A1 A0
C(S) 1 0 0 0
M2 0 0 0 2
C0 1 0 1 0
H20 0 2 1 0
NO 0 0 1 1
H2 0 2 0 0

```

```

C02      1      0      2      0
02        0      0      2      0
4         1      6      3      7      5      2      8
8         1      2      3      5      4      6      7
CON 3AM   RDX, RHO=1.8, C02=ARBITRARY COMPOSITION GUESS
8
1.8      E+00 0.0      E+00 2.9816 E+02 2.2213 E+02 1.471 E+01
1.5      E+00 3.0      E+00 0.0      E+00 3.0      E+00 0.0      E+00 0.0      E+00
1.5      E+00 0.0      E+00
CON PV
1         0
2.0      E+03 3.0      E+01
0.0      E+00 0.0      E+00
CON DEBUG
CON TED   OETCNAION HUGDN1OT
0.3      0.2      0.0
CON CJ    CJ LOCUS
1.6      1.8
CON PV    CJ ISENTROPE
3         1
0.0      0.0
0.3      0.2
CON REND
CON JEND

```

Calculation

```

MES1 = 744:420      MES1 = SHORT TEST = CJ. HUG. ISENTROPE
TIME=113.      .004 SEC ON RUN.      .056 SEC ON JOB

```

```

CON SWIT DIFF
DIFF: FX DIFF: GAS. SOLID. MIX. EO. CJ. PV
1      -0      -0      -0      -0      -0      -0      -0      -0      -0      -0

```

```

CON FOR
FROM FPSICC.CH*(C*CG+C5-C)/ RATIOS/ DP*OT*EPSIN*OHT/ FROMT HOINOS
5.00000E-05 2.00000E-06 1.20000E-05 7.00000E-07 1.00000E-07
0. 0. 1.00000E-00 1.10000E-00 0.
4.70000E-01 0. 1.01000E-00 1.01000E-02 1.00000E-05
2.00000E-06 0. 0. 1.00000E-03 1.00000E-06
5.00000E-02 0.00000E-03 4.30000E-01 0. 0.
0. 0. 0. 0. 0.

```

```

CON GEP
0      2      1
POT (1=LJ/2-MCM*3=MR1 *W INOW 18 / N*M*AN*AN*R*+*Y*
1.00000E-01 6.00000E-00 1.00000E-00 1.00000E-00 4.43650E-00
7.54837E-01
V*      37.2000000

```

```

CON SEP
CX      0. CPH= 4L. V0. T0. FOR / C0. C1. C2. C3. C4
1.45600E-01 2.50000E-00 8.03000E-06 5.33300E-00 2.98160E-02
4.24600E-01 0. 3.27510E-00 -7.90150E-00 6.66560E-00
-2.03920E-00 0.

```

CON TIP
 KS,KKL/ T BOUNDS/ FIT COEFFS=A1 TO AN,0,0EL=HF,HR...
 8 4
 1.40000E+03 6.00000E+03
 4.87610E-01 1.49440E+03 -4.28960E+07 6.26440E+11 -3.49910E+15
 -2.91000E+00 0. 0. 4.24570E+01
 3.14970E+00 5.8710E+04 -1.36450E+07 1.67540E+11 -8.22780E+16
 4.47700E+00 0. 0. 3.49750E+00
 3.10180E+00 5.94540E+04 -1.40450E+07 1.73070E+11 -8.47000E+16
 5.21570E+00 -2.72020E+01 -2.54160E+01 3.49790E+00
 3.27220E+00 1.14370E+03 -2.14920E+07 2.24480E+11 -1.08740E+15
 3.14730E+00 -5.71070E+01 -5.77980E+01 3.99610E+00
 3.32700E+00 5.40470E+04 -1.50080E+07 2.04140E+11 -1.09440E+15
 5.93400E+00 2.14770E+01 2.14000E+01 3.70320E+00
 3.27500E+00 2.31470E+04 5.09380E+09 -3.96310E+12 2.93100E+16
 -2.22040E+00 0. 0. 3.41570E+00
 3.71080E+00 1.94440E+03 -5.12100E+07 6.80310E+11 -3.53680E+15
 3.44550E+00 -9.39640E+01 -9.40520E+01 3.77720E+00
 3.42340E+00 4.58000E+04 -8.05830E+08 9.45570E+12 -4.85560E+16
 4.84200E+00 0. 0. 3.49340E+00

CON AIP M2 = BEST MCM SET FROM OTHER SOURCES ,GMX=10=54.P43
 KR,KKL/ SCH,SCY,RHFF,TORFF,NIM/ IR*1/ IT*)
 7 2
 1.00000E+00 1.00000E+00 3.80012E+00 1.41744E+02 6.00000E+00
 1.20000E+01
 4.05000E+00 4.05000E+00 3.35000E+00 3.56000E+00 3.34000E+00
 4.20000E+00 3.73000E+00
 1.20000E+02 1.20000E+02 1.38000E+02 1.31000E+02 3.70000E+01
 2.00000E+02 1.32000E+02

CON EGP
 C,S,P,-,PP,PHI / CAP Q
 4 R . 1 0 1 1
 3.00000E+00 6.00000E+00 6.00000E+00 6.00000E+00

	C	H	O	N	A1	A0
C151	1	0	0	0	4	8
M2	0	0	0	2	1	1
CO	1	0	0	0	6	2
M20	0	2	1	0	3	3
NO	0	0	1	1	7	5
M2	0	2	0	0	5	4
CO2	1	0	2	0	2	6
O2	0	0	2	0	8	7

QBAR .3333333E+00 .3333333E+00 .3333333E+00 0.
 NU MAT .5000000E+00 0. .8000000E+01 -.1000000E+01
 2 0. .1000000E+01 .1000000E+01 -.1000000E+01
 3 0. 0. .2000000E+01 -.2000000E+01
 4 0. .1000000E+01 -.1000000E+01 .1000000E+01
 QBAR .4000000E+00 .2000000E+00 .4000000E+00
 NU MAT 0. -.5000000E+00 .1000000E+01 .5000000E+00
 2 0. .5000000E+00 0. .5000000E+00
 3 .5000000E+00 .5000000E+00 0. -.5000000E+00
 4 0. .1000000E+01 0. -.1000000E+01

CON SAM RDX. RHQ=1.8; CO2=ARBITRARY COMPOSITION GUESS

59

MES1 = 7641620 MES1 = SHORT TEST = CJ. HUG. ISENTROPE
 TFICKETIGN. .055 SEC ON RUN. .107 SEC ON JOB
 MS/ RMO. P0, T0, M0, HFE/ N1

09/02/76
 SAM = INPUT PART 2

8
 1.80000E+00 0. 2.98160E+02 2.22170E+02 1.47100E+01
 1.50000E+00 3.00000E+00 0. 3.00000E+00 0.
 0. 1.50000E+00 0.

CON PV

MES1 = 7641620 MES1 = SHORT TEST = CJ. HUG. ISENTROPE
 TFICKETIGN. .063 SEC ON RUN. .115 SEC ON JOB
 BRANCH (1=T,2=V,3=S,4=E) / TC/PC/ P=TABLE

09/02/76
 LOCUS

1
 2.00000E+03 3.00000E+01
 0.

OUTPUT LABELS

1	P	V/V0	T	U	D	RHO	QCAL
2	V	E	S	NG	NS	N	SUPSAT
3	V	E/RT	S/P	PV/RT	N1	N2	N3
4	DO. FOR GAS				N4,N5,N6		
5	DO. FOR RFF.				N7,N8,N9		
6	DO. FOR SOLID				N10,N11,N12		
7	PRAR	TBAR	VRAR	GAMMA	ALPHA	BETA	C
POINT 1	1	3.000000E+01	6.2501147E+01	2.0000000E+03	0.	0.	1.8000000E+00
	2	3.4722859E+01	6.5145242E+03	5.6504530E+05	7.5019585E+00	1.4980495E+00	9.0000080E+00
	3	8.5699799E+00	9.6691129E+01	1.6773249E+01	1.5461110E+01	1.4980495E+00	2.9999918E+00
	4	9.5186840E+00	4.8978060E+00	-1.5675174E+00	1.6172668E+01	2.9985825E+00	1.6077797E+05
	5	9.5182069E+00	4.8980736E+00	-1.5673720E+00	1.6171806E+01	1.4994504E+00	6.9640955E+11
	6	3.8190426E+00	1.1026119E+00	-1.4349374E+01	6.8899389E+00	0.	0.
	7	3.9000514E+00	1.4179073E+02	2.3377078E+01	3.1776524E+00	4.7999481E+00	1.8252305E+00

CON DBUG

OUTPUT LABELS

1	P	V/V0	T	U	D	RHO	QCAL
2	V	E	S	NG	NS	N	SUPSAT
3	V	E/RT	S/P	PV/RT	N1	N2	N3
4	DO. FOR GAS				N4,N5,N6		
5	DO. FOR RFF.				N7,N8,N9		
6	DO. FOR SOLID				N10,N11,N12		
7	PRAR	TBAR	VRAR	GAMMA	ALPHA	BETA	C
POINT 2	1	3.0000000E+01	6.2460797E+01	2.0000000E+03	0.	0.	1.8000000E+00
	2	3.4722859E+01	6.5145242E+03	5.6504530E+05	7.5017720E+00	1.4982350E+00	9.0000070E+00
	3	8.5644442E+00	1.0251742E+00	1.6785067E+01	1.5608777E+01	1.4982350E+00	2.9999930E+00
	4	9.5123142E+00	4.9430188E+00	-1.5737047E+00	1.6336280E+01	2.9987042E+00	1.4021508E+05
	5	9.5118041E+00	4.9433074E+00	-1.5735481E+00	1.6335343E+01	1.4995168E+00	5.4543140E+11
	6	3.8183935E+00	1.1149935E+00	-1.4354516E+01	6.9590543E+00	0.	0.
	7	3.9000467E+00	1.4179416E+02	2.3376997E+01	3.1776524E+00	4.7999481E+00	1.8252305E+00

[illegible]

XMU	25.2446190	25.2446190	16.4160201	19.3774848	12.0422775	29.8665753	21.6020048	0	0	0
APF	120.0000000	120.0000000	128.6856635	125.3774241	66.5333250	154.4193338	125.8570618	0	0	0
XPG	4.0500000	4.0500000	3.7000000	3.8050000	3.6950000	4.1250000	3.8900000	0	0	0
XPR	4.0500000	4.0500000	3.3500000	3.5600000	3.3400000	4.2000000	3.7300000	0	0	0
XPT	120.0000000	120.0000000	138.0000000	131.0000000	37.0000000	200.0000000	132.0000000	0	0	0

CCN TEO DETONATION HUGONIOT

MES1 = 76AUG20 MES1 = SHORT TEST = CJ, HUG, ISENTROPE
 TFICKET16N, 255 SEC ON RUN, 306 SEC ON JOB
 P-TABLE
 3.00000E-01 2.00000E-01 0.

09/02/76
TEO = HUGONIOT

OUTPUT LABFLS

	1	P	V/V0	T	U	O	RHO	QCAL
	2	V	E	S	NG	NS	N	SUPSAT
	3	V	E/RT	S/P	PV/RT	N1	N2	N3
	4	DO. FOR GAS				N4, N5, N6		
	5	DO. FOR RFF.				N7, N8, N9		
	6	DO. FOR SOLIN				N10, N11, N12		
	7	RRAR*	TBAR*	VRAR*	GAMMA	ALPHA	RETA	C
POINT 3	1	3.0000000E-01	6.8209108E-01	4.1800622E-03	2.3018432E-01	7.2405743E-01	1.8000000E-00	1.4490847E-00
	2	3.7893949E-01	3.2889349E-02	7.2717497E-05	7.8132457E-00	1.1953025E-00	9.0085483E-00	1.5298412E-01
	3	9.3437728E-00	2.3334302E-00	2.1571501E-01	8.0654831E-00	1.1953025E-00	2.9914696E-00	4.7909272E-01
	4	1.0178271E-01	2.5983520E-00	-1.0676278E-00	7.7858160E-00	2.8526013E-00	1.7060806E-02	1.4739874E-01
	5	1.0239780E-01	2.5880818E-00	-1.0812547E-00	7.8389102E-00	1.3256048E-00	1.7850473E-05	0.
	6	3.8889734E-00	4.6778127E-01	-1.4289480E-01	3.3569362E-00	0.	0.	0.
	7	3.8054155E-00	1.3674799E-02	2.3476215E-01	2.7005031E-00	3.4377594E-00	1.6433084E-00	5.5407417E-01
POINT 4	1	2.0000000E-01	7.9305378E-01	3.8045213E-03	1.5161781E-01	7.3274016E-01	1.8000000E-00	1.4282619E-00
	2	4.4058543E-01	1.7894021E-02	7.2769569E-05	7.9598912E-00	1.0428837E-00	9.0027748E-00	1.3101733E-01
	3	1.0870786E-01	1.3957523E-00	2.1504852E-01	6.8732248E-00	1.0428837E-00	2.9972708E-00	7.0824972E-01
	4	1.1733924E-01	2.0083885E-00	-1.0222304E-00	6.4189573E-00	2.7884647E-00	5.5375631E-03	2.1153484E-01
	5	1.1814529E-01	1.9896503E-00	-1.0439009E-00	6.4699210E-00	1.2488675E-00	6.0617958E-06	0.
	6	4.2828177E-00	2.4792361E-01	-1.0179689E-01	2.7078785E-00	0.	0.	0.
	7	3.8091047E-00	1.3463469E-02	2.3544560E-01	2.6846183E-00	3.0978413E-00	1.5264149E-00	4.8637510E-01

CON CJ CJ LOCUS

MES1 = 76AUG20 MES1 = SHORT TEST = CJ, HUG, ISENTROPE
 TFICKET16N, 583 SEC ON RUN, 634 SEC ON JOB
 CJ RHO=TABLE
 1.60000E-00 1.80000E-00 0.

09/02/76
CJ

OUTPUT LABELS

	1	P	V/V0	T	U	O	RHO	QCAL
	2	V	E	S	NG	NS	N	SUPSAT
	3	V	E/RT	S/P	PV/RT	N1	N2	N3
	4	DO. FOR GAS				N4, N5, N6		
	5	DO. FOR RFF.				N7, N8, N9		
	6	DO. FOR SOLIN				N10, N11, N12		
	7	RRAR*	TBAR*	VRAR*	GAMMA	ALPHA	RETA	C
POINT 5	1	1.9888975E-01	7.2232555E-01	4.0889243E-03	1.8578651E-01	6.6968030E-01	1.6000000E-00	1.4015000E-00
	2	4.5145347E-01	2.3655305E-02	7.4780944E-05	8.1163490E-00	8.8812807E-01	9.0034771E-00	1.0942458E-01
	3	1.1136433E-01	1.7198412E-00	2.2187546E-01	6.5280758E-00	8.8812807E-01	2.9955360E-00	9.4626716E-01
	4	1.1885171E-01	1.9013426E-00	-9.5906179E-01	5.9667285E-00	2.7135671E-00	8.9273000E-03	2.8643254E-01
	5	1.1991605E-01	1.8784533E-00	-9.8744023E-01	6.0291173E-00	1.1656054E-00	1.3430422E-05	0.
	6	4.2979901E-00	2.2279628E-01	-1.0119332E-01	2.5193522E-00	0.	0.	0.
	7	3.8114124E-00	1.3238677E-02	2.3596662E-01	2.8013401E-00	2.9184306E-00	1.5063123E-00	4.8329384E-01

POINT 6	1	2.4894704F-01	7.2997845E-01	3.9844666E-03	1.9324864E-01	7.1567857E-01	1.8000000E-00	1.4418736E-00
	2	4.0554358F-01	2.5069501E-02	7.2603660E-05	7.8656632F-00	1.1353011F-00	9.0049643E-00	1.4426299F-01
	3	1.0003748F-01	1.8666819E-00	2.1540388E-01	7.5174255F-00	1.1353011E-00	2.9950458E-00	5.6811003F-01
	4	1.0855513F-01	2.3172328E-00	-1.0528061E-00	7.1597479E-00	2.8287812E-00	9.9076675E-03	1.7121836E-01
	5	1.0926612F-01	2.3031322E-00	-1.0707144F-00	7.2109219E-00	1.2965897E-00	1.0485669E-05	0.
	6	4.0787010F-00	3.5453600E-01	-1.2246953E-01	3.0649847E-00	0.	0.	0.
	7	3.8070314F-00	1.3593882E-02	2.3506133E-01	2.7034071E-00	3.2774684E-00	1.5822509E-00	5.2242984E-01

CON PV LJ ISENTROPE

MES1 = 76AUG20

MES1 = SHORT TEST = CJ. HUG. ISENTROPE

09/02/76

TFICKET16N. 1.632 SEC ON RUN. 1.684 SEC ON JOB

LOCUS

BRANCH 11=T.2-V.3-S.4-E1 / TC.PC/ P-TABLE

3 1
0. 0.
3.00000E-01 2.00000E-01 0.

OUTPUT LABELS

		P	V/V0	T	U	D	RHO	OCAL
		V	E	S	NG	NS	N	SUPSAT
		V	E/RT	S/R	PV/RT	N1	N2	N3
		00. FOR GAS				N4.N5.N6		
		00. FOR DEF.				N7.N8.N9		
		00. FOR SOL ID				N10.N11.N12		
		RRAP.	TRAR.	VRAR.	GAMMA	ALPHA	RETA	C
POINT 7	1	2.4894704F-01	7.2997845E-01	3.9844666E-03	1.9324864E-01	7.1567857E-01	1.8000000E-00	1.4418736E-00
	2	4.0554358F-01	2.5069501E-02	7.2603660E-05	7.8656632F-00	1.1353011F-00	9.0049643E-00	1.4426299F-01
	3	1.0003748F-01	1.8666819E-00	2.1540388E-01	7.5174255F-00	1.1353011E-00	2.9950458E-00	5.6811003F-01
	4	1.0855513F-01	2.3172328E-00	-1.0528061E-00	7.1597479E-00	2.8287812E-00	9.9076675E-03	1.7121836E-01
	5	1.0926612F-01	2.3031322E-00	-1.0707144F-00	7.2109219E-00	1.2965897E-00	1.0485669E-05	0.
	6	4.0787010F-00	3.5453600E-01	-1.2246953E-01	3.0649847E-00	0.	0.	0.
	7	3.8070314F-00	1.3593882E-02	2.3506133E-01	2.7034071E-00	3.2774684E-00	1.5822509E-00	5.2242984E-01
POINT 8	1	3.0000000F-01	6.8133790E-01	4.1506194E-03	6.2285134E-01	7.1567857E-01	1.8000000E-00	1.4504140F-00
	2	3.7852100F-01	3.2457083E-02	7.2603704E-05	7.8661860F-00	1.2020925F-00	9.0082784E-00	1.5399230F-01
	3	9.3357347F-00	2.3147033E-00	2.1532647E-01	8.0983612F-00	1.2020925E-00	2.9917379F-00	4.6527416F-01
	4	1.0172292F-01	2.6091067E-00	-1.0716390F-00	7.8259305F-00	2.8558995F-00	1.6523390F-02	1.4410009F-01
	5	1.0232402F-01	2.5589927E-00	-1.0849242E-00	7.8780844F-00	1.3296342E-00	1.6865346E-05	0.
	6	3.8882439F-00	4.7078891E-01	-1.4249568F-01	3.3736489E-00	0.	0.	0.
	7	3.8053078F-00	1.3685726E-02	2.3474259E-01	2.7056370F-00	3.4509657E-00	1.6450713E-00	5.3429430F-01
POINT 9	1	2.0000000F-01	7.9167471E-01	3.7817053E-03	2.6341168E-01	7.1567857E-01	1.8000000E-00	1.4302499F-00
	2	4.3981928F-01	1.7418127E-02	7.2603722F-05	7.9482801F-00	1.0543765E-00	9.0026566F-00	1.3265467F-01
	3	1.0852425F-01	1.3664470E-00	2.1545919E-01	6.9027591F-00	1.0543765F-00	2.9973494F-00	6.9044535F-01
	4	1.1723572F-01	2.0172005E-00	-1.0273858E-00	6.4571326E-00	2.7938894E-00	5.3018977F-03	2.0611114E-01
	5	1.1802714E-01	1.9957990E-00	-1.0485454E-00	6.5071586E-00	1.2551761E-00	5.6424670F-06	0.
	6	4.2819856F-00	2.4994174E-01	-1.0180381E-01	2.7236865E-00	0.	0.	0.
	7	3.8088931F-00	1.3480486E-02	2.3540636E-01	2.6714850E-00	3.1134498E-00	1.5283198E-00	4.8657312F-01

CON REHD

CON JEND

MES1 = 76AUG20

MES1 = SHORT TEST = CJ. HUG. ISENTROPE

09/02/76

TFICKET16N. 2.112 SEC ON RUN. 2.164 SEC ON JOB

JOBEND

DAY=TIME START 21.00.59 . END 21.01.01

COMPLETE TFICKET16N

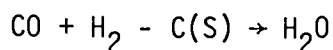
ACKNOWLEDGMENTS

James D. Kershner, T-4, and Jack D. Jacobson, T-4, helped with the programming required to reactivate the code. The equilibrium routine was redone earlier in FORTRAN by Paul Bird, L-3.

APPENDIX A

CHEMICAL EQUILIBRIUM EXAMPLE

We give in Table A-I an example of a system with an equilibrium number of phases (solid carbon may be present or absent). The user must specify two systems, a two-phase system and a one-phase system, and make an appropriate choice of independent species for each. He does this, after defining the species and empirical formula via α and Q , by giving the two renumberings a_i^1 and a_i^0 . Recall the definition of a_i : the (original) i th species becomes the a_i th. Take, for example, $i = 4$, $a_4^1 = 1$; CO, originally the fourth species, becomes the first in this the two-phase system. Recall that the solid must be number c in the two-phase system, and number s in the one-phase (where the program assigns it a large F to make its mole fraction negligibly small). The horizontal dashed lines divide the α matrices into independent and dependent parts. The corresponding v and q are given below each α , and the reactions are written out in full below the v 's. The saturation test for the one-phase system is made on the two-phase system reaction



with the saturation index \hat{s} ,

$$\hat{s} = \left(x_{H_2O} / x_C x_{H_2} \right) / K_4 ,$$

evaluated for the mole fractions from the one-phase solution. If $\hat{s} < 1$ the system is unsaturated with respect to deposition of solid carbon, and the one-phase system is the correct choice.

TABLE A-I
EQUILIBRIUM EXAMPLE CH_2O_2 , $c=3$, $s=6$

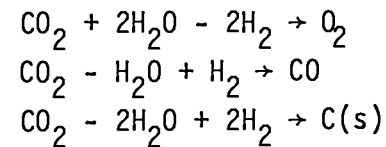
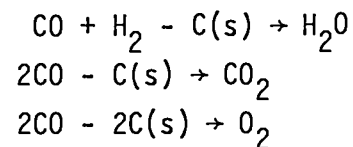
\underline{a} , $\underline{\alpha}$, and \underline{Q} :

		Entry			Two-Phase(p=1)					One-Phase(p=0)				
<u>i</u>		<u>C</u>	<u>H</u>	<u>O</u>	<u>a_i¹</u>		<u>C</u>	<u>H</u>	<u>O</u>	<u>a_i⁰</u>		<u>C</u>	<u>H</u>	<u>O</u>
1	C(s)	1	0	0	3	CO	1	0	1	6	CO ₂	1	0	2
2	H ₂	0	2	0	2	H ₂	0	2	0	3	H ₂ O	0	2	1
3	O ₂	0	0	2	6	C(s)	1	0	0	4	H ₂	0	2	0
4	CO	1	0	1	1	H ₂ O	0	2	1	5	O ₂	0	0	2
5	CO ₂	1	0	2	5	CO ₂	1	0	2	1	CO	1	0	1
6	H ₂ O	0	2	1	4	O ₂	0	0	2	2	C(s)	1	0	0
Q		1	2	2										

\underline{v} and \underline{q} :

\underline{k}		CO	H ₂	C(s)		CO ₂	H ₂ O	H ₂
4	H ₂ O	1	1	-1	O ₂	0	2	-2
5	CO ₂	2	0	-1	CO	1	-1	+7
6	O ₂	2	0	-2	C(s)	1	-2	+2
	\underline{q}	2	1	-1	\underline{q}	1	0	1

Reactions:



APPENDIX B

QUASI-STATIC WORK

Summarized here is what might be loosely termed the Carnot cycle for explosives; plus a numerical example. The object is to calculate the maximum energy that can be extracted quasi-statically from an explosive by detonating it. The quasi-static process is that given by Jacobs.³

Confine the explosive in an upright cylinder of unit length and cross section, closed at the top by a rigid cap and at the bottom by a movable piston. Assume that all confining materials including the piston are rigid massless non-conductors of heat. Move the piston into the cylinder with constant velocity u_1 greater than or equal to the Chapman-Jouguet (CJ) particle velocity. As the piston begins to move, instantaneously initiate the detonation at the piston surface. The detonation front will then move upward with complete-reaction wave velocity D_1 determined by u_1 . The detonation products (reacted material) will be in a uniform state with pressure p_1 and particle velocity u_1 . When the detonation wave reaches the upper end of the cylinder, attach the piston to the cylinder at its position at that instant of time and remove the driving force on the piston. Allow the cylinder to move upward under gravity deceleration until its velocity is reduced to zero. Extract work reversibly from the cylinder of product gases in this position by first lowering it slowly to its original position, and then releasing the piston and allowing the products to expand adiabatically and reversibly to some final pressure.

Calculate the net work done on the surroundings in this process. The cylinder has unit volume and contains ρ_0 grams of material. Take work and energy per unit mass of material. The piston moves a distance u_1/D_1 with force p_1 , so the work W_p done by it is

$$W_p = p_1 u_1 / \rho_0 D_1 \quad ,$$

or, using the conservation relation $p = \rho_0 u_1 D_1$ (neglecting p_0),

$$W_p = u_1^2 \quad .$$

The kinetic energy K of the reaction products is

$$K = u_1^2/2 \quad .$$

The work done by the system in expanding to pressure p is

$$I(p) = \int_{v_1}^{v_i(p)} p_i(v) \, dv \quad ,$$

where $p_i(v)$ is the isentrope through the product state (p_1, v_1) . Summing the contributions gives for the net work $W(p)$ on the surroundings for expansion to pressure p

$$\begin{aligned} W(p) &= -W_p + K + I(p) \\ &= I(p) - \frac{1}{2} u_1^2 \\ &= e_1 - \frac{1}{2} u_1^2 - e_i(p) \quad . \end{aligned}$$

We remark that $W(p_0)$ differs little from the heat of reaction q as conventionally defined -- the energy change in the surroundings for reaction to products at T_0, p_0 . To see this and show how the various energy changes enter, we have prepared Fig. B-1, which shows the closed cycle in the p - v plane, and Table B-I, which lists the steps in clockwise traversal beginning at point 0, the unreacted explosive. The numerical example consists of the calculated values for Comp. B from Ref. 2, and is for $T_0 = 300$ K, $p_0 = 1$ atm. For state 2, the calculated temperature is 518 K and the mean γ is 1.25.

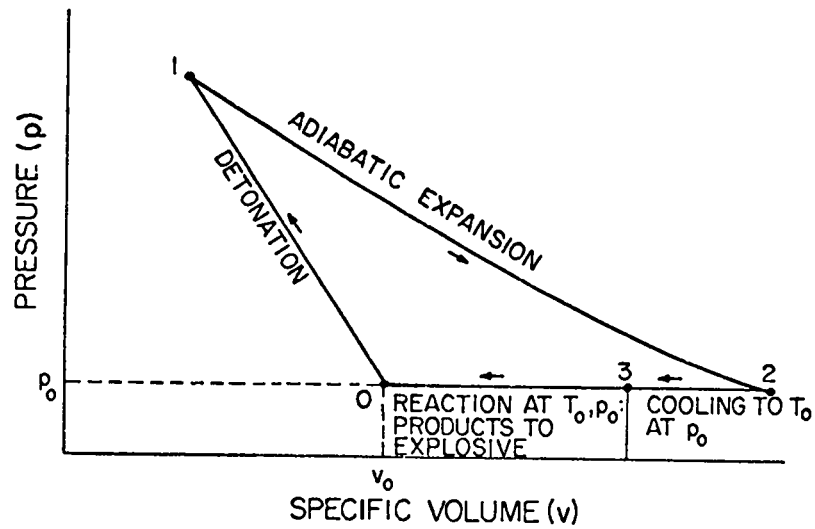


Fig. B-1. Closed cycle of energy changes in the p-v plane.

TABLE B-I

ENERGY STEPS IN CLOCKWISE TRAVERSAL OF FIG. B-1

Process	Energy Change	Comp. B $(\text{mm/s})^2 = \text{Mj/kg}$
Detonation	$e_1 - e_0 = \frac{1}{2} p_1 (v_0 - v_1) = \frac{1}{2} u_1^2$	1.80
Adiabatic expansion	$e_2 - e_1 = -I(p_0)$	-7.56
Cooling at p_0	$e_3 - e_2 = C_p (T_0 - T_2)$	-0.28
Reverse reaction	$e_0 - e_3 = q$	6.04
Thus	$W(p_0) = e_0 - e_2 = q - C_p (T_2 - T_0)$	5.76

APPENDIX C

PROGRAM

I.D. LP-0730

C	AAA	AAA	2
C	CAA	CAA	2
C	MES CONF - WFC-5H-1, DET. PROD. LUN EUS / W. FICKELI, 14	MES0	2
C	*****	MES0	3
C	CONTENTS	MES0	4
C	1. MAIN PROGRAM MES0	MES0	5
C	2. UTILITY	MES0	6
C	3. CALCULATION SECTIONS AND PRINT	MES0	7
C	4. CALCULATION CONTROLS	MES0	8
C	5. HEAD CONTROL (CON)	MES0	9
C	6. OUT OF PLACE	MES0	10
C	ENDS PACKAGE (SEC. 3)	MES0	11
C	HEAD (SEC.2)	MES0	12
C	7. DUMMIES	MES0	13
C		MES0	14
C	*****	MES0	15
C	1. MAIN PROGRAM	MES0	16
C	*****	MES0	17
	PROGRAM MES0(INP, OUT, FSET9=OUT, FSET10=INP	MES0	18
	1. JOIN	MES0	19
	X)	MES0	20
C	***** COMMON *****	MES0	21
2	COMMON / (4000)	MES0	22
2	DIMENSION	MES0	23
	1 BS (60) ,CONT (20)	MES0	24
	2. KON (60)	MES0	25
2	EQUIVALENCE	MES0	26
	1 (Z(400),BS) , (Z(460),CONT)	MES0	27
	2. (Z(1600) , KON)	MES0	28
C	***** LOCAL *****	MES0	29
2	DIMENSION EHS(40),ECOUNT(10)	MES0	30
	DATA EHS/	MES0	31
	1 1H , 2HPS, 4HSAIT, 3HFUB, 1H	MES0	32
	2. 3HPIP, 3HDIS, 3HUTG, 1H , 3HGEF	MES0	33
	3. 3HSEP, 3HTIP, 3HATP, 3HEOP, 1H	MES0	34
	4. 3HSAH, 3HTEU, 2HPV, 2HCU, 4HTEST	MES0	35
	5. 4HCEC, 1H , 4HSPC, 5HSPC1, 1H	MES0	36
	6. 4HCGRE, 4HDBUG, 4HLOAO, 1H , 1H	MES0	37
	7. 1H , 1H , 1H , 4HCKM, 4HRENU	MES0	38
	8. 4HJEND, 1H , 1H , 3HCON, 1H	MES0	39
	*/	MES0	40
C		MES0	41
	DATA ECHIT/	MES0	42
	1 1.98719, 8.31439E-5, 1.01325E-6, 4.184E-2, 0.426012	MES0	43
	2. 3LOUT	MES0	44
	*/	MES0	45
	DATA JOIN /5LJOIN/,OUT /3LOUT/	MES0	46
2	INTEGER OUT	MES0	47
C	***** EXECUTE *****	MES0	48
2	CALL SEPR	MES0	49
3	CALL HEAD (MES0	50
	1 0L*MES1 - 76AUG20*	MES0	51
5	CALL MOVE (EHS,BS,40)	MES0	52
10	CALL MOVE (ECOUNT,CONT,10)	MES0	53
C	--- DATA STATEMENT CANT LOAD BLANK COMMON	MES0	54
C	----- PRINT DECK -----	MES0	55
13	CALL HEAD (5LINPUT)	MES0	56
C	----- HEAD CONTROL -----	MES0	57
15	CALL CON(0.)	MES0	58

17	END	MESO	59
	C*****	MESO	60
	C Z. IIII.JTY	MESO	61
	C*****	MESO	62
	SUBROUTINE DBUG(A,B)	DEBUG	2
	C OLD ERR ROUTINE	DEBUG	3
	C CHANGE DBUG CALLS TO ERR CALLS AS NEEDED	DEBUG	4
6	CALL ERR(A,B,4LPBUG)	DEBUG	5
7	RETURN	DEBUG	6
10	END	DEBUG	7
	SUBROUTINE ERR(ISUB,IMES,ERRM)	ERR	2
	C*****	ERR	3
	C ERROR CONTROL	ERR	4
	C ARGS = ROUTINE, MESSAGE, DATA (10 WORDS)	ERR	5
	C***** COMMONS *****	ERR	6
10	COMMON Z(4000)	ERR	7
10	DIMENSION KUN(60), CONT(20)	ERR	8
10	EQUIVALENCE (Z(440),CONT), (Z(1640),KUN)	ERR	9
10	EQUIVALENCE (CONT(0),OUT), (KUN(6),QERRGAT)	ERR	10
10	COMMON /SFERRC/ SFERRCA(16)	ERR	11
	C***** LOCALS *****	ERR	12
10	DIMENSION ILAB(5)	ERR	13
	DATA ILAB/30H//////// ERROR (ERR CALL) IN - ,1H ,1L	ERR	14
	C***** EXECUTE *****	ERR	15
10	ILAB(2)=ISUB	ERR	16
	C----- 1. CHECK GATE - WARN IF CLOSED	ERR	17
10	IF (QERRGAT.EQ.0.) GOTO 150	ERR	18
12	PRINT 130, ILAB	ERR	19
	130 FORMAT(/// 30X,4(//),* ERR RE-ENTERED FROM ,5A10///)	ERR	20
21	150 QERRGAT = QERRGAT + 1.0	ERR	21
23	IF (QERRGAT.GT. 1.) CALL EXIT	ERR	22
	C----- 2. PRINT HEAD ARGS, ERR -----	ERR	23
26	CALL HEAD (ILAB)	ERR	24
32	CALL PRINT (IMES, 10, ERRM)	ERR	25
36	IF (ISUB.EQ.4LSEERR) CALL UMPPK(OUT,SFERRCA)	ERR	26
44	CALL TRACE	ERR	27
47	CALL ERR (T,ERR)	ERR	28
	C----- 3. TERMINAL LINE -----	ERR	29
51	PRINT 860	ERR	30
	860 FORMAT(///21(5H***),* END OF RUN AFTER ERR* ///)	ERR	31
61	CALL CON(1.)	ERR	32
63	END	ERR	33
	SUBROUTINE ERP(L)	ERP	2
	C DIAGNOSTIC COMMON PRINT	ERP	3
3	COMMON Z(4000)	ERP	4
3	EQUIVALENCE	ERP	5
	1 (Z(920),CAR), (Z(460),CONT), (Z(1000),DER), (Z(1010),EMG)	ERP	6
	2 (Z(1030),EMN), (Z(1170),ENX), (Z(1370),FPU), (Z(1340),FVN)	ERP	7
	3 (Z(1410),FGR), (Z(1450),GUM), (Z(1470),GP), (Z(1540),HE)	ERP	8
	4 (Z(1600),KAL), (Z(1620),KEN), (Z(1680),KIM), (Z(1640),KUN)	ERP	9
	5 (Z(1750),PT), (Z(1800),ROT), (Z(1820),SM), (Z(1840),SP)	ERP	10
	6 (Z(1880),SUC), (Z(1900),SUCG), (Z(1920),THER), (Z(1970),TMO)	ERP	11
	7 (Z(1990),TMS), (Z(2010),IP), (Z(2210),XMT), (Z(2240),XMU)	ERP	12
	8 (Z(2260),XPF), (Z(2660),APG), (Z(3060),XPR), (Z(3080),XPT)	ERP	13

	X=(Z(400),HS),(Z(400),CA),(Z(680),EV),(Z(3100),FLAB)	ENT	14
	Y=(Z(1530),GMT),(Z(900),KEV),(Z(1860),SPC)	ENT	15
3	CALL PRTN(1L,0,0)	ENT	16
6	CALL PRTN(1L,0,0)	ENT	17
11	CALL POUT(1)	ENT	18
13	CALL POUT(2)	ENT	19
15	CALL POUT(3)	ENT	20
17	CALL PRTN(2ALCAH=CC/CH/CM/CG/CS/CE,60,CAR)	ENT	21
22	CALL PRTN(3LDER,10,DER)	ENT	22
25	CALL PRTN(4LCONT,10,CONT)	ENT	23
30	CALL PRTN(3LEMG,10,EMG)	ENT	24
33	CALL PRTN(3LEMN,10,EMN)	ENT	25
36	CALL PRTN(3LEMX,10,EMX)	ENT	26
41	CALL PRTN(3LFMU,10,FMU)	ENT	27
44	CALL PRTN(2LFN,10,FN)	ENT	28
47	CALL PRTN(3LF0B,10,F0B)	ENT	29
52	CALL PRTN(2LGM,30,GM)	ENT	30
55	CALL PRTN(2LGP,10,GP)	ENT	31
60	CALL PRTN(2LHE,10,HE)	ENT	32
63	CALL PRTN(2LBS,50,BS)	ENT	33
66	CALL PRTN(2LEA,80,EA)	ENT	34
71	CALL PRTN(2LEV,10,EV)	ENT	35
74	CALL PRTN(4FLAB,10,FLAB)	ENT	36
77	CALL PRTN(3LGMT,10,GMT)	ENT	37
102	CALL PRTN(3LKEV,10,KEV)	ENT	38
105	CALL PRTN(3LSPC,10,SPC)	ENT	39
110	CALL PRTN(3LKAL,10,KAL)	ENT	40
113	CALL PRTN(3LKON,40,KON)	ENT	41
116	CALL PRTN(3LKEN,20,KEN)	ENT	42
121	CALL PRTN(3LKIM,10,KIM)	ENT	43
124	CALL PRTN(2LPT,10,PT)	ENT	44
127	CALL PRTN(4LRHOT,10,RHOT)	ENT	45
132	CALL PRTN(2LSM,20,SM)	ENT	46
135	CALL PRTN(2LSP,20,SP)	ENT	47
140	CALL PRTN(3LSUC,10,SUC)	ENT	48
143	CALL PRTN(4LSUG,10,SUG)	ENT	49
146	CALL PRTN(4LTHER,10,THER)	ENT	50
151	CALL PRTN(3LTMG,10,TMG)	ENT	51
154	CALL PRTN(3LTMS,20,TMS)	ENT	52
157	CALL PRTN(2LTP,40,TP)	ENT	53
162	CALL PRTN(3LXMT,20,XMT)	ENT	54
165	CALL PRTN(3LXMU,10,XMU)	ENT	55
170	CALL PRTN(3LXPF,10,XPF)	ENT	56
173	CALL PRTN(3LXPG,10,XPG)	ENT	57
176	CALL PRTN(3LXPR,10,XPR)	ENT	58
201	CALL PRTN(3LXPT,10,XPT)	ENT	59
204	RETURN	ENT	60
205	END	ENT	61

	SUBROUTINE FIO (H,FMT,N,A,KL)	FIG	2
C		FIG	3
C	H=HEAD,MIT,PRINT,MU!	FIG	4
C	FMT=FORMAT	FIG	5
C	N=NUMBER OF WORDS OF ARRAY A FOR I.O.	FIG	6
C	FOR N=0,FMT IS HOLLERITH ARGUMENT LABEL	FIG	7
C	,KL IS THE WORD LENGTH OF THE LABEL.	FIG	8
14	DIMENSION BS(4),FMT(60),A(10)	FIG	9
14	INTEGER H,FMT,BS	FIG	10
C		FIG	11

C	BS(1)=READ , BS(2)=KIT	FIG	12
C	BS(3)=PRINT , BS(4)=WUT	FIG	13
14	BS(1)=4=READ	FIG	14
14	BS(2)=3=KIT	FIG	15
14	BS(3)=5=PRINT	FIG	16
14	BS(4)=3=WUT	FIG	17
C		FIG	18
21	DO 24 J=1.4	FIG	19
23	I=J	FIG	20
23	IF (H.EQ.BS(I))GO TO 30	FIG	21
26	24 CONTINUE	FIG	22
30	WRITE(9,26)H	FIG	23
26	FORMAT (1BH0 F10 -BAO ARG= A6)	FIG	24
40	CALL EXIT(3)	FIG	25
45	30 IF (N1200,100,200	FIG	26
C	I.O. *ITH NU DATA	FIG	27
46	100 GO TO (500,500,130,140),1	FIG	28
C		FIG	29
C		FIG	30
56	130 WRITE (2,150) (FMT(J),J=1,KL)	FIG	31
67	GO TO 500	FIG	32
C		FIG	33
C		FIG	34
73	140 WRITE (9,150) (FMT(J),J=1,KL)	FIG	35
104	GO TO 500	FIG	36
150	FORMAT (12A6)	FIG	37
C	I.O. WITH DATA	FIG	38
110	200 GO TO (210,220,230,240),1	FIG	39
C		FIG	40
120	210 READ (2,FMT) (A(J),J=1,N)	FIG	41
132	GO TO 500	FIG	42
C		FIG	43
136	220 READ(10,FMT) (A(J),J=1,N)	FIG	44
150	GO TO 500	FIG	45
C		FIG	46
154	230 WRITE (2,FMT) (A(J),J=1,N)	FIG	47
166	GO TO 500	FIG	48
C		FIG	49
172	240 WRITE(9,FMT) (A(J),J=1,N)	FIG	50
204	GO TO 500	FIG	51
C		FIG	52
210	500 CONTINUE	FIG	53
210	510 CONTINUE	FIG	54
210	520 RETURN	FIG	55
211	END	FIG	56
C	SUBROUTINE FROOTT(C,K)	FROOTT	2
C	FROOT FUNCTION TABULATOR	FROOTT	3
C		FROOTT	4
C	C - FROOT ARG ARRAY	FROOTT	5
C	C(5) - X0	FROOTT	6
C	C(6) - DELTA X	FROOTT	7
C	C(7) - XN	FROOTT	8
C		FROOTT	9
C	FOR K=0,ITERATE	FROOTT	10
C	FOR K=1,TABULATE. PROVIDE FROOT WITH VALUES	FROOTT	11
C	X0,X0+DELTA X,...,XN,THEN EXIT	FROOTT	12
C		FROOTT	13
6	EQUIVALENCE (E1,KC1),(E2,KC2)	FROOTT	14

6	DIMENSION C(10)	FRUUTT	15
8	E1=C(8)	FRUUTT	16
10	E2=C(9)	FRUUTT	17
12	10 IF (K)50,20,50	FRUUTT	18
13	20 CALL FRUIT (C)	FRUUTT	19
17	30 GO TO 210	FRUUTT	20
20	50 IF (K1)100,60,100	FRUUTT	21
21	60 C(2)=C(5)	FRUUTT	22
23	70 GO TO 102	FRUUTT	23
24	100 C(2)=C(2)+C(6)	FRUUTT	24
26	102 K1=K1+1	FRUUTT	25
30	110 IF ((C(2)-C(7))*C(6)) 150,150,120	FRUUTT	26
34	120 K2=1	FRUUTT	27
35	130 GO TO 200	FRUUTT	28
36	150 K2=2	FRUUTT	29
37	200 C(8)=E1	FRUUTT	30
41	202 C(9)=E2	FRUUTT	31
43	210 RETURN	FRUUTT	32
44	END	FRUUTT	33
C*****		GEP	2
C*	3. CALCULATION SECTIONS	* GEP	3
C*****		GEP	4
SUBROUTINE GEP(K)		GEP	5
C K=1 - CALCULATE PURE GAS EOS AT GIVEN T,P		GEP	6
C K=2 - APPROXIMATE SAME BY LM EXPANSION		GEP	7
C CALLED BY XIM		GEP	8
C-----SPECS-----		GEP	9
C K=1		GEP	10
C REGULAR CALCULATION OF GAS EOS FOR PURE		GEP	11
C SPECIES AT GIVEN T,P BY ITERATIVE SOLUTION		GEP	12
C OF P(T,V)=P, WITH P(T,V) GIVEN BY GEM.		GEP	13
C FOR CS OR 1-FLUID MIX, THIS CAN BE A MIXTURE		GEP	14
C EOS VIA COMPOSITION DEPENDENCE OF THE		GEP	15
C MEAN RSTAR AND TSTAR.		GEP	16
C INPUT		GEP	17
C P=TEMP(1)		GEP	18
C IMPLICIT FOR GEM -		GEP	19
C T=TEMP(1)		GEP	20
C MEAN RSTAR, TSTAR = RSTAR=GP(5), TSTAR=GP(6)		GEP	21
C KAL(5) = 1,2,3 FOR IDEAL,LJD, KW		GEP	22
C OUTPUT		GEP	23
C V=VR=GM(15) - VOLUME		GEP	24
C IMPLICIT FROM GEM -		GEP	25
C ISM - STATE POINT		GEP	26
C		GEP	27
C VARIABLES		GEP	28
C PG=GM(16) - CALCULATED (GAS) PRESSURE		GEP	29
C VRL, VRU - LOWER AND UPPER LIMITS ON ITERATION V		GEP	30
C ROUTINES		GEP	31
C GEM(2) - PURE-FLUID EOS AT T,P		GEP	32
C FRUIT - ITERATE		GEP	33
C PLAN		GEP	34
C SOLVE ITERATIVELY PG(V,T)=P FOR V(=VR) BY		GEP	35
C FROOT ITERATION.		GEP	36
C VARIABLE, FUNCTION = LOG(V), LOG(P/PG)		GEP	37
C SECOND GUESS - NEWTON-RAPHSON FROM DP/DV=GM(12)		GEP	38
C K=2		GEP	39
C INPUT		GEP	40

C	I,P=THEM(1),(3)	GET	41
C	GM = STATE POINT FROM PREVIOUS K=1 CALCULATION	GET	42
C	(GEN(2) OUTPUT)	GET	43
C	EMX(2,...) = (GAS) MOLE FRACTIONS	GET	44
C	OL)PUT	GET	45
C	AMT = MIXTURE STATE POINT	GET	46
C	(NOTE = CHEMICAL POTENTIALS IN XMU ARE	GET	47
C	CALCULATED BY CALLER)	GET	48
C	VARIABLES	GET	49
C	EV = 1,2 = TSTAR AND RSTAR DISPLACEMENTS	GET	50
C	3,5 = EXPANSION COEFFICIENTS	GET	51
3	COMMON Z(4000)	GET	52
3	DIMENSION	GET	53
	1 CAR (80) ,CONT (20) ,EV (20)	GET	54
	2,FOH (40) ,GM (40) ,KEN (60)	GET	55
	3,KON (4,10) ,THER (50) ,AMT (30)	GET	56
	4,GP(20)	GET	57
3	EQUIVALENCE	GET	58
	1 (Z(921),CAR) ,(Z(460),CONT) ,(Z(680),EV)	GET	59
	2,(Z(1410),FOH) ,(Z(1490),GM) ,(Z(1620),KEN)	GET	60
	3,(Z(1690),KON) ,(Z(1920),THER) ,(Z(2210),AMT)	GET	61
	4,(Z(1470),GP)	GET	62
3	DIMENSION CG(10),KCG(2)	GET	63
C		GET	64
3	EQUIVALENCE	GET	65
	1 (CAR(31),CG),(CG(4),KCG)	GET	66
	2,(CONT(2),R)	GET	67
	3,(FOH(24),VRU),(FOH(19),VRL)	GET	68
	4,(GM(15),VR),(GM(10),PG)	GET	69
	5,(THEM(1),P),(THEM(3),T)	GET	70
	6,(GP(5),RSTA),(GP(6),TSTA)	GET	71
	7,(XMI(16),RSTAT),(AMT(17),TSTAT)	GET	72
C		GET	73
C		GET	74
3	4 GO TO (10,300) , K	GET	75
C	----- K=1 - REGULAR -----	GET	76
11	10 IF (VR) 20,12,50	GET	77
12	12 VR=10.0	GET	78
14	20 CG(4)=ALOG(VR)	GET	79
20	22 CALL COUT (3HGEF,1)	GET	80
24	40 KCG(1)=0	GET	81
C		GET	82
25	50 CALL FROTT (CG,KON(4,8))	GET	83
31	52 KEXIT=KCH(2)	GET	84
33	60 GO TO (150,80,80,70),KEXIT	GET	85
42	70 CALL DBMS (3HGEF,1)	GET	86
47	72 GO TO 150	GET	87
50	80 CALL CBMS (3HGEF,2)	GET	88
54	82 GO TO 150	GET	89
55	88 IF (KON(4,8)) 92,90,92	GET	90
55	90 IF (KCG(1)-2) 92,91,92	GET	91
60	91 CG(2)=CG(4)-CG(3)*PG/(VR*GM(12))	GET	92
65	92 VR= EXP(CG(2))	GET	93
71	93 IF (VRU=VR) 94,94,96	GET	94
74	94 VR=VRU	GET	95
76	95 GO TO 90	GET	96
77	96 IF (VR=VRL) 97,97,98	GET	97
102	97 VR=VRL	GET	98
104	98 KEN(11)=KEN(11)+1	GET	99
		GET	100

106	100 CALL GEP(2)	GEF	101		
111	105 IF (PG) GO TO 110,110	GEF	102		
113	106 IF (VRL-VR/3.) 107,97,97	GEF	103		
117	107 VR=VR/3.	GEF	104		
121	108 GO TO 100	GEF	105		
122	110 CG(3)=ALOG(PG/P)	GEF	106		
130	112 CG(2)=ALOG(VR)	GEF	107		
134	120 CALL DOUT (JHGEF,2)	GEF	108		
140	130 GO TO 50	GEF	109		
141	150 CALL DOUT (JHGEF,3)	GEF	110		
145	160 GO TO 600	GEF	111		
C----- K=2 - LM EXPANSION -----					
146	300 EV(1)=TSTAT/TSTA-1.0	GEF	112		
151	310 EV(2)=RSTAT/RSTA-1.0	GEF	113		
C	400	GEF	114		
C	410 E	GEF	115		
		COMPUTE THERMO OUTPUT			
154	412 EV(3)=GM(4)*EV(1)+3.0*GM(10)*EV(2)	GEF	116		
161	420 EV(4)=-((GM(14)+P/GM(12))*EV(1)	GEF	117		
	1	+.0*(GM(15)+P/GM(12))*EV(2)	118		
172	430 EV(5)=(GM(8)+(T*GM(13)-P)*(GM(14)/H))*EV(1)	GEF	119		
	1	+.0*(P*GM(14)/H-1.0)*EV(2)	120		
206	500 XMT(1)=GM(15)+EV(4)	GEF	121		
210	510 XMT(2)=GM(4)+EV(3)-(P/(H*T))*EV(4)-EV(5)	GEF	122		
217	520 XMT(7)=P*XMT(1)/(H*T)-1.0	GEF	123		
224	530 XMT(3)=XMT(2)+XMT(7)	GEF	124		
225	540 XMT(5)=GM(5)+EV(3)	GEF	125		
231	550 XMT(4)=XMT(5)-XMT(7)	GEF	126		
232	560 XMT(6)=GM(11)-EV(5)	GEF	127		
234	570 XMT(8)=XMT(1)-XMT/P	GEF	128		
C	580 U	GEF	129		
C		GEF	130		
240	590 CALL DOUT (JHGEF,4)	GEF	131		
C		GEF	132		
244	600 RETURN	GEF	133		
C		GEF	134		
C	SPECS (FOR PART 2)	GEF	135		
C		GEF	136		
C	IN	OUT	ERASE		
C			GEF	137	
C	NOTE - Z=PV/RT		GEF	138	
C	1.0		GEF	139	
C	EMX		GEF	140	
C	GM		GEF	141	
C	1	XMT 1 VG	EV 1 F=1	GEF	142
C	2	2 ERP/RT	2 B=1	GEF	143
C	3	3 MGP/RT	3 FGP	GEF	144
C	4 ERP/RT	4 AGP/RT	4 U F/DP	GEF	145
C	5 FRP/RT	5 FGP/RT	5 U F/U RT	GEF	146
C	6	6 SGP/H		GEF	147
C	7	7 ZGP		GEF	148
C	8 U ERP/U RT	8 VGP		GEF	149
C	10 ZGP			GEF	150
C	11 SRP/H			GEF	151
C	12 U P/U VR			GEF	152
C	13 U P/U I			GEF	153
C	14 U VR/U T			GEF	154
C	15 VR			GEF	155
C	16			GEF	156
C	17	XMT MUGP/RT		GEF	157
C				GEF	158
C				GEF	159
C				GEF	160


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SUBROUTINE GEM (K)
C PURE GAS EOS AT GIVEN T,V
C -----
C K=1 PRELIM. READ INPUT PACKS AND FOR LJO
C CALL GES (1,...) FOR PRELIMINARY PROCESSING (SETS UP GP).
C CALLED BY CGW
C K=2: MAIN. CALCULATE STATE POINT; KAL(3)=
C 0 - IDEAL GAS; LOCAL
C 9 - KW EOS; CALL HKW
C OTHER - LJO MUST CALL GES(2,...)
C -----
C MAIN (K=2) SPECS
C INPUT
C T=THER(3)
C V=VR=GM(15)
C ISTAVSTA=GP(6),(7) - TSTA, VSTA. THESE ARE
C COMPOSITION DEPENDENT FOR LM AND 1-FLUID MIX.
C KAL(3) - EOS CHOICE. SEE ABOVE
C OUTPUT
C GM - STATE POINT. GM IS REARRANGED AND
C FILLER OUT HERE.
C NOTES
C 1. NO IDEAL-GAS BRANCH IN PRELIM FOR THIS
C CASE; GEP PACK SHOULD NOT BE ENTERED.
C 2. PACK LOGICAL ORGANIZATION: HKW WAS ADDED
C LATE WITH BRANCH UNDER LJO. IDEAL
C GAS, KW, AND LJO SHOULD ALL HAVE SAME LEVEL.
C 3. I DO NOT NOW (WT 1/75) UNDERSTAND WHY
C TMS (IDEAL PART) IS USED IN CPM. IT SEEMS TO
C ME IT SHOULD BE AN
C IMPERFECTION QUANTITY LIKE THE OTHERS,
C ***** COMMONS *****
3 COMMON /4000/
3 DIMENSION
3 1 CONT ( 20) ,GP ( 20) ,GM ( 40)
3 2,KAL ( 20) ,KEN ( 6,10) ,KUN ( 6,10)
3 3,THER ( 50) ,TMS ( 20)
3 DIMENSION KE(6)
3 EQUIVALENCE
3 1 (7( 460),CONT ) ,(2( 1470),GP ) ,(2( 1490),GM )
3 2,(7( 1500),KAL ) ,(2( 1520),KEN ) ,(2( 1590),KUN )
3 3,(2( 1920),THER ) ,(2( 1990),TMS )
C
C LOCAL EQ
C
3 EQUIVALENCE (GP(6),TSTA),(GP(7),VSTA)
3 1 ,(GM(1),TAU),(GM(2),THEIA),(GM(16),PG)
3 2 ,(THER(3),T),(CONT( ),K)
3 3 ,(GM(15),VR)
C
3 EQUIVALENCE (GM(25),GAM),(GM(26),ALPH),(GM(27),BET)
3 1 ,(GM(28),CGAM),(GM(29),CPH),(GM(30),ULVUT)
C
C
3 100 GO TO (1000,2000),K
C 994
C 996 PRELIMINARY

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GEM 2
GEM 3
GEM 4
GEM 5
GEM 6
GEM 7
GEM 8
GEM 9
GEM 10
GEM 11
GEM 12
GEM 13
GEM 14
GEM 15
GEM 16
GEM 17
GEM 18
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GEM 49
GEM 50
GEM 51
GEM 52
GEM 53
GEM 54
GEM 55
GEM 56
GEM 57
GEM 58

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	C 998		GEN	59
11	1000 CALL REAP (GEN	60
	1 1000 POT (1-LJ,2-MCM,3-MK) ,W (NUM I) / N,M,AN,AM,R*,T*,S		GEN	61
	1 1000 KE)		GEN	62
14	CALL REAP(0,6,GP)		GEN	63
20	1010 KE(1)=0		GEN	64
21	1012 KE(4)=0		GEN	65
22	1020 KE (5)=KON(1,4)		GEN	66
24	1022 KE (6)=KON(2,4)		GEN	67
26	1024 IF (KE(1)-9) 1030,1025,1030		GEN	68
30	1025 KAL(3)=9		GEN	69
31	1026 VSTA=1.0		GEN	70
33	1027 TSTA=1.0		GEN	71
35	1028 GO TO 3000		GEN	72
36	1030 CALL GES(1,KE,GP,GM)		GEN	73
43	1040 CALL PRIN(4RV*5 ,1,VSTA)		GEN	74
47	1050 KAL(1)=1		GEN	75
50	1060 GO TO 3000		GEN	76
	C1094		GEN	77
	C1096	MAIN	GEN	78
	C1098		GEN	79
51	2000 KEN(1)=KEN(1)+1		GEN	80
53	2002 E1 = V0		GEN	81
	C2004		GEN	82
	C2006	IDEAL	GEN	83
55	2010 IF (KAL(3)) 2200,2050,2200		GEN	84
56	2050 DO 2060 I=3,15		GEN	85
63	2060 GM(1)=0.0		GEN	86
65	2070 GM(3)=1.0		GEN	87
67	2080 GM(4)=1.0		GEN	88
71	2090 GM(14)=1.0		GEN	89
73	2100 GO TO 2300		GEN	90
	C2194		GEN	91
	C2196	LJD	GEN	92
74	2200 TA)=VR/VSTA		GEN	93
76	2210 THETA=T/TSTA		GEN	94
100	2220 KE(5)=KON(1,4)		GEN	95
102	2230 KE(6)=KON(2,4)		GEN	96
	C		GEN	97
104	2234 IF (KAL(3)-9) 2240,2236,2240	KW	GEN	98
106	2236 CALL HKW(1)		GEN	99
111	2238 GO TO 2300		GEN	100
	C		GEN	101
112	2240 CALL GES (2,KE,GP,GM)		GEN	102
	C	REARRANGE AND FINISH GM	GEN	103
117	2300 GM(22)=GM(15)		GEN	104
121	2310 GM(21)=GM(14)		GEN	105
123	2320 GM(20)=GM(6)		GEN	106
125	2330 GM(19)=GM(13)		GEN	107
127	2340 GM(18)=GM(12)		GEN	108
131	2350 GM(17)=GM(5)		GEN	109
133	2352 VR = E1		GEN	110
135	2360 PG=GM(3)*R*T/VR		GEN	111
141	2370 GM(15)=VR		GEN	112
143	2380 GM(12)=(R*T/VR**2)*(GM(10)-GM(3))		GEN	113
150	2390 GM(13)=(2/VR)*GM(9)		GEN	114
153	2400 GM(14)=-GM(13)/GM(12)		GEN	115
155	2410 E1=GM(11)		GEN	116
157	2412 E2=GM(7)		GEN	117
161	2420 GM(11)=GM(8)		GEN	118

163	2430	GM(7)=GM(10)	GEH	119
165	2440	GM(8)=GM(9)	GEH	120
167	2450	GM(11)=GM(3)-1.0	GEH	121
172	2460	GM(9)=VR-K*T/PG	GEH	122
176	2470	GM(8)=E1	GEH	123
210	2490	GM(5)=E2	GEH	124
	C2496		GEH	125
202	2500	KEN(1,4)=KE(3)	GEH	126
204	2510	KEN(2,4)=KE(4)	GEH	127
	C		GEH	128
216	2514	CGAM=-VR*GM(12)/PG	GEH	129
211	2520	CVR=IMS(7)-1.0*GM(8)	GEH	130
215	2524	ULV1:=GM(14)/VR	GEH	131
217	2530	GAM=CGAM*(1.0+CGAM*GM(3) * (1*ULV1)*2/CVM)	GEH	132
225	2534	HET=1.0/(CGAM*GM(3) * T*ULV1/CVM)	GEH	133
232	2540	ALPH=GAM*HET-1.0	GEH	134
235	2544	CPR=CVR*GAM/CGAM	GEH	135
	C2544		GEH	136
240	2600	CALL DOUT (3HGEH,1)	GEH	137
	C2544		GEH	138
244	3000	RETURN	GEH	139
245		END)	GEH	140

		SUBROUTINE GES (K,L,GP,GM)	GES	2
C			GES	3
C		LJD CELL THEORY GAS EQU. STATE SUBROUTINE	GES	4
C			GES	5
C		REVISION 1. CORRECT MINOR ERROR =	GES	6
C		POINTS 14 AND 16 USE A FOR 13 AND 15	GES	7
C		W. F. 1/5/62	GES	8
C			GES	9
C		REVISION 2. CHANGE OBS. CALL ON NEG. KAP PRINT	GES	10
C		W. F. 2/26/62	GES	11
C			GES	12
C			GES	13
12	10	DIMENSION A(8),Y(4),S(7),W(5),W1(5),W2(5),	GES	14
	1	C(4),GM(15),G(15),UP(7),L(6),E(10)	GES	15
12		EQUIVALENCE (G(1),[AU]),(G(2),[META]),(G(15),B),(W,X)	GES	16
C	96		GES	17
C	98	PHEL.-MAIN BRANCH	GES	18
12	100	GO TO (200,1000),K	GES	19
20	200	Y(1)=0.94940693	GES	20
22	202	Y(2)=0.94457502	GES	21
24	204	Y(3)=0.85663120	GES	22
26	206	Y(4)=0.75541641	GES	23
30	208	Y(5)=0.61787624	GES	24
32	210	Y(6)=0.45001678	GES	25
34	212	Y(7)=0.24164355	GES	26
36	214	Y(8)=0.045012510	GES	27
40	220	A(1)=0.027152459	GES	28
42	222	A(2)=0.062253524	GES	29
44	224	A(3)=0.035158512	GES	30
46	226	A(4)=0.12462897	GES	31
50	228	A(5)=0.14959599	GES	32
52	230	A(6)=0.16015652	GES	33
54	232	A(7)=0.18260342	GES	34
56	234	A(8)=0.18945061	GES	35
60	240	u=0.276335	GES	36
62	242	BMAX=0.276335	GES	37

64	244	BUP=1.0667420	GES	38
66	246	BDHWN=0.97778543	GES	39
70	248	EPS=18.0	GES	40
72	250	GP(7)=0.426012*GP(5)**3	GES	41
75	300	CALL WR(1,L,GP)	GES	42
102	310	GO TO 5000	GES	43
	C 990		GES	44
	C 992	MAIN ENTRY	GES	45
	C 994	INITIAL	GES	46
103	1000	TAU=GM(1)	GES	47
104	1010	THETA=GM(2)	GES	48
106	1012	L(3)=L(3)+1	GES	49
110	1020	IF (TAU) 1040,1040,1030	GES	50
112	1030	IF (THETA) 1040,1040,1050	GES	51
114	1040	CALL DHUB(3HGES,1)	GES	52
122	1050	CH(1)=TAU	GES	53
124	1060	CALL WR(2,L,CH)	GES	54
132	1070	KE1=0	GES	55
133	1080	IF (L(5)) 4000,1200,4000	GES	56
	C1190	FIND LIMIT	GES	57
134	1200	W1=H*(1.0+Y(1))	GES	58
137	1210	CALL WR(3,L,W1)	GES	59
145	1220	IF ((W1(3)-ABS(CH(2)))/THETA-EPS) 1400,1400,1250	GES	60
	C1238		GES	61
	C1240	CHECK AND LOWER	GES	62
153	1250	W2=H*(1.0+Y(3))	GES	63
156	1260	CALL WR(3,L,W2)	GES	64
164	1270	IF ((W2(3)-ABS(CH(2)))/THETA-EPS) 1600,1600,1300	GES	65
172	1300	KE1=KE1+1	GES	66
174	1310	DO 1320 I=1,5	GES	67
201	1320	W1(I)=W2(I)	GES	68
205	1330	B=RHUBDWN	GES	69
207	1340	IF (L(5)) 4100,1250,4100	GES	70
	C1394		GES	71
	C1396	RAISE	GES	72
211	1400	IF (B-BMAX) 1450,1410,1410	GES	73
214	1410	W2=H*(1.0+Y(3))	GES	74
217	1420	CALL WR(3,L,W2)	GES	75
225	1430	GO TO 1600	GES	76
226	1450	DO 1460 I=1,5	GES	77
233	1460	W2(I)=W1(I)	GES	78
237	1470	B=H*BUP	GES	79
241	1472	IF (L(5)) 4150,1474,4150	GES	80
242	1474	KE1=KE1+1	GES	81
244	1480	IF (B-BMAX) 1520,1520,1490	GES	82
247	1490	B=BMAX	GES	83
251	1500	W2=H*(1.0+Y(3))	GES	84
254	1510	CALL WR(3,L,W2)	GES	85
262	1520	W1=H*(1.0+Y(1))	GES	86
265	1530	CALL WR(3,L,W1)	GES	87
273	1540	IF ((W1(3)-ABS(CH(2)))/THETA-EPS) 1550,1600,1600	GES	88
301	1550	IF (B-BMAX) 1450,1600,1600	GES	89
	C1596	FINISH	GES	90
302	1600	KE2=KE1*KE2	GES	91
306	1610	L(4)=KE2/L(3)	GES	92
	C1096		GES	93
	C1098	INTEGRATE	GES	94
312	2000	DO 2010 I=1,7	GES	95
317	2010	S(I)=0.0	GES	96
	C2048		GES	97

567	3160	G(7)=G(6)+G(3)-1.0	GES	158
573	3170	G(8)=G(4)-G(6)	GES	159
	C		GES	160
575	3200	DO 3210 I=3,15	GES	161
602	3210	GM(I)=G(I)	GES	162
606	3220	IF(L(5)) 4300,5000,4300	GES	163
	C3954		GES	164
	C3956	DIAGNOSTIC PRINT	GES	165
	C3958		GES	166
610	4000	CALL PRIM (28H GES DIAG. -TAU,THEIA,B S,0,B)	GES	167
616	4010	E(1)=TAU	GES	168
620	4020	E(2)=THETA	GES	169
622	4030	E(3)=B	GES	170
624	4040	CALL PRIM (2H S,3,E)	GES	171
632	4050	GO TO 1200	GES	172
633	4100	CALL PRIM (2HRS,1,B)	GES	173
641	4110	GO TO 1250	GES	174
642	4150	CALL PRIM (2HRS,1,B)	GES	175
650	4160	GO TO 1474	GES	176
651	4200	DO 4210 I=1,7	GES	177
661	4210	E(I)=E(I)/A(KE)	GES	178
665	4220	E(8)=1G	GES	179
667	4230	E(9)=X	GES	180
671	4240	E(10)=W(3)	GES	181
673	4250	CALL PRIM(7MI,X,W S,3,E(8))	GES	182
700		CALL PRIM(7MINTS S,7,E)	GES	183
706	4260	GO TO 2550	GES	184
707	4300	CALL PRIM(7MG(OUT)S,15,G)	GES	185
712		CALL PRIM(7MS(INT)S,S)	GES	186
	C4950		GES	187
717	5000	RETURN	GES	188
720		END	GES	189

		SUBROUTINE WR(K,L,D)	WR	2
	C	GES CELL POTENTIAL	WR	3
10	20	DIMENSION CC(6),C(6),WN(6),WC(6),W(6)	WR	4
	1	,KFPS(2),NMAX(2),F(5),A(60),AL(30),D(7),L(6)	WR	5
10	30	EQUIVALENCE (WN,CC(7)),(KUNE,UNE),(KY,Y)	WR	6
	1	, (A(31),AL)	WR	7
10	200	GO TO (1000,2000,3000),K	WR	8
	C 990		WR	9
	C 994	PRELIM. ENTRY	WR	10
	C 996		WR	11
	C 998	SET POT. AND EQUIV. ANGS	WR	12
17	1000	DO 1004 I=1,6	WR	13
21	1002	W(I)=0.0	WR	14
23	1004	C(I)=0.0	WR	15
25	1006	M=30	WR	16
26	1010	GO TO (1020,1040,1060),L	WR	17
35	1020	KA=1	WR	18
36	1022	KR=1	WR	19
37	1030	GO TO 1100	WR	20
40	1040	KA=2	WR	21
41	1042	KR=2	WR	22
42	1050	GO TO 1100	WR	23
43	1060	KA=1	WR	24
44	1062	KR=2	WR	25
	C1070		WR	26
	C		WR	27

45	1100	FN=0(1)	W	28
46	1110	FM=0(2)	W	29
50	1120	AN=0(3)	W	30
52	1130	AM=0(4)	W	31
	C1140		W	32
	C1144		W	33
54	1200	IF (AN) 1400,1800,1210	W	34
	C		W	35
56	1210	G=FN	W	36
60	1212	GB=FM	W	37
62	1220	AG=AN	W	38
64	1230	KB=KR	W	39
66	1240	KQ=1	W	40
	C1240		W	41
	C1244		W	42
67	1300	BB= 12.0*GB/(FN-FM)	W	43
73	1310	AA=-AG*BB/2.0	W	44
	C1320		W	45
76	1330	GO TO (1350,1650),KB	W	46
	C1344		W	47
	C1348		W	48
104	1350	J=(KQ-1)*M	W	49
110	1352	KE1=J*M	W	50
112	1360	A(KE1)=G*(G-1.0)/6.0	W	51
117	1370	E=A(KE1)/4.0	W	52
122	1380	E1=1.0E-7*E	W	53
	C1384		W	54
124	1400	UC 1480 I=2,M	W	55
126	1410	KE=KE1+1-I	W	56
131	1420	E2=2*(I-1)	W	57
134	1440	E3=(G+FB)*((G+E2)-1.0)/((E2+3.0)*(E2+2.0))	W	58
144	1450	A(KE)=E3*A(KE+1)	W	59
147	1460	E=E3*E/4.0	W	60
152	1470	IF (E1-E) 1480,1480,1510	W	61
155	1480	CONTINUE	W	62
	C1488		W	63
160	1500	CALL FIO (3*WOT,	W	64
		1 53H (140,12X,32H A=DIM. TOO SMALL+ A30*1/4*30= 1PE15.7),	W	65
		21,A(J+1),0)	W	66
	C1508		W	67
171	1510	WMAX(KQ)=I	W	68
173	1520	KEPS(KQ)=-ALOG(1.0E-7*A(KE1)/A(KE))/0.6931	W	69
	C1544		W	70
206	1550	J=(KJ-1)*3	W	71
211	1560	CC(J+1)=AA	W	72
213	1570	CC(J+2)=-AA*G/3.0	W	73
217	1580	CC(J+3)=-CC(J+2)*G/3.0	W	74
223	1590	WN(J+1)=BB	W	75
225	1600	WN(J+2)=-WB*G/3.0	W	76
231	1610	WN(J+3)=-WN(J+2)*G/3.0	W	77
235	1620	GO TO 1750	W	78
	C1644		W	79
	C1646		W	80
236	1650	J=(KJ-1)*3	W	81
241	1660	CC(J+1)=AA	W	82
243	1670	CC(J+2)=-AA/3.0	W	83
246	1680	CC(J+3)=AA/9.0	W	84
251	1690	WN(J+1)=BB	W	85
253	1700	WN(J+2)=WB /3.0	W	86
256	1710	WN(J+3)=WB /9.0	W	87

	C1746		WH	88
261	1750	GO TO (1400,1900),KQ	WH	89
	C1796		WH	90
	C1798	ATTRACTIVE PART	WH	91
267	1800	IF (AM) 5000,5000,1810	WH	92
271	1810	G=FM	WH	93
273	1812	GB=FM	WH	94
275	1820	AG=AM	WH	95
277	1830	KB=KA	WH	96
301	1840	KQ=2	WH	97
302	1850	GO TO 1300	WH	98
	C1894		WH	99
303	1900	IF (L(6))4000,5000,4000	WH	100
	C1990		WH	101
	C1992		WH	102
	C1994	MAIN INITIAL ENTRY	WH	103
	C1996		WH	104
	C1998	REPULSIVE PART	WH	105
305	2000	IF (AN) 2500,2500,2010	WH	106
307	2010	G=FM	WH	107
311	2020	KB=KA	WH	108
313	2030	KQ=1	WH	109
	C2044		WH	110
	C2046	CALC.	WH	111
314	2050	GO TO (2060,2150),KB	WH	112
	C2054		WH	113
	C2058	LJ	WH	114
322	2060	E=N(1)*(-G/3.0)	WH	115
327	2070	J=(KQ-1)*3	WH	116
332	2080	DO 2110 I=1,3	WH	117
334	2090	KE=J+I	WH	118
336	2100	C(KI)=CC(KE)*E	WH	119
341	2110	*C(KE)=WN(KE)*E	WH	120
344	2120	GO TO 2450	WH	121
	C2144		WH	122
	C2146	EXP	WH	123
345	2130	I=D(1)*0.33333333	WH	124
	C2176		WH	125
351	2180	S=G*T	WH	126
353	2190	E=EXP(G-S)	WH	127
362	2200	J=(KQ-1)*3	WH	128
365	2210	DO 2240 I=1,3	WH	129
367	2220	KE=I+J	WH	130
371	2230	C(KI)=CC(KE)*E	WH	131
374	2240	*C(KE)=WN(KE)*E	WH	132
377	2250	C(J+2)=C(J+2)*S	WH	133
402	2260	C(J+3)=C(J+3)*(S*S-S)	WH	134
	C2296		WH	135
406	2300	J=(KQ-1)*4	WH	136
412	2310	A(1)=S	WH	137
414	2320	S1=1.0/S	WH	138
416	2330	A(J+2)=S1	WH	139
420	2340	A(J+3)=1.0*S1	WH	140
423	2350	A(1+4)=-(S+2.0+2.0*S1)	WH	141
430	2360	A(1+5)=2.0*(1.0+S1)	WH	142
435	2370	A(1+6)=S*S+2.0*S+4.0+4.0*S1	WH	143
444	2380	A(J+7)=2.0+3.0*S	WH	144
450	2390	A(J+8)=-(3.0*S+4.0+4.0*S1)	WH	145
456	2400	A(J+9)=S-S*S	WH	146
	C2444		WH	147

461	2450	GO TO (2400,2600),KQ	WH	148
	C2444		WH	149
	C2446		WH	150
		ATTRACTIVE PART	WH	151
467	2500	IF (AM) 2400,2600,2510	WH	152
471	2510	G=FM	WH	153
473	2520	KB=KA	WH	154
475	2530	KQ=2	WH	155
476	2540	GO TO 2050	WH	156
	C2544		WH	157
	C2546		WH	158
		WHOLE	WH	159
477	2600	U(2)=C(1)-C(4)	WH	160
502	2610	U(3)=C(2)-C(5)	WH	161
505	2620	U(4)=C(3)-C(6)	WH	162
510	2630	IF (L(6)) 4100,5000,4100	WH	163
	C2640		WH	164
	C2642		WH	165
	C2644		WH	166
	C2646	MAIN ENTRY FOR CELL POTENTIAL	WH	167
	C2648		WH	168
		REPULSIVE PART	WH	169
512	3000	X=P(1)	WH	170
513	3002	U(2)=X**2	WH	171
515	3004	IF (AN) 3600,3600,3010	WH	172
517	3010	KB=KR	WH	173
521	3020	KQ=1	WH	174
	C3030		WH	175
	C3040		WH	176
		CALC.	WH	177
522	3050	GO TO (3060,3300),KB	WH	178
	C3054		WH	179
	C3056		WH	180
		LJ	WH	181
530	3060	UNF=1.0	WH	182
532	3070	Y=0(2)	WH	183
534	3080	KK=(KCNF-KY-1)/512	WH	184
541	3090	N=2+KEP5(KQ)/KK	WH	185
546	3100	NN=MIN(N,NMAX(KQ))	WH	186
552	3110	GO TO (3150,3200),KQ	WH	187
	C3144		WH	188
560	3150	KE=N+1-NN	WH	189
563	3160	F(1)=A(KE)*Y	WH	190
566	3162	KE=KE+1	WH	191
570	3170	DO 3180 I=KE,M	WH	192
575	3180	F(1)=(F(1)+A(I))*Y	WH	193
602	3190	GO TO 3250	WH	194
	C3194		WH	195
603	3200	KE=N+1-NN	WH	196
606	3210	F(4)=AL(KE)*Y	WH	197
611	3220	KE=KE+1	WH	198
613	3230	DO 3240 I=KE,M	WH	199
620	3240	F(4)=(F(4)+AL(I))*Y	WH	200
	C3244		WH	201
625	3250	J=(KQ-1)*3	WH	202
630	3260	W(J+1)=WC(J+1)*F(J+1)	WH	203
633	3270	W(J+2)=WC(J+2)*F(J+1)	WH	204
636	3280	W(J+3)=WC(J+3)*F(J+1)	WH	205
641	3290	GO TO 3450	WH	206
	C3294		WH	207
	C3296		WH	208
		EXP	WH	209
642	3300	J=(KQ-1)*M	WH	210
646	3310	E=A(J+1)*X	WH	211
651	3320	E1=EXP(E)/2.0	WH	212

657	3330	E2=0.25/F1	WH	208
661	3340	FC=(E1+E2)	WH	209
663	3350	FS=(E1-E2)	WH	210
665	3360	IF (E=0.1) 3370,3370,3450	WH	211
670	3370	E1=F+E	WH	212
672	3380	E2=E1+E1	WH	213
674	3390	FSS=1.0+E1/6.0+E2/120.0	WH	214
701	3400	GO TO 3452	WH	215
	C3444		WH	216
702	3450	FSS=FS/F	WH	217
704	3452	FS=X*FS	WH	218
	C3454		WH	219
706	3460	I=(KU-1)*3	WH	220
711	3462	F(I+1)=A(J+3)*FSS-A(J+2)*FC-1.0	WH	221
720	3470	F(I+2)=A(J+4)*FSS-FS+A(J+5)*FC+A(J+1)	WH	222
730	3480	F(I+J)=A(J+6)*FSS+A(J+7)*FS	WH	223
		1 + (A(J+8)-A(J+1)*D(2))*FC+A(J+9)	WH	224
743	3490	J=I	WH	225
	C3494		WH	226
745	3500	W(J+1)=WC(J+1)*F(J+1)	WH	227
750	3510	W(J+2)=WC(J+2)*F(J+2)	WH	228
753	3520	W(J+3)=WC(J+3)*F(J+3)	WH	229
	C3544		WH	230
756	3530	GO TO (3600,3650),KQ	WH	231
	C3594		WH	232
	C3596	ATTRACTIVE PART	WH	233
764	3600	IF (AM) 3610,3650,3610	WH	234
765	3610	K8=KA	WH	235
767	3620	KQ=P	WH	236
770	3630	GO TO 3650	WH	237
	C3644		WH	238
	C3646	FINISH	WH	239
773	3650	U(3)=W(1)-W(4)	WH	240
774	3660	U(4)=W(2)-W(5)	WH	241
777	3670	U(5)=W(3)-W(6)	WH	242
1002	3680	IF(L(6)) 4200,5000,4200	WH	243
	C3692		WH	244
	C3694	DIAGNOSTIC PRINT	WH	245
	C3696		WH	246
	C3698	PRELIM	WH	247
1004	4000	CALL PRIN(13,MPREL,WR CC3,6,CC)	WH	248
1007		CALL PRIN(3,WN5,6,WN)	WH	249
1014	4010	IF (L(1)-2) 4020,4030,4020	WH	250
1016	4020	CALL PRIN(2,AS,30,A1	WH	251
1021		CALL PRIN(3,ALS,30,AL)	WH	252
1026	4030	GO TO 5000	WH	253
	C4048	MAIN INITIAL	WH	254
1027	4100	CALL PRIN(13,MAIN,WR C 3,6,C)	WH	255
1032		CALL PRIN(3,WC3,6,WC)	WH	256
1037	4120	IF (L(1)-1) 4130, 4140,4130	WH	257
1041	4130	CALL PRIN(2,AS,9,A)	WH	258
1044		CALL PRIN(4,AL 3,9,AL)	WH	259
1051	4140	GO TO 5000	WH	260
	C4144	MAIN INTEGRATE	WH	261
1052	4200	CALL PRIN(2,FS,6,F)	WH	262
1055		CALL PRIN(13,HW (WR ROUT) 3,6,W)	WH	263
1062	4210	GO TO 5000	WH	264
	C4214		WH	265
1063	5000	RETURN	WH	266
	C		WH	267

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SUBROUTINE FKW(K)
C KISTIAKOWSKY-WILSON EQUATION OF STATE
C -----
C K=1: EOS, CALLED FROM GEM(2)
C K=2: MUS, CALLED FROM XIM(2)
C K=1
C INPUT
C 1,V=TAU,THETA=GM(1),(2). (FOR KW,V$IAK=ISIAK=1)
C XI=EMX - (GAS) MOLE FRACTIONS
C KI=XPG - COVOLUMES. NOTE: THIS ARRAY IS COVOLUMES
C KR=KIM(1) - NO. SPECIES
C OUTPUT
C AE = X*EXP(THETA*X)=7-1.LOCAL, USED BY K=2 ENTRY.
C
C FOR KW, KSTARIJ FOR LJO.
C K=2
C INPUT (SEE DEFINITIONS ABOVE)
C AE FROM K=1
C GM FROM K=1
C KI=XPG
C NCIES
C 1. UNLIKE LJO, FOR WHICH MIX PART IS DONE IN XIM-XIMS,
C FOR KW EVERYTHING IS DONE HERE.
C -----
3 COMMON Z(4000)
3 DIMENSION
3 1 ENX ( 20),GM ( 40),GP ( 20)
3 2,KTM ( 10),XMU ( 20),XMT ( 30)
3 3,XPG ( 20, 20)
3 EQUIVALENCE
3 1 (Z(11711),EMX) ,(Z(14911),GM) ,(Z(14711),GP)
3 2,(Z(16811),KIM) ,(Z(22411),XMU) ,(Z(22111),XMT)
3 3,(Z(26601),XPG)
C
C KISTIAKOWSKY-WILSON EQUATION OF STATE
C
C EQUIVALENCE (GP(1),ALP),(GP(2),BET),(GP(3),TH)
3 EQUIVALENCE (GM(1),V),(GM(2),I),(GM(12),X)
3 EQUIVALENCE (XMT(10),MK)
3 EQUIVALENCE (KIM(1),KR)
C
C
C GO TO (100,500),K
C ----- K=1, EOS -----
11 100 MK=0
12 110 DO 120 I=1,KR
21 120 MK=MK+EMX(I+1)*XPG(I)
C
25 130 X=MK/(V*(T+TH)*ALP)
34 140 E=EXP(THETA*X)
42 170 AE=X*E
C
44 200 GM(3)=XF+1.0
47 210 GM(4)=ALP*TH*E/(T+TH)
53 212 GM(6)=(E-1.0)/BET-ALOG(GM(3))

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62	220	GM(9)=GM(3)-(1.0*HET*X)*GM(4)	HKA	59
67	230	GM(10)=-(1.0*HET*X)*XE	HKA	60
73	240	GM(11)=GM(4)*(2.0-(1.0*ALP*(1.0*HET*X))*T/(T+TM))	HKA	61
105	250	GM(5)=GM(4)*XE	HKA	62
107	260	GM(7)=GM(6)*XE	HKA	63
111	270	GM(8)=GM(5)-GM(7)	HKA	64
	C		HKA	65
113	400	GO TO 2000	HKA	66
	C	----- K=2, MUS -----	HKA	67
114	500	DO 510 I=1,KR	HKA	68
123	510	AMII(I)=GM(5)+(XPG(I)/HK-1.0)*XE	HKA	69
	C		HKA	70
	C	520 NOTE- GEM MOVES F/R! FROM GM(7) TO GM(5)	HKA	71
	C		HKA	72
131	2000	RETURN	HKA	73
132		END	HKA	74

		SUBROUTINE SEM (K,L)	SEM	2
	C		SEM	3
	C	SOLID EQ. OF STATE ADAPTOR	SEM	4
	C		SEM	5
	C	REVISION I - FOR NEW SEMS CODE	SEM	6
	C	W.F. 10/61	SEM	7
	C		SEM	8
	C		SEM	9
	C	SEM	SEM	10
	C		SEM	11
6		COMMON 7(4000)	SEM	12
6		DIMENSION	SEM	13
		1 KEN (6, 10),KUN (6, 10),CAR (10, 8)	SEM	14
		2 CONT (20),EV (20),FUR (6, 10)	SEM	15
		3 KAL (20),KEV (20),SP (20)	SEM	16
		4 SPC (20),SM (20),TMS (20)	SEM	17
		5 THER (50)	SEM	18
6		DIMENSION CE(10)	SEM	19
6		EQUIVALENCE	SEM	20
		1 (7(1620),KEN) ,(2(1690),KUN) ,(2(920),CAR)	SEM	21
		2 (7(460),CONT) ,(2(680),EV) ,(2(1410),FUR)	SEM	22
		3 (2(1600),KAL) ,(2(900),KEV) ,(2(1840),SP)	SEM	23
		4 (2(1860),SPC) ,(2(1820),SM) ,(2(1990),TMS)	SEM	24
		5 (2(1920),THER)	SEM	25
	C		SEM	26
	C	LOCAL EQ	SEM	27
	C		SEM	28
6		EQUIVALENCE (CAR(51),CE),(CONT(2),K)	SEM	29
		1 (THER(1),P),(THER(3),T),(SM(1)+VS)	SEM	30
6		GO TO (1000,10),K	SEM	31
	C 994		SEM	32
	C 996	PRELIMINARY	SEM	33
	C 998		SEM	34
13	1000	CALL REAP (SEM	35
		1 5400X G, CPR, AL, VU, TU, EOR / C0, C1, C2, C3, C4 5	SEM	36
		2 ,12,SP)	SEM	37
20	1001	KAL(4)=1	SEM	38
21	1002	IF(SP(2))1004,1003,1004	SEM	39
22	1003	KAL(4)=0	SEM	40
	C		SEM	41
23	1004	CALL SEMS(1)	SEM	42
27	1006	SM(9)=0.8	SEM	43

31	C	1010 CALL OOUT (3HSEM,1)	SEM	44
36		1020 GO TO 300	SEM	45
	C1098		SEM	46
	C		SEM	47
	C	SES MAIN	SEM	48
37		10 KEM(2)=KEM(2)+1	SEM	49
41		20 IF (KAL(2)) 40,100,40	SEM	50
	C		SEM	51
42		40 CALL SEMS(2)	SEM	52
	C		SEM	53
46		50 GO TO 200	SEM	54
	C		SEM	55
	C	CALC. INCOMPRESSIBLE SOLID OUTPUT	SEM	56
47		100 SM(9)=1.0	SEM	57
51		102 SM(10)=1.0	SEM	58
53		104 SM(1)=SP(4)	SEM	59
55		106 SM(2)=0.0	SEM	60
56		108 SM(3)=P*VS/(R*T)	SEM	61
62		110 SM(4)=0.0	SEM	62
63		112 SM(5)=SM(3)	SEM	63
65		114 SM(6)=0.0	SEM	64
66		116 SM(7)=SM(3)	SEM	65
70		118 SM(8)=P	SEM	66
72		200 CALL OOUT (3HSEM,2)	SEM	67
77		300 RETURN	SEM	68
			SEM	69
	C	ARGS K=1, PMEL.	SEM	70
	C	K=2, MATN	SEM	71
	C	L=1, ISOTHERM	SEM	72
	C	L=2, ISENTROPIC	SEM	73
	C		SEM	74
	C		SEM	75
	C	SPECS	SEM	76
	C	INPUT	SEM	77
	C	SP SEPS INPUT (SEE SEPS)	SEM	78
	C	SPC SEPS OUTPUT (SEE SEPS)	SEM	79
	C	T TEMP	SEM	80
	C	VS -SOLID VOL	SEM	81
	C	OUTPUT	SEM	82
	C	SM SES IMPERFECTION THERMO FNS-SEE SEPS	SEM	83
	C	HERE E,K,A,F,S FURT,P=1 ATM HAVE BEEN	SEM	84
	C	SUBTRACTED TO FORM IMPERFECTION FNS.	SEM	85
	C		SEM	86
100		END	SEM	87
		SUBROUTINE SEMS (K)	SEMS	2
	C		SEMS	3
	C	NEW SES SUBROUTINE	SEMS	4
	C	WITH SINGLE ITERATION FOR V(P,T)	SEMS	5
	C	INPUT - P,T	SEMS	6
	C	OUTPUT - V AND SES IMP. THERMO FNS	SEMS	7
	C	K=1 FOR PMEL	SEMS	8
	C	K=2 FOR MAIN	SEMS	9
	C		SEMS	10
	C	W. F. -10/61	SEMS	11
	C		SEMS	12
	C		SEMS	13
			SEMS	14
3		COMMON Z(4000)	SEMS	15

	DIMENSION											SEMS	16	
3	1 CAR	(10,	8),EV	(20),FOD	(6,	10)			SEMS	17	
	2,KON	(6,	10),SM	(20),SP	(20)			SEMS	18	
	3,THER	(50)								SEMS	19	
3	(DIMENSION C(5)*CN(5)+CG(5)+CGI(5)+CS(10) + KCS(2))											SEMS	20	
3	EQUIVALENCE												SEMS	21
	1 (Z(920),CAR) , (Z(080),EV) , (Z(1410),FOD)					SEMS	22	
	2,(Z(1690),KON) , (Z(1820),SM) , (Z(1840),SP)					SEMS	23	
	3,(Z(1920),THER)								SEMS	24		
C												SEMS	25	
C	#ARGUMENTS#												SEMS	26
3	EQUIVALENCE												SEMS	27
	1 THER(1),P),(THER(3),T)											SEMS	28	
	2 ,(FOR(11),FOBI),(FOD(23),YL),(KON(47),KONI)											SEMS	29	
	3 ,(CAR(41),CS),(CS(8),KCS)											SEMS	30	
	4 ,(EV(1),E1),(EV(2),E2)											SEMS	31	
C												SEMS	32	
C												SEMS	33	
C												SEMS	34	
3	EQUIVALENCE												SEMS	35
	1 (SP(1),G),(SP(3),ALPH),(SP(4),V0),(SP(5),TO)											SEMS	36	
	2 ,(SP(8),C),(SP(13),A),(SP(14),GI)											SEMS	37	
	3 ,(SP(15),G2),(SP(16),CONST)											SEMS	38	
	4 ,(SP(18),CN),(SP(24),CG),(SP(30),CGI)											SEMS	39	
	5 ,(SM(9),Y),(SM(10),Y1),(SM(11),IC)											SEMS	40	
	6 ,(SM(12),T1),(SM(13),PH),(SM(15),WEEG)											SEMS	41	
	7 ,(SM(16),P2),(SM(17),Y11),(SM(18),X)											SEMS	42	
	8 ,(SM(19),YU)											SEMS	43	
C												SEMS	44	
C												SEMS	45	
C												SEMS	46	
3	20 GO TO (100,1000),K											SEMS	47	
C	PRELIM												SEMS	48
C												SEMS	49	
11	100 M=R.31474E-5											SEMS	50	
13	112 A=(4*SP(2)/(ALPH*V0))*(G/(G+1.0))											SEMS	51	
22	110 G1=1.0/(3+1.0)											SEMS	52	
25	140 G2=0.5+1.0/G											SEMS	53	
C												SEMS	54	
31	150 CN(I)=G1											SEMS	55	
33	160 DO 140 I=2,4											SEMS	56	
35	170 FI=1											SEMS	57	
36	180 CN(I)= CN(I-1)*(G1-(FI-1.0))/_PI											SEMS	58	
C												SEMS	59	
45	200 DO 230 I=1,5											SEMS	60	
47	210 FI=I-1											SEMS	61	
52	220 CG(I)=C(I)/(G+FI)											SEMS	62	
56	230 CGI(I)=C(I)/(G+FI+1.0)											SEMS	63	
C												SEMS	64	
64	250 E1=0.0											SEMS	65	
65	260 E2=0.0											SEMS	66	
66	270 DO 270 I=1,5											SEMS	67	
70	280 E1=E1+CG(I)											SEMS	68	
73	290 E2=E2+CGI(I)											SEMS	69	
76	300 CONST=0.5+E1-G2+E2											SEMS	70	
C												SEMS	71	
102	GO TO 2000											SEMS	72	
C												SEMS	73	
C												SEMS	74	
	MAIN											SEMS	75	

C		SEMS	76
103	1000 CS(4)=Y	SEMS	77
105	1020 CS(2)=Y*(F/R)	SEMS	78
107	1030 YU=1.0+ALPH*(T-T0)	SEMS	79
113	1040 ACS(1)=0	SEMS	80
C		SEMS	81
C	ITERATE ON Y=V/V0	SEMS	82
114	1100 CALL FRONTT (CS,KONT)	SEMS	83
120	1110 KEXIT=KCS(2)	SEMS	84
122	1120 GO TO (1500,1150,1130,1140),KEXIT	SEMS	85
132	1130 CALL DOUT (4HSEMS,1)	SEMS	86
136	1132 GO TO 1500	SEMS	87
137	1140 CALL DOUT (4HSEMS,1)	SEMS	88
143	1142 GO TO 1500	SEMS	89
C		SEMS	90
C	FUNCTION	SEMS	91
144	1150 IF (CS(2)-YU) 1180,1180,1160	SEMS	92
147	1160 CS(2)=YU	SEMS	93
151	1170 GO TO 1200	SEMS	94
152	1180 IF (YL-CS(2)) 1200,1200,1190	SEMS	95
155	1190 CS(2)=YL	SEMS	96
C		SEMS	97
157	1200 Y=CS(2)	SEMS	98
C		SEMS	99
161	1210 PH=C(5)	SEMS	100
163	1220 E1=C(5)	SEMS	101
165	1230 E2=C(15)	SEMS	102
167	1240 DO 1290 I=1,4	SEMS	103
171	1260 KE=5-I	SEMS	104
173	1270 PH=PH*Y+C(KE)	SEMS	105
176	1280 E1=E1*Y+C(KE)	SEMS	106
201	1290 E2=E2*Y+C(15)(KE)	SEMS	107
C		SEMS	108
206	1300 WEEG=(0.5-G2*Y)*PH	SEMS	109
212	1310 YG=Y*G	SEMS	110
C		SEMS	111
216	1320 P2=- (G/Y)*WEEG+G*(G/Y)* 1 (0.5*E1-G2*Y*E2-CONST/YG)	SEMS	112
C		SEMS	113
C		SEMS	114
231	1330 IF (Y-1.0) 1700,1800,1800	SEMS	115
C		SEMS	116
C		SEMS	117
C		SEMS	118
235	1400 CS(3)=2.0E-6*(TC-T)	SEMS	119
C		SEMS	120
243	1470 CALL DOUT (4HSEMS,1)	SEMS	121
244	1480 GO TO 1100	SEMS	122
C		SEMS	123
C		SEMS	124
C	CALCULATE OUTPUT	SEMS	125
245	1500 SM(1)=Y*V0	SEMS	126
247	1510 SM(7)=P*(1)/(H*T)	SEMS	127
253	1520 SM(1)=(1.0+1.0/G)*SM(7)+V0*WEEG/(H*T)-SP(2)*(1.0-[0/T)	SEMS	128
265	1530 SM(6)=SP(2)*ALUG(T1/T)	SEMS	129
274	1540 SM(5)=SM(3)-SM(6)	SEMS	130
276	1550 SM(2)=SM(3)-SM(7)	SEMS	131
300	1560 SM(4)=SM(5)-SM(7)	SEMS	132
302	1572 GO TO 2000	SEMS	133
C		SEMS	134
C		SEMS	135
C		SEMS	136
C	CALC. FN. FOR Y LESS THAN 1	SEMS	137

C		SEMS	136
303	1700 X=(P-P2)*YG*Y/A	SEMS	137
310	1710 YG1=1.0*X	SEMS	138
313	1720 Y11=CN(4)*X	SEMS	139
315	1730 DO 1740 I=1,3	SEMS	140
317	1732 KE=4-I	SEMS	141
321	1740 Y11=(Y11+CN(KE))*X	SEMS	142
324	1742 Y1=Y11+1.0	SEMS	143
C		SEMS	144
331	1750 T1=Y11/ALPH+T0	SEMS	145
334	1760 TC=T1*(Y11/Y1)/YG	SEMS	146
340	1770 GO TO 1400	SEMS	147
C		SEMS	148
C		SEMS	149
341	1800 X=P/A	SEMS	150
343	1810 YG1=1.0*X	SEMS	151
346	1820 Y11=CN(4)*X	SEMS	152
350	1830 DO 1850 I=1,3	SEMS	153
352	1840 KE=4-I	SEMS	154
354	1850 Y11=(Y11+CN(KE))*X	SEMS	155
361	1860 Y11=Y-1.0+Y*Y11	SEMS	156
365	1862 Y1=Y11+1.0	SEMS	157
C		SEMS	158
370	1870 T1=Y11/ALPH+T0	SEMS	159
373	1880 TC=T1*YG1*Y/(Y11+1.0)	SEMS	160
400	1890 GO TO 1400	SEMS	161
C		SEMS	162
401	2000 RETURN	SEMS	163
402	END	SEMS	164

	SUBROUTINE TIM (K)	TIM	2
C		TIM	3
C	ITF ADAPTOR	TIM	4
C		TIM	5
C	REVISION 1. FIX TIM FOR TMS REVISION 1	TIM	6
C	W.F. DEC. 61	TIM	7
C		TIM	8
C	TIM	TIM	9
3	COMMON Z(4000)	TIM	10
3	DIMENSION	TIM	11
	1 CONT (20) ,EA (200) ,EMX (20)	TIM	12
	2 ME (10) ,KEN (60) ,KIM (10)	TIM	13
	3 THER (50) ,TMS (20) ,TMG (20)	TIM	14
	4 TP (20,10)	TIM	15
3	DIMENSION KE(2),TH(5)	TIM	16
3	EQUIVALENCE	TIM	17
	1 (Z(400) ,CONT) , (Z(480) ,EA) , (Z(1170) ,EMX)	TIM	18
	2 (Z(1590) ,ME) , (Z(1620) ,KEN) , (Z(1680) ,KIM)	TIM	19
	3 (Z(1920) ,THER) , (Z(1990) ,TMS) , (Z(1970) ,TMG)	TIM	20
	4 (Z(2010) ,TP)	TIM	21
C	LOCAL E,J,DIM	TIM	22
3	EQUIVALENCE (KIM(2),KS), (KIM(4),KN), (CONT(3),ATM)	TIM	23
	1 , (THER(1),P), (THER(3),T)	TIM	24
C		TIM	25
C	98	TIM	26
3	100 GO TO (1000,2000),K	TIM	27
C	996	TIM	28
C	998	TIM	29
	PRELIMINARY	TIM	30

11	1000 CALL HEAD (TIM	31
	1 6000X KS,KN/ T BCUNOS/ FIT COEFFS.-A1 TO AN,D,DEL,PF,MR...S		TIM	32
	2 0=-2*KE)		TIM	33
14	CALL HEAD(0.2,TH(4))		TIM	34
20	1010 KS=KE(1)		TIM	35
22	1020 KN=KE(2)		TIM	36
24	1030 KE1=KN+K		TIM	37
26	1040 DO 1070 I=1,KS		TIM	38
30	1050 CALL HEAD (0,KE1,EA)		TIM	39
34	1060 DO 1070 J=1,KE1		TIM	40
44	1070 IP(I,J)=EA(J)		TIM	41
52	GO TO 3000		TIM	42
	C1996		TIM	43
	C1998	MAIN	TIM	44
52	2000 KEH(3)=KEH(3)+1		TIM	45
54	2010 TH(1)=T		TIM	46
56	2060 KE(1)=KS		TIM	47
60	2070 KE(2)=KN		TIM	48
62	2080 TH(2)=P/ATM		TIM	49
64	2090 TH(3)=HE(3)		TIM	50
	C2100		TIM	51
66	2110 CALL TIMS (KE,TH,TP,EMX,IMS,IMG)		TIM	52
74	2120 CALL DOUT (3HTIM,1)		TIM	53
	C2900		TIM	54
100	3000 RETURN		TIM	55
	C		TIM	56
	C		TIM	57
101	END		TIM	58
	SUBROUTINE TIMS (K,TH,A,X,G,F)		TIMS	2
C			TIMS	3
C	IDEAL GAS THERM FNS SUBROUTINE		TIMS	4
C	REVISION 1.-CONST. CP EXTENSIONS		TIMS	5
C	W. F. UEC. 61		TIMS	6
C			TIMS	7
C	K(1)=KS, NO. OF SPECIES		TIMS	8
C	K(2)=KN, DEGREE OF FIT		TIMS	9
C	TH(1)=T IN DEGREES K.		TIMS	10
C	TH(2)=PINATM.		TIMS	11
C	TH(3)=T SUB ZERO		TIMS	12
C	TH(4)=TMIN		TIMS	13
C	TH(5)=TMAX		TIMS	14
C	A = COEFFICIENT MATRIX (SEE WRITE-UP)		TIMS	15
C	X = MOLE FRACTIONS (X(1) FOR SOLID)		TIMS	16
C			TIMS	17
C	IDEAL GAS THERMODYNAMIC FUNCTIONS		TIMS	18
C	INPUT		TIMS	19
C	OUTPUT		TIMS	20
C			TIMS	21
C	G = TOTAL THERMO FUNCTIONS FOR GAS,SOLID		TIMS	22
C	F = FREE ENERGIES AT 1,P		TIMS	23
C	RELATIVE TO ELEMENTS AT 0 KELVIN		TIMS	24
C	IMS		TIMS	25
16	COMMON 7(4000)		TIMS	26
16	DIMENSION K(2),TH(5),A (20,10),X(20),G(20),F(20)		TIMS	27
	1,EA(40),C(20),H(20),S(20),GI(20)		TIMS	28
16	EQUIVALENCE		TIMS	29
	1 (Z(480),EA)		TIMS	30
	1 , (EA(1),C), (EA(41),H), (EA(41),S)		TIMS	31
	2, (EA(61),GI)		TIMS	

C			TIMS	32
C			TIMS	33
C	2 E		TIMS	34
16	3	$\mu=1.98719E-3$	TIMS	35
20	4	$KS=K(1)$	TIMS	36
21	5	$N=K(4)$	TIMS	37
23	6	$T=TH(1)$	TIMS	38
25	7	$PLUG=ALOG(TH(2))$	TIMS	39
34	8	$TH=TH(3)$	TIMS	40
34		$TMIN=TH(4)$	TIMS	41
34		$TMAX=TH(5)$	TIMS	42
C	9 I(E)		TIMS	43
41	10	DO 20 I=1,80	TIMS	44
46	20	EA(I)=0.0	TIMS	45
C		BOUND T1 TO FIT RANGE	TIMS	46
53	30	IF (T-TMAX) 60,60,40	TIMS	47
56	40	T1=TMAX	TIMS	48
60	50	GO TO 110	TIMS	49
61	60	IF (T-TMIN) 70,70,90	TIMS	50
64	70	T1=TMIN	TIMS	51
66	80	GO TO 110	TIMS	52
67	90	T1=T	TIMS	53
C	100 I	ALL SPECIES	TIMS	54
71	110	DO 240 T=1,KS	TIMS	55
C	112 I(E)	J=N,1 FOR SERIES	TIMS	56
73	120	J=N	TIMS	57
75	130	FJ=J	TIMS	58
77	140	A1J=A(I,J+1)	TIMS	59
103	150	H(I)=(H(I)+A1J)*T1	TIMS	60
107	160	C(I)=(C(I)+(FJ+1.0)*A1J)*T1	TIMS	61
115	170	S(I)=(S(I)+((FJ+1.0)/FJ)*A1J)*T1	TIMS	62
124	180	J=J-1	TIMS	63
126	190	IF (J) 130,210,130	TIMS	64
C	210 E	ADD FIRST TERMS	TIMS	65
127	210	A1J=A(I,1)	TIMS	66
132	220	H(I)=H(I)+A1J	TIMS	67
135	230	C(I)=C(I)+A1J	TIMS	68
140	240	S(I)=S(I)+A1J*ALOG(T1)+A(I,N+2)-PLUG	TIMS	69
C			TIMS	70
C		ADD CONST CP FUNCTIONS OUTSIDE	TIMS	71
155	250	IF (T-T1) 260,290,260	TIMS	72
157	260	H(I)=(T1*H(I)+C(I)*(T-T1))/T	TIMS	73
165	270	S(I)=S(I)+C(I)*ALOG(T/T1)	TIMS	74
C			TIMS	75
200	290	F(I)=H(I)-S(I)+A(I,N+3)/(K*T)	TIMS	76
C	300 I(E)	MIXTURE SUMS	TIMS	77
213	310	DO 360 T=2,KS	TIMS	78
215	312	XI=X(I)	TIMS	79
217	320	GI(2)=GI(2)+XI*(H(1)+A(I,N+3)/(K*T))	TIMS	80
230	330	GI(3)=GI(3)+XI*C(I)	TIMS	81
230		FXI=0.0	TIMS	82
234		IF (XI.GT.0.0) FXI=XI*ALOG(XI)	TIMS	83
244	340	GI(4)=GI(4)+XI*S(I)-FXI	TIMS	84
251	350	GI(5)=GI(5)+XI*A(I,N+4)	TIMS	85
257	360	GI(6)=GI(6)+XI*(H(1)-(T0/T)*A(I,N+5)+A(I,N+4)/(R*T))	TIMS	86
C	370 E		TIMS	87
301	380	GI(1)=GI(2)-1.0	TIMS	88
C	400 E	PURE PHASE	TIMS	89
304	410	GI(7)=H(1)+A(I,N+3)/(K*T)	TIMS	90
312	420	GI(8)=C(I)	TIMS	91

314	430	GI(9)=S(1)*PLCG	TIMS	92
316	440	GI(10)=C(1)-PLCG	TIMS	93
320	450	GI(11)=A(1,N+4)	TIMS	94
323	460	GI(12)=H(1)-(T0/T)*A(1,N+5)+GI(11)/(R*T)	TIMS	95
334	470	F(1)=GI(0)	TIMS	96
	C 500	I(E) STONE GI	TIMS	97
336	610	DO 520 I=1,12	TIMS	98
343	620	G(I)=GI(1)	TIMS	99
350	600	RETURN	TIMS	100
351		END	TIMS	101

		SUBROUTINE XIM (K,L1	XIM	2
C		GAS (MIXTURE) EQUATION OF STATE AT T, P, XI	XIM	3
C		K=1 PEAC INPUT DATA (PREL.)	XIM	4
C		K=2 MAIN CALCULATION	XIM	5
C		L SPECIFIES PORTION OF EQ CODE FROM	XIM	6
C		WHICH XIM IS CALLED (SEE WRITEUP)	XIM	7
C		INPUT	XIM	8
C		T,P=THEM(3),(1)	XIM	9
C		XI = (GAS) MOLE FRACTIONS	XIM	10
C		OUTPUT	XIM	11
C		XMT = MIXTURE STATE	XIM	12
C		XMU = MU#S	XIM	13
C		ROUTINES	XIM	14
C		XIMS - DETAILED CALCULATIONS FOR LH, CS, 1-FLUID.	XIM	15
C		CALLS GEP(2) IN MIDDLE FOR REF. STATE FOR MU#S	XIM	16
C		GEP(1/2) = PURE STATE POINT (REGULAR/LH EXPANSION)	XIM	17
C		-----	XIM	18
C		REVISION 1 - ADD K# EQ N. OF STATE	XIM	19
C		M.F. 9/61	XIM	20
C			XIM	21
C			XIM	22
C			XIM	23
C		XIM	XIM	24
			XIM	25
5		COMMON 7(4000)	XIM	26
6		DIMENSION	XIM	27
		1 CONT (20),EA (200),EMX (20)	XIM	28
		2 GP (20),GM (40),GMT (3, 20)	XIM	29
		3 KAL (20),KIM (10),THEM (50)	XIM	30
		4 XMT (30),XMU (20),XPF (20, 20)	XIM	31
		5 XPG (20, 20),XPH (20),XPT (20)	XIM	32
		6 KEN(6,10)	XIM	33
6		DIMENSION KE(2),E1(6)	XIM	34
		1 SXG(20),SXF(20)	XIM	35
6		EQUIVALENCE	XIM	36
		1 (7(460),CONT) ,(2(480),EA) ,(2(1170),EMX)	XIM	37
		2 (7(1470),GP) ,(2(149),GM) ,(2(1530),GMT)	XIM	38
		3 (7(1670),KAL) ,(2(1680),KIM) ,(2(1920),THEM)	XIM	39
		4 (7(2210),XMT) ,(2(2240),XMU) ,(2(2260),XPF)	XIM	40
		5 (7(2660),XPG) ,(2(3060),XPH) ,(2(3080),XPT)	XIM	41
		6 (21620),KEN)	XIM	42
C			XIM	43
C		LOCAL EQUIM	XIM	44
C			XIM	45
6		EQUIVALENCE	XIM	46
		1 (CONT(2),R),(GP(5),RSTA),(GP(6),TSTA),(GP(7),VSTA)	XIM	47
		2 (KIM(1),KR),(THEM(1),P),(THEM(3),T)	XIM	48
		3 (XMT(16),RSTAT),(XMT(17),TSTAT),(XMT(18),VSTAT)	XIM	49

	4*(EA(21),SXG),(EA(41),SXF)	XIM	50
C		XIM	51
6	80 GO TO (100,400),K	XIM	52
C	-----PRELIM-----	XIM	53
14	100 CALL READ (XIM	54
	154000 K9,KAL/ SCH,5CT,R*REF,T*REF,N*W/ (K*)/ (T*) S	XIM	55
	1,=2*KE)	XIM	56
17	CALL READ(0.6,E1)	XIM	57
22	CALL READ(0,KE,XPR)	XIM	58
25	CALL READ(0,KE,XPT)	XIM	59
32	110 KR=KE(1)	XIM	60
34	120 KAL(5)=KE(2)	XIM	61
36	130 DO 150 I=1,KR	XIM	62
40	140 XPR(I)=XPR(I)*E1(1)	XIM	63
43	150 XPT(I)=XPT(I)*E1(2)	XIM	64
C	160	XIM	65
46	170 DO 200 I=1,KR	XIM	66
50	180 DO 200 J=1,KR	XIM	67
52	140 XPR(I,J)=(XPR(I)+XPR(J))/2.0	XIM	68
60	200 XPR(I,J)= SQRT (XPR(I)*XPR(J))	XIM	69
C	208	XIM	70
75	210 XMT(11)=E1(3)	XIM	71
77	220 XMT(12)=E1(4)	XIM	72
101	230 XMT(13)=E1(5)	XIM	73
103	240 XMT(14)=E1(6)	XIM	74
105	250 IF (KAL(5)-9) 300,260,300	XIM	75
107	260 DO 270 I=1,KR	XIM	76
115	270 XPR(I)=E1(3)*CONT(5)*XPR(I)*.5	XIM	77
121	300 GO TO 6000	XIM	78
C	-----MAIN-----	XIM	79
122	800 KE=KAL(5)+1	XIM	80
124	802 KE(4)=KE(4)+1	XIM	81
C	CHECK FOR KIASIOWSKY-WILSON	XIM	82
126	804 IF (KAL(5)-9) 810,806,810	XIM	83
130	806 CALL GEP(1)	XIM	84
134	808 CALL HKW(2)	XIM	85
C		XIM	86
140	809 GO TO 1100	XIM	87
C		XIM	88
141	810 GO TO (1000,2000,3000,4000,4000),KE	XIM	89
C	-----	XIM	90
C	840 NU MIX (ZERO)	XIM	91
C	848	XIM	92
152	1000 GO TO (1020,6000,1100),L	XIM	93
C	1010 NU MIX-ONE	XIM	94
161	1020 CALL GEP(1)	XIM	95
165	1030 DO 1040 I=1,KR	XIM	96
172	1040 XMT(I)=GM(5)	XIM	97
174	1050 GO TO 6000	XIM	98
C	1098 NU MIX-THREE	XIM	99
C	MIXTURE=REF. FLUID	XIM	100
175	1100 XMT(1)=GM(15)	XIM	101
177	1110 XMT(2)=GM(4)	XIM	102
201	1120 XMT(3)=GM(17)	XIM	103
203	1130 XMT(4)=GM(20)	XIM	104
205	1140 XMT(5)=GM(5)	XIM	105
207	1150 XMT(6)=GM(11)	XIM	106
211	1160 XMT(7)=GM(10)	XIM	107
213	1170 XMT(8)=GM(9)	XIM	108
215	1180 GO TO 6000	XIM	109

	C-----		XIM	110
	C1999	IDEAL MIXING (ONE)	XIM	111
	C1998		XIM	112
216	2000 GO TO (2070,6000,2200),L		XIM	113
	C2010		XIM	114
	C2020	IDEAL -ONE	XIM	115
225	2030 DO 2110 I=1,KR		XIM	116
227	2040 ISTA=XPT(I)		XIM	117
231	2050 RSTA=XPR(I)		XIM	118
233	2060 VSTA=CONT(5)*RSTA**3		XIM	119
236	2070 CALL GEP(1)		XIM	120
242	2080 GMT(1,I)=GM(15)		XIM	121
245	2090 GMT(2,I)=GM(17)		XIM	122
250	2100 GMT(3,I)=GM(5)		XIM	123
253	2110 AMH(1)=GM(5)		XIM	124
257	2120 GO TO 6000		XIM	125
	C	IDEAL -THREE	XIM	126
260	2200 XMT(1)=0.0		XIM	127
261	2210 XMT(3)=0.0		XIM	128
262	2220 XMT(5)=0.0		XIM	129
263	2230 DO 2250 I=1,KR		XIM	130
265	2240 XMT(1)=EMX(I+1)*GM(1,I)+XMT(1)		XIM	131
271	2250 XMT(3)=EMX(I+1)*GM(2,I)+XMT(3)		XIM	132
275	2260 XMT(5)=EMX(I+1)*GM(3,I)+XMT(5)		XIM	133
	C2270		XIM	134
303	2280 XMT(7)=XMT(1)/(R*T) -1.0		XIM	135
310	2290 XMT(2)=XMT(3)-XMT(7)		XIM	136
312	2300 XMT(4)=XMT(5)-XMT(7)		XIM	137
314	2310 XMT(6)=XMT(3)-XMT(5)		XIM	138
316	2320 XMT(8)=XMT(1)-R*T/P		XIM	139
322	2330 GO TO 6000		XIM	140
	C-----		XIM	141
	C1999	LH (TWO)	XIM	142
	C2098		XIM	143
323	3000 GO TO (3010,3100,3400),L		XIM	144
	C3004		XIM	145
	C3006	LH-ONE	XIM	146
332	3010 RSTA=XMT(11)		XIM	147
334	3020 ISTA=XMT(12)		XIM	148
336	3030 VSTA=CONT(5)*RSTA**3		XIM	149
341	3040 CALL GEP(1)		XIM	150
	C		XIM	151
	C	LH-TWO	XIM	152
345	3100 CALL XIMS (1)		XIM	153
351	3120 GO TO 6000		XIM	154
	C3198	LH-THREE	XIM	155
352	3400 CALL GEP(2)		XIM	156
354	GO TO 6000		XIM	157
	C-----		XIM	158
	C	CS (THREE) AND ONE FLUID (FOUR)	XIM	159
356	4000 GO TO (4010,4100,6000),L		XIM	160
	C4004		XIM	161
	C4006	CS, 1-FLUID - ONE	XIM	162
365	4010 CALL XIMS (0)		XIM	163
371	4020 ISTA=ISTAT		XIM	164
373	4030 RSTA=RSTAT		XIM	165
375	4040 VSTA=VSTAT		XIM	166
377	4050 CALL GEP(1)		XIM	167
	C	CS, 1-FLUID - TWO	XIM	168
403	4100 CALL XIMS (1)		XIM	169

405	GO TO 6000	XIM	170
C		XIM	171
407	6000 CALL DOUT(3HXIM,1)	XIM	172
414	6010 RETURN	XIM	173
C		XIM	174
415	END	XIM	175
SUBROUTINE XIMS (K)		XIMS	2
C	THIS ROUTINE HAD 840 PUNCHES IN COL 73, REMOVED FOR PHOTOSTORE	XIMS	3
C		XIMS	4
C	PERFORM DETAILED CALCULATIONS FOR XIM	XIMS	5
C		XIMS	6
C		XIMS	7
C	XIMS	XIMS	8
		XIMS	9
3	COMMON 7(4000)	XIMS	10
3	DIMENSION	XIMS	11
	1 XPF (20,20), XPG (20,20), CON1 (20)	XIMS	12
	2,EA (200),EMA (20),GM (40)	XIMS	13
	3,GP (20),KAL (20),KIM (10)	XIMS	14
	4,XM (20),XMT (30),EV (20)	XIMS	15
3	DIMENSION BILK(15)	XIMS	16
3	DIMENSION SXG(20),SXF(20),SHN(20),STN(20)	XIMS	17
3	EQUIVALENCE	XIMS	18
	1 (7(2260),XPF) ,(Z(2060),XPG) ,(Z(460),CON1)	XIMS	19
	2,(7(480),EA) ,(Z(1170),EMA) ,(Z(1490),GM)	XIMS	20
	3,(Z(1470),GP) ,(Z(1000),KAL) ,(Z(1680),KIM)	XIMS	21
	4,(Z(2240),XM) ,(Z(2210),XMT) ,(Z(680),EV)	XIMS	22
C		XIMS	23
3	EQUIVALENCE (KIM(1),KN),(KIM(2),KS),(KIM(3),KC),(KIM(4),KN)	XIMS	24
3	EQUIVALENCE (XMT(16),MSTAT),(XMT(17),TSTAT),(XMT(18),VSTAT)	XIMS	25
	1 (GP(5),RSTA),(GP(6),TSTA),(GP(7),VSTA)	XIMS	26
C		XIMS	27
C	704 TO 7090 (N,MFOR ONE FLUID)	XIMS	28
3	EQUIVALENCE (XMT(1),BILK(4))	XIMS	29
C		XIMS	30
3	EQUIVALENCE	XIMS	31
	1(EA(21),SXG),(EA(41),SXF),(EA(61),SHN),(EA(81),STN)	XIMS	32
C		XIMS	33
C	90 CALCULATE BAR= T+R* / M00 II.4	XIMS	34
3	100 DO 130 I=1,KR	XIMS	35
5	120 SXF(I)=0.0	XIMS	36
7	130 SXG(I)=0.0	XIMS	37
12	140 TSTAT=0.0	XIMS	38
13	150 MSTAT=0.0	XIMS	39
C	160 L-BRANCH= CS OR 1-FLUID	XIMS	40
14	200 KQ=KAL(5)	XIMS	41
16	210 GO TO (1500,300,350,400),KQ	XIMS	42
C	240 CS(OR LH)	XIMS	43
24	300 DO 350 I=1,KR	XIMS	44
30	310 DO 330 J=1,KR	XIMS	45
32	320 SXF(I)=EMX(J+1)*XPF(I,J)+SXF(I)	XIMS	46
37	330 SXG(I)=EMX(J+1)*XPG(I,J)+SXG(I)	XIMS	47
45	340 TSTAT=EMX(I+1)*SXF(I)+TSTAT	XIMS	48
50	350 MSTAT=EMX(I+1)*SXG(I)+MSTAT	XIMS	49
55	360 GO TO 700	XIMS	50
C	390 ONE-FLUID	XIMS	51
56	400 EV(11)=0.0	XIMS	52
57	410 EV(12)=0.0	XIMS	53

50	400 DO 550 I=1,KR	XIMS	54
60	510 DO 530 J=1,KR	XIMS	55
64	520 SXF(I)=FHX(J+1)*XPF(1,J)*XPG(1,J)**HILK(14) *SXF(I)	XIMS	56
77	530 SXG(I)=FHX(J+1)*XPF(1,J)*XPG(1,J)**HILK(15) *SXG(I)	XIMS	57
113	540 EV(11)=FHX(I+1)*SXF(I)*EV(11)	XIMS	58
116	550 EV(12)=FHX(I+1)*SXG(I)*EV(12)	XIMS	59
123	600 E3=1.0/(HILK(14)-HILK(15))	XIMS	60
126	610 E4=HILK(14)*E3	XIMS	61
130	620 E5=HILK(15)*E3	XIMS	62
132	630 TSTAT=EV(12)**E4/EV(11)**E5	XIMS	63
142	640 RSTAT=(EV(11)/EV(12))**E3	XIMS	64
	C REJOIN-CALC. VSTA	XIMS	65
147	700 VSTAT=CONT(5)*RSTAT**3	XIMS	66
	C 800	XIMS	67
	C 810 CALC MUS IF K=1	XIMS	68
152	1000 IF IK)1010,1500,1010	XIMS	69
	C	XIMS	70
153	1010 CALL GEP(2)	XIMS	71
	C1090 I-BRANCH= CS OR 1-FLUID	XIMS	72
	C LM	XIMS	73
156	1100 GO TO (1570,1150,1400,1300),KW	XIMS	74
166	1150 DO 1160 I=1,KR	XIMS	75
175	1160 AMI(I)=GM(5)	XIMS	76
	1 *GM(4)*(2.0*(SXF(I)/XMT(12)-1.0)-(TSTAT/TSTA-1.0))	XIMS	77
	2 *3.0*GII(10)*(2.0*(SXG(I)/XMT(11)-1.0)-(RSTAT/RSTA-1.0))	XIMS	78
216	1170 GO TO 1500	XIMS	79
	C1190 CS	XIMS	80
217	1200 DO 1220 I=1,KR	XIMS	81
221	1210 STN(I)=2.0*(SXF(I)/TSTAT-1.0)	XIMS	82
224	1220 SRN(I)=2.0*(SXG(I)/RSTAT-1.0)	XIMS	83
234	1230 GO TO 1400	XIMS	84
	C1290 ONE-FLUID	XIMS	85
235	1300 DO 1320 I=1,KR	XIMS	86
237	1310 STN(I)= -2.0-2.0*E3*(HILK(15)*SXF(I)/EV(11)	XIMS	87
	1 -HILK(14)*SXG(I)/EV(12))	XIMS	88
251	1320 SRN(I)= 2.0*E3*(SXF(I)/EV(11)-SXG(I)/EV(12))	XIMS	89
	C1390 REJOIN FOR MU CALC.	XIMS	90
261	1400 DO 1410 I=1,KR	XIMS	91
270	1410 AMI(I)=XMT(5)+3.0*AMT(7)*SRN(I)+AMI(2)*STN(I)	XIMS	92
277	1500 RETURN	XIMS	93
300	END	XIMS	94

	SUBROUTINE EWP	EWP	2
C	EW PRELIMINARY	EWP	3
C	MSVISION 1 ERROR IN STATEMENT S20	EWP	4
C	LOOP GOES 10 KS, NOT 10	EWP	5
C	*F. 3/60	EWP	6
C		EWP	7
C	EQN	EWP	8
		EWP	9
1	COMMON Z(4090)	EWP	10
1	DIMENSION	EWP	11
	1 EPAL (20, 6),EPA (20),EPA1 (20)	EWP	12
	2 EPC (10),EPW (10),FLAB (12, 8)	EWP	13
	3 KAL (20),KIM (10),KUN (6, 10)	EWP	14
1	DIMENSION KEPA(20),KEPA1(20),KEPAL(20,6),KEPC(10)	EWP	15
1	DIMENSION KE1(12),L(12)	EWP	16
1	EQUIVALENCE	EWP	17
	1 (Z(1210),EPAL) ,(Z(1190),EPA) ,(Z(1330),EPA1)	EWP	18

	2*(Z(1350),EPC)*(Z(1360),EPW)*(Z(3100),FLAH)	EQU	19
	3*(Z(1600),KAL)*(Z(1680),KIM)*(Z(1690),KUN)	EQU	20
C		EQU	21
1	EQUIVALENCE (KIM(2),KS),(KIM(3)+KC)	EQU	22
	2 , (EPA,KEPA),(EPAL,KEPAL),(EPAL,KEPAL)	EQU	23
	3 , (EPC,KEPC)	EQU	24
C		EQU	25
1	EQUIVALENCE (FLAH(49),L)	EQU	26
C		EQU	27
C		EQU	28
1	80 KAL(6)=1	EQU	29
2	100 CALL READ (EQU	30
	1 30H0X C,S,P,-,PP,PHI / CAP Q S	EQU	31
	2 , -6,KEPC)	EQU	32
5	CALL READ(0,KEPC,EPG)	EQU	33
10	110 KC=KEPC(1)	EQU	34
12	120 KS=KEPC(2)	EQU	35
14	130 READ(10,140) (KE1(I),I=1,12)	EQU	36
	140 FORMAT (12A6)	EQU	37
22	150 DO 160 I=1,KS	EQU	38
24	160 READ(10,170) L(I),(KEPAL(I,J),J=1,KC)	EQU	39
	170 FORMAT (A6,11I6)	EQU	40
46	180 READ(10,200) (KEPA(I),I=1,KS)	EQU	41
55	190 READ(10,200) (KEPAL(I),I=1,KS)	EQU	42
	200 FORMAT (12I6)	EQU	43
C		EQU	44
64	200 WRITE(9,310) (KE1(I),I=1,KS)	EQU	45
	310 FORMAT (6I0 ,12A6/)	EQU	46
73	220 DO 330 I=1,KS	EQU	47
75	230 WRITE(9,340) L(I),(KEPAL(I,J),J=1,KC)	EQU	48
	1 , KEPA(I)+KEPAL(11	EQU	49
	340 FORMAT (6H ,A6,11I6)	EQU	50
C		EQU	51
124	500 DO 510 I=1,10	EQU	52
131	510 EPC(I)=KEPC(I)	EQU	53
133	520 DO 530 I=1,KS	EQU	54
135	530 EPA(I)=KEPA(I)	EQU	55
140	540 EPAL(I)=KEPAL(I)	EQU	56
144	550 DO 570 I=1,KS	EQU	57
146	560 DO 570 J=1,KC	EQU	58
156	570 EPAL(I,J)=KEPAL(I,J)	EQU	59
163	580 KAL(6)=1	EQU	60
C		EQU	61
164	600 CALL EQPS(KUN(1,8),EPC,EPW,EPAL,EPAL(1,2),EPA,EPAL)	EQU	62
C		EQU	63
174	1000 RETURN	EQU	64
C		EQU	65
175	END	EQU	66
	SUBROUTINE EQM	EQU	2
C	EQUILIBRIUM COMPOSITION AND STATE AT T,P	EQU	3
C	INPUT	EQU	4
C	P,T=TEMP(1),(3), IMPLICIT FOR GEP VIA XIM-XIMS	EQU	5
C	SM = STATE OF SOLID	EQU	6
C	IMG = IDEAL STATE	EQU	7
C	OUTPUT	EQU	8
C	XI=EMX = (GAS) MOLE FRACTIONS	EQU	9
C	XMT = GAS (MIXTURE) STATE	EQU	10
C	VARIABLES	EQU	11

C	P-TILDE=ENG - FREE ENERGIES FROM EQMS	EQM	12
C	EMN - PHASE MOLE NUMBERS FROM EQMS	EQM	13
C	KSTAT=XST(14),(17) - KSTAR-BAN	EQM	14
C	KSTAT-TSTA=GP - KSTAR FOR GEP	EQM	15
C	RCUTINES	EQM	16
C	XIM - MIXTURE ECS VIA GEP, INCLUDING MU'S	EQM	17
C	EQMS - COMPOSITION AT FIXED P-TILDE	EQM	18
1	COMMON 7(4000)	EQM	19
1	UINENSIGN	EQM	20
	1 ENH (20),EMN (20),EMX (20) FOM	EQM	21
	2 FOM (6, 10),GP (20),GM (40) FOM	EQM	22
	3 KAL (20),KEN (6, 10),KEV (20) FOM	EQM	23
	4 KIM (10),KUN (6, 10),SM (20) FOM	EQM	24
	5 TMG (20),XMU (20),XMT (30) FOM	EQM	25
	7 EA(200),FV(20)	EQM	26
1	EQUIVALENCE	EQM	27
	1 (Z(1010),FOM) ,(Z(1030),EMN) ,(Z(1170),EMX)	EQM	28
	2 (Z(1410),FOM) ,(Z(1470),GP) ,(Z(1490),GM)	EQM	29
	3 (Z(1000),KAL) ,(Z(1020),KEN) ,(Z(900),KEV)	EQM	30
	4 (Z(1600),KIM) ,(Z(1690),KUN) ,(Z(1820),SM)	EQM	31
	5 (Z(1970),TMG) ,(Z(2240),XMU) ,(Z(2210),XMT)	EQM	32
	7 (Z(480),EA),(Z(480),EV)	EQM	33
C	EQUIVALENCE (FOM(15),EPS),(KIM(2),KS)	EQM	34
1	EQUIVALENCE (GP(5),KSTAT),(XMT(16),KSTAT)	EQM	35
1	EQUIVALENCE (GM(15),VM)	EQM	36
C		EQM	37
1	100 KEN(5)=KEN(5)+1	EQM	38
C	BACK HERE FOR OUTER (LM OR 1-FLUID)	EQM	39
3	200 CALL XIM(2,1)	EQM	40
6	210 EMG(1)=TMG(1)+SM(5)	EQM	41
C		EQM	42
10	300 CALL DOUT (3HEQM,1)	EQM	43
C	BACK HERE FOR INNER (ALL)	EQM	44
13	500 DO 520 I=1,KS	EQM	45
15	510 EMG(I+1)=TMG(I+1)+XMU(I)	EQM	46
20	520 EA(I)=EMX(I)	EQM	47
C	SKIP FOR PX. COMP.	EQM	48
24	600 IF (KAL(4)) 800,2000,800	EQM	49
C		EQM	50
25	800 KEV(1)=KAL(4)	EQM	51
27	810 KEV(2)=KUN(2,7)	EQM	52
31	820 KEV(3)=KUN(3,7)	EQM	53
33	830 KEV(4)=0	EQM	54
C		EQM	55
34	850 KEN(13)=KEN(13)+1	EQM	56
C	EQUIL. XI AT FIXED P-TILDE (EMG)	EQM	57
36	900 CALL EQMS (KEV,EMX,EMN,EMG)	EQM	58
C		EQM	59
42	910 DO 920 I=1,6	EQM	60
50	920 KEN(I+7)=KEV(I+6)	EQM	61
C		EQM	62
52	950 CALL DOUT (3HEQM,2)	EQM	63
C	DIFF FOR INNER CONV., NEXT X	EQM	64
55	1000 EV=0.0	EQM	65
56	1010 DO 1050 I=1,KS	EQM	66
60	1020 EV=EV+ABS(EMX(I)-EA(I))	EQM	67
64	1030 IF (KEN(13)-1) 1050,1050,1040	EQM	68
67	1040 EMX(I)=(EMX(I)+EA(I))/2.0	EQM	69
73	1050 CONTINUE	EQM	70
		EQM	71

76	C	1070 CALL DOUT (3HEQM,3)	EQM	72
	C	INNER CONVERGENCE TEST	EQM	73
101	1100	IF (EV-F.HH(16)) 1300,1300,1110	EQM	74
104	1110	CALL XIM(2,2)	EQM	75
107	1120	GO TO 500	EQM	76
	C	OUTER CONVERGENCE TEST	EQM	77
110	1100	IF ((KAL(5)-3)*(KAL(5)-4)) 2000,1310,2000	EQM	78
114	1110	IF (ABS(RSTA-RSTAL)-EPS) 1320,200,200	EQM	79
121	1120	VR=XMT(1)	EQM	80
	C		EQM	81
	C	CALC FINAL THERMU	EQM	82
123	2000	CALL XIM(2,3)	EQM	83
126	2004	CALL DOUT (3HEQM,3)	EQM	84
	C		EQM	85
131	3000	RETURN	EQM	86
	C		EQM	87
	C		EQM	88
132	END		EQM	89
	C		EQM	90
	C	***** MES	MES	2
	C	4. CALCULATION 40NHOLS	MES	3
	C	***** MES	MES	4
	C	SUBROUTINE MES	MES	5
	C		MES	6
	C	MIXTURE EQUATION OF STATE CONTROL	MES	7
	C	CALCULATE EQUATION OF STATE AT	MES	8
	C	GIVEN T AND P	MES	9
	C		MES	10
	C	REPLACE (CALL SEP) BY (CALL SEP)	MES	11
	C	IF SEP REQUIRES ITER. FOR V(P,T).	MES	12
	C	INPUT	MES	13
	C	ITER(1),(2) = P,T (IMPLICIT)	MES	14
	C	OUTPUT = SEE COUT	MES	15
	C		MES	16
	C	MES	MES	17
	C		MES	18
1	COMMON	7(4000)	MES	19
1	DIMENSION	KEN(60)	MES	20
			MES	21
1	EQUIVALENCE		MES	22
	1 (7(1620),KEN)	MES	23
	C		MES	24
1	KEN(111)	=0	MES	25
1	KEN(12)	=0	MES	26
1	KEN(13)	=0	MES	27
1	KEN(6)	=KEN(6)+1	MES	28
1	KEN(12)	=KEN(14)+1	MES	29
6	CALL	DOUT (3HMES,1)	MES	30
	C		MES	31
10	CALL	TIM(2)	MES	32
12	CALL	SEP (2,1)	MES	33
14	CALL	EQM	MES	34
15	CALL	TIM(2)	MES	35
17	CALL	COUT	MES	36
	C		MES	37
20	CALL	DOUT (3HMES,2)	MES	38
22	RETURN		MES	39
	C		MES	40
	C	END	MES	41

	SUBROUTINE COUT	COUT	2
C	CALCULATE MES OUTPUT	COUT	3
C	CALLED FROM MES	COUT	4
C		COUT	5
C	INPUT = ECS ROUTINES OUTPUT	COUT	6
C	EMN(1), EMN(2) = NS, NG	COUT	7
C	TMS = IMEAL	COUT	8
C	THER(1), (3) = P, T	COUT	9
C	XMT = GAS	COUT	10
C	SM = SOLID	COUT	11
C	HE = INITIAL	COUT	12
C	EMS = MOLE FRACTIONS	COUT	13
C	EMG = MU SUM I PRIME (IMPERF. CHEM. POTENTIALS)	COUT	14
C	OUTPUT	COUT	15
C	REST OF EMN = PHASE COMPOSITION	COUT	16
C	THER = THERMO FUNCTIONS	COUT	17
C	FN = MOLE NUMBERS	COUT	18
C	FMI = CHEM. POTENTIALS	COUT	19
1	COMMON / (4000)	COUT	20
1	DIMENSION	COUT	21
	1 CONT (20), EMG (20), EMN (20)	COUT	22
	2 ENX (20), EV (20), FN (20)	COUT	23
	3 FMI (20), HE (10), KIM (10)	COUT	24
	4 SM (20), THER (50), TMS (20)	COUT	25
	5 XMT (30)	COUT	26
1	EQUIVALENCE	COUT	27
	1 (7(454), CONT) , (2(1010), EMG) , (2(1030), EMN)	COUT	28
	2 (7(1170), ENX) , (2(680), EV) , (2(1390), FN)	COUT	29
	3 (7(1370), FMI) , (2(1570), HE) , (2(1680), KIM)	COUT	30
	4 (7(1820), SM) , (2(1920), THER) , (2(1990), TMS)	COUT	31
	5 (7(2210), XMT)	COUT	32
C		COUT	33
1	EQUIVALENCE (CONT(2),R), (CONT(4),CALMB)	COUT	34
1	EQUIVALENCE (THER(1),P), (THER(3),T)	COUT	35
1	EQUIVALENCE (THER(6),U), (THER(8),V), (THER(9),E)	COUT	36
1	EQUIVALENCE (THER(11),M), (THER(13),A), (THER(12),F)	COUT	37
1	EQUIVALENCE (THER(15),S), (THER(16),VM)	COUT	38
1	EQUIVALENCE (KIM(7),KS)	COUT	39
1	EQUIVALENCE (HE(5),VO), (HE(7),MU)	COUT	40
1	EQUIVALENCE (SM(1),VS)	COUT	41
1	EQUIVALENCE (EMN(4),XS), (EMN(5),XS), (EMN(6),XS)	COUT	42
1	EQUIVALENCE (TMS(2),HG10), (TMS(4),SG10), (TMS(6),MHG10)	COUT	43
	1 (TMS(7),MS10), (TMS(9),SS10), (TMS(12),MMS10)	COUT	44
	2 (TMS(5),HFG), (TMS(11),MFS)	COUT	45
1	8 EMN(3)=EMN(2)+EMN(1)	COUT	46
3	10 AG=EMN(1)/EMN(3)	COUT	47
5	20 XS=EMN(2)/EMN(3)	COUT	48
7	30 VM=XG*XMT(1)+XS*VS	COUT	49
13	40 THER(21)=P*VM/(R*T)	COUT	50
17	50 THER(17)=XG*(HG10+XMT(3))+XS*(MS10+SM(3))	COUT	51
25	60 THER(20)=XG*(SG10+XMT(6))+XS*(SS10+SM(6))	COUT	52
33	70 THER(16)=THER(17)-THER(21)	COUT	53
35	80 THER(19)=THER(17)-THER(20)	COUT	54
37	90 THER(18)=THER(19)-THER(21)	COUT	55
41	100 BN=EMN(2)/HE(4)	COUT	56
43	110 EV=BN*R*T	COUT	57
46	120 V=BN*VM	COUT	58

50	130	E=FV*THFR(16)	COUT	59
52	140	M=FV*THFR(17)	COUT	60
54	150	A=FV*THFR(18)	COUT	61
56	160	F=FV*THFR(19)	COUT	62
60	170	S=HNR*THFR(20)	COUT	63
63	172	THFR(14)=FV*(XG*(HMGID+XM1(3))+XS*(HMSID+SM(3)))	COUT	64
72	190	THFR(2)=V/V0	COUT	65
74	200	Q=-HNR*CALMB*(XG*HFG+XS*HFD)+HU+HNR*HME(3)	COUT	66
105	210	THFR(7)=1/CALMB	COUT	67
107	220	FN(1)=EMN(2)	COUT	68
111	230	UO 240 J=2,KS	COUT	69
117	240	FN(I)=EMX(I)*EMN(1)	COUT	70
121	250	UO 260 I=1,KS	COUT	71
123		E1=0	COUT	72
123		IF (EMX(I),NE,0) E1=ALOG(EMX(I))	COUT	73
130	260	FMU(I)=FMG(I)*E1	COUT	74
135	270	FMU(I)=EMG(I)	COUT	75
	C		COUT	76
137	300	RETURN	COUT	77
	C	SPECS	COUT	78
	C	INPUT	COUT	79
	C	P,T,ROUTINE OUTPUTS	COUT	80
	C	OUTPUT	COUT	81
	C	THESE REF.STATE IS ELEMENTS AT 0 K.	COUT	82
	C	HOLE NUMBERS	COUT	83
140		END	COUT	84
		SUBROUTINE POUT(K)	POUT	2
	C		POUT	3
	C		POUT	4
	C		POUT	5
	C	PRINT OUTPUT	POUT	6
	C		POUT	7
	C	K=1 PRINT LABELS	POUT	8
	C	K=2 MAIN PRINT	POUT	9
	C	K=3 DIFFERENTIATION PRINT	POUT	10
	C		POUT	11
	C	PRINT POINT NUMBER AND P,V,I,KHU ON LINE	POUT	12
	C		POUT	13
	C		POUT	14
	C	REVISION 1. ADD PUNCH OUTPUT (KAL(11) ON)	POUT	15
	C	*. F. 10/16/61	POUT	16
	C		POUT	17
	C		POUT	18
	C	POUT	POUT	19
	C		POUT	20
3		COMMON Z(4000)	POUT	21
3		DIMENSION	POUT	22
	1	EMN (20),FN (20),GM (40)	POUT	23
	2	HE (10),KAL (20),KEN (6, 10)	POUT	24
	3	SM (20),THFR (50),XMT (30)	POUT	25
	4	FLAB (12, 8),KIM(10)	POUT	26
3		EQUIVALENCE	POUT	27
	1	(Z(1030),EMN) ,(Z(1390),FN) ,(Z(1490),GM)	POUT	28
	2	(Z(1590),HE) ,(Z(1630),KAL) ,(Z(1620),KEN)	POUT	29
	3	(Z(1620),SM) ,(Z(1920),THFR) ,(Z(2210),XMT)	POUT	30
	4	(Z(3100),FLAB) ,(Z(1680),KIM)	POUT	31
	C		POUT	32
3		EQUIVALENCE (KIM(2),KS)	POUT	33

C			POUT	34
3	10	GO TO (100,180,300),K	POUT	35
C	96	LABELS	POUT	36
C	98		POUT	37
12	100	WRITE(9,7100)	POUT	38
17	120	WRITE(9,7120)	POUT	39
24	140	WRITE(9,7130)	POUT	40
30		IF(0.EQ.0) GO TO 400	POUT	41
C		--- SKIP PUNCH	POUT	42
32	142	IF (KAL(11)) 400,150,400	POUT	43
C			POUT	44
33	150	WRITE(9,7150) ((FLAB(J,I),J=1,12),I=1,4)	POUT	45
50	160	WRITE(9,7160)	POUT	46
55	162	WRITE(9,7162) (FLAB(I,5),I=1,KS)	POUT	47
65	164	WRITE(9,7164)	POUT	48
72	170	GO TO 400	POUT	49
C	176	REG. PRINT	POUT	50
C	178		POUT	51
73	180	KEM(9)=KEM(9)+1	POUT	52
75	200	WRITE(9,7200) KEM(9)	POUT	53
	1	(THER(I),I=1,5),HE(1),THER(7)	POUT	54
	2	THER(8),THER(9),THER(13), (EMN(I),I=1,3),EMN(7)	POUT	55
124	230	WRITE(9,7210) THER(15),THER(16),	POUT	56
		THER(20),THER(21), (FN(I),I=1,3),XMT(1),XMT(2),	POUT	57
		XMT(7),XMT(7), (FN(I),I=4,6),GM(15),GM(4),GM(11),	POUT	58
		GM(15), (FN(I),I=7,9),SM(1),SM(2),SM(6),SM(7), (FN(I),I=10,12)	POUT	59
		4, (XMT(I+15), I=1,3)	POUT	60
217	240	CALL DOUT (4*POUT,1)	POUT	61
213		IF(0.EQ.0) GO TO 400	POUT	62
C		--- SKIP PUNCH	POUT	63
215	242	IF (KAL(11)) 400,250,400	POUT	64
C			POUT	65
216	250	WRITE(9,7250)	POUT	66
		1,HE(1),THER(1),THER(2),THER(3),THER(4),THER(5)	POUT	67
		7,THER(8),THER(9),XMT(16),XMT(18),XMT(17),THER(7)	POUT	68
		3,EMN(2),EMN(1),EMN(3),SM(1),XMT(1),THER(15)	POUT	69
		4, (FN(I),I=1,12)	POUT	70
271	260	GO TO 400	POUT	71
C	276	DIFF. PRINT	POUT	72
C	298		POUT	73
272	300	WRITE(9,7300) (THER(I),I=22,25)	POUT	74
301	310	CALL DOUT (4*POUT,2)	POUT	75
304		IF(0.EQ.0) GO TO 400	POUT	76
C		---SKIP PUNCH	POUT	77
306	312	IF (KAL(11)) 400,320,400	POUT	78
C			POUT	79
307	320	WRITE(9,7320)	POUT	80
		1,HE(22),THER(23),THER(24),THER(25),THER(27)	POUT	81
326	400	RETURN	POUT	82
	7100	FORMAT (160,7X,13HOUTPUT LABELS//12X,1H1,6X,	POUT	83
		11H,14X,4HV/V0,11X,1H1,14X,1H1,14X,1H1,14X,3HHRMO,12X,4HGCAL	POUT	84
		2/12X,1H2,6X,1HV,14X,1HE,14X,1H5,14X,2HNG,13X,2HNS,13X,1HN,14X	POUT	85
		36H50PSAT)	POUT	86
C			POUT	87
	7120	FORMAT (12X,1H3,6X,1HV,14X,4HE/RT,11X,3HS/R,12X,5HMPV/RT,	POUT	88
		110X,2HN1,13X,2HN2, 3X,2HN3 / 12X,1H4,6X,11H00, FOR GAS,	POUT	89
		249X,6HN4,15,1H6/12X,1H5,6X,12H00, FOR REF.,48X,8HN7,1H8,1H9	POUT	90
		3/12X,1H6,6X,13H00, FOR SOLID,47X,11HN10,11,1H12)	POUT	91
C			POUT	92
	7130	FORMAT (12X,1H7,6X,5HRSBAR*,10X,5HTIBAR*,10X,5HVBAR*,10X	POUT	93

	1	,5HIGAMMA,10X,5HALPHA,10X,4MBEIA,11X,1HC)	POUT	94
C			POUT	95
C			POUT	96
	7200	FORMAT (1H0,6HP01N1 12,3X	POUT	97
	1	,3H1 1P/E15.7/12X,3H2 7E15.7)	POUT	98
C			POUT	99
	7210	FORMAT (12X,3H3 1P7E15.7/12X,3H4 7E15.7/12X,	POUT	100
		13H5 7E15.7/12X3H6 7E15.7 / 2X,3H7 3E15.7)	POUT	101
C			POUT	102
	7300	FORMAT (1H0,14X,45X, 1P4E15.7)	POUT	103
C			POUT	104
C		PUNCH FORMATS	POUT	105
	7150	FORMAT	POUT	106
	1	(2H\$1 11A6.A5 / (2H\$0 11A6.A5))	POUT	107
327	7160	FORMAT (POUT	108
		1*H\$01 3H\$H0 0X,1HP 11X,4HV/V0 8X,1HT 11X,1HU 11X,1HD	POUT	109
		2/4H\$ 2 1HV 11X,1HE 11X,4HKBAR 8X,4HVBAR 8X,4HTBAR 8X,1HW	POUT	110
		3/4H\$ 3 2H\$S 10X,2HNG 10X,1HN 11X,2HVS 10X,2HVG 10X,1HV)	POUT	111
327	7162	FORMAT (1H\$ 6A12)	POUT	112
327	7164	FORMAT (POUT	113
		1/4H\$ 5HIGAMMA 7X,5HALPHA 7X,4MBETA 8X,1HC 11X,6HCJ FN	POUT	114
		7)	POUT	115
327	7250	FORMAT (2H\$0 1PE11.4 ,5E12.4 / (1H\$ 6E12.4)	POUT	116
327	7320	FORMAT (2H\$ 1PE11.4 ,5E12.4)	POUT	117
327		END	POUT	118
		SUBROUTINE MESC(KG,ASUC)	MESC	2
C			MESC	3
C		CALCULATE MIXTURE EQUATION OF STATE	MESC	4
C		AT GIVEN T AND	MESC	5
C		P FOR KG=1	MESC	6
C		V FOR KG=2	MESC	7
C		S FOR KG=3	MESC	8
C		E FOR KG=4	MESC	9
C			MESC	10
C		ITERATE ON T UNDER CONTROL OF FROUT,	MESC	11
C		USING MES FOR FUNCTION CALCULATION	MESC	12
C			MESC	13
C			MESC	14
C		ALL USE SAME FROUT CALL,	MESC	15
C		BRANCH ON FUNCTION	MESC	16
C			MESC	17
C		REVISION 1.CALC INTEGRAL PDV ON ISE	MESC	18
C		*. F. 1/3/64	MESC	19
C		MESC	MESC	20
	6	COMMON Z140H0)	MESC	21
6		DIMENSION	MESC	22
		1 KEN (60),KUN (6*10),CAN (80)	MESC	24
		2,FOH (60),THER (50)	MESC	25
		5,CONT(2A),HE(10)	MESC	26
6		DIMENSION ASUC (10)	MESC	27
C		ASUC - INITIAL STATE ON CURVE - SEE SUC	MESC	28
6		EQUIVALENCE	MESC	29
		1 (Z(1620),KEN) ,(Z(1690),KUN) ,(Z(920),CAN)	MESC	30
		2,(Z(1410),FOH) ,(Z(1920),THER)	MESC	31
		5,(Z(460), CONT),(Z(4590),HE)	MESC	32
C			MESC	33
6		DIMENSION CM(10),KCM(2)	MESC	34

6	EQUIVALENCE (CAR(21),CM),(CM(8),KCM)	ME3C	35
7	EQUIVALENCE (THER(8),V),(THER(13),S),(THER(9),L)	ME3C	36
8	EQUIVALENCE (THER(3),T)	ME3C	37
C		ME3C	38
6	4 KEN(14)=0	ME3C	39
7	6 KEN(8)=KEN(8)+1	ME3C	40
11	8 KEN(15)=KEN(14)+1	ME3C	41
13	10 IF (KG-1) 10,15,30	ME3C	42
15	15 I=ASUC(1)	ME3C	43
16	20 CALL MES	ME3C	44
21	25 GO TO 200	ME3C	45
22	30 KCM(1)=0	ME3C	46
23	35 CM(4)=T	ME3C	47
25	40 CM(2)=T*FOR(9)	ME3C	48
27	45 CALL FRGNTT (CM,KON(3,8))	ME3C	49
34	46 KEXIT=KCM(2)	ME3C	50
35	50 GO TO (200,110,70,60), KEXIT	ME3C	51
40	60 CALL DBUG (4HMESC,1)	ME3C	52
53	62 GO TO 200	ME3C	53
56	70 CALL DBUG (4HMESC,2)	ME3C	54
61	72 GO TO 200	ME3C	55
62	80 T=CM(2)	ME3C	56
64	CALL MES	ME3C	57
65	I=KG-1	ME3C	58
70	90 GO TO (40,190,110)*I	ME3C	59
76	90 CM(3)=V-ASUC(3)	ME3C	60
100	95 GO TO 120	ME3C	61
101	100 CM(3)=((EXP((S/ASUC(4))*ALOG(ASUC(1))))/ASUC(1))-1.	ME3C	62
116	105 GO TO 120	ME3C	63
117	110 CM(4)=E-ASUC(5)	ME3C	64
121	120 CALL DOUT (4HMESC,1)	ME3C	65
126	125 GO TO 45	ME3C	66
C		ME3C	67
127	200 IF (KG-3) 220,210,220	ME3C	68
131	210 THER(4)=(1+E(8)-THER(9))/CUNT(4)	ME3C	69
C		ME3C	70
134	220 CALL DOUT (4HMESC,2)	ME3C	71
141	300 RETURN	ME3C	72
142	END	ME3C	73

	SUBROUTINE HUG	HUG	2
C	DETONATION HUGONIOT POINT	HUG	3
C	NCIES	HUG	4
C	1. SPECIAL SECOND GLESS - FROM FIRST	HUG	5
C	ARG AND FUNC AND SLOPE SAVED IN FOR(d)	HUG	6
C	FROM PREVIOUS ITER	HUG	7
1	COMMON 7(4000)	HUG	8
1	DIMENSION	HUG	9
1	1 CAR (10,8), KEN (6,10), KON (6,10)	HUG	10
1	2, FOR (60), HE (10), THER (50)	HUG	11
1	DIMENSION CM(10), KCM(2)	HUG	12
1	EQUIVALENCE	HUG	13
1	1 (Z(420), CAR) , (Z(1620), KEN) , (Z(1690), KON)	HUG	14
1	2, (Z(1410), FOR) , (Z(1590), HE) , (Z(1920), THER)	HUG	15
C		HUG	16
C		HUG	17
1	EQUIVALENCE (THER(1),P),(THER(3),T),(THER(4),U)	HUG	18
1	EQUIVALENCE (THER(5),V),(THER(8),V1),(THER(14),MH)	HUG	19
1	EQUIVALENCE (HE(2),P0),(HE(6),V0),(HE(7),H0)	HUG	20

1	EQUIVALENCE (FOR(21),TL),(FOR(22),TU)	HUG	21
1	EQUIVALENCE (CAR(11),CH),(CH(8),KCH)	HUG	22
C		HUG	23
C	CALCULATE HUGONIOT POINT AT GIVEN P,	HUG	24
C	ITERATE ON T UNDER CONTROL OF FROUT,	HUG	25
C	USING MES IN FUNCTION CALCULATION	HUG	26
C		HUG	27
C	TL AND TU ARE BOUNDS ON ITERATION T	HUG	28
C		HUG	29
1	4 KEN(14)=0	HUG	30
2	6 KEN(15)=KEN(15)+1	HUG	31
4	8 KEN(7)=KEN(7)+1	HUG	32
6	10 IF (T)20,12,20	HUG	33
7	12 T=7000.0	HUG	34
11	20 CH(4)=T/1000.	HUG	35
13	30 KCH(1)=0	HUG	36
14	40 CALL FROUT (CH,KON(2,8))	HUG	37
17	42 KEXIT=KCH(2)	HUG	38
21	50 GO TO (150,72,70,60),KEXIT	HUG	39
31	60 CALL DBOUT (3HHUG,1)	HUG	40
34	62 GO TO 150	HUG	41
35	70 CALL DBOUT (3HHUG,2)	HUG	42
40	71 GO TO 150	HUG	43
41	72 IF (KON (2,8)) 81,75,81	HUG	44
42	75 IF (KCH(1)=2) 81,76,81	HUG	45
44	76 CH(2)=CH(4)-CH(5)/PCB(8)	HUG	46
47	81 I=CH(5)*1000.	HUG	47
51	82 IF (TU-T) 83,83,85	HUG	48
54	83 I=TU	HUG	49
56	84 GO TO 90	HUG	50
57	85 IF (I-TL) 86,90,90	HUG	51
62	86 I=TL	HUG	52
64	90 CALL MES	HUG	53
65	92 U=V0*SQRT((P-P0)/(V0-V))	HUG	54
75	94 U=SQRT((P-P0)*(V0-V))	HUG	55
104	95 CH(2)=T/1000.	HUG	56
106	100 CH(3)=20.0*P*(HH-HU)/((P-P0)*V0)-0.5*(1.0+V/V0)	HUG	57
121	110 CALL DBOUT (3HHUG,1)	HUG	58
124	120 GO TO 40	HUG	59
125	150 IF (KCH(1)=2) 200,200,151	HUG	60
130	151 FOR(8)=(CH(7)-CH(3))/(CH(6)-CH(2))	HUG	61
134	200 RETURN	HUG	62
C		HUG	63
C		HUG	64
135	END	HUG	65
C			
C	SUBROUTINE GAMM(K1,K2)	GAMM	2
C		GAMM	3
C		GAMM	4
C	CALCULATE EQUATION OF STATE DERIVATIVES	GAMM	5
C	BY NUMERICAL DIFFERENCING OF P AND T	GAMM	6
C	USING MES FOR EQ. OF STATE POINTS	GAMM	7
C		GAMM	8
C	INPUT	GAMM	9
C	(1) K1=1 - DIFFERENTIATE WITH CURRENT CONDITION	GAMM	10
C	(FIXED OR EQUILIBRIUM COMPOSITION)	GAMM	11
C	(2) K2=1 - DIFFERENTIATE AT FIXED COMPOSITION	GAMM	12
C		GAMM	13
C	(3) THER (1) P CENTER POINT QUANTITIES	GAMM	14

C	(3) T	GAMM	15
C	(2) V	GAMM	16
C	(21) PV/RT	GAMM	17
C		GAMM	18
C	(4) EMN (3) N	GAMM	19
C		GAMM	20
C	OUTPUT	GAMM	21
C	SUCG (1) GAMMA	GAMM	22
C	(2) ALPHA	GAMM	23
C	(3) BETA	GAMM	24
C	(4) C (SOUND SPEED)	GAMM	25
C	(5) C ₀ FUNCTION	GAMM	26
C	$=((V/V_0)/(GAM/(GAM+1-P/P_0)))^{*}(-GAM)-1$	GAMM	27
C	(6) CAP GAMMA (ISOTHERMAL)	GAMM	28
C	(7) CP/M	GAMM	29
C	(8) (C LN V/D T) (CONSTANT P)	GAMM	30
C		GAMM	31
C	ABOVE OUTPUT IS FORMED FOR EITHER	GAMM	32
C	OR BOTH CONDITIONS AND PLACED IN	GAMM	33
C	APPROPRIATE OTHER LOCATIONS	GAMM	34
C		GAMM	35
C	DATA)	GAMM	36
C	FOR (13) H = H* = PC*P	GAMM	37
C	FOR (14) DEL = T* = IC*(1.0+DEL)	GAMM	38
C	DER (1) PC	GAMM	39
C	(2) VC	GAMM	40
C	(3) TC	GAMM	41
C	(4) PC*VC/H*TC	GAMM	42
C	(5) V+	GAMM	43
C	(6) V-	GAMM	44
C	(7) H+	GAMM	45
C	(8) H-	GAMM	46
C	EP	GAMM	47
C	SAVE NC	GAMM	48
C		GAMM	49
C	GAMM	GAMM	50
5	COMMON Z(4000)	GAMM	51
6	DIMENSION	GAMM	52
	1 DER (10) ,EMN (20) ,FOR (60)	GAMM	53
	2,HF (10) ,KAL (20) ,THER (50)	GAMM	54
	3,SUCG (20)	GAMM	55
6	EQUIVALENCE	GAMM	56
	1 (7(1000),HER) ,(Z(1030),EMN) ,(Z(1410),FOR)	GAMM	57
	2,(7(1500),HF) ,(Z(1000),KAL) ,(Z(1920),THER)	GAMM	58
	3,(Z(1900),SUCG)	GAMM	59
C		GAMM	60
4	EQUIVALENCE (THER(1),P),(THER(3),T),(THER(8),V)	GAMM	61
C	18 SAVE CENTER VALUES	GAMM	62
6	20 HER(1)=P	GAMM	63
10	30 DEP(2)=V	GAMM	64
12	40 DEP(3)=T	GAMM	65
14	50 DEP(4)=THER(21)	GAMM	66
16	60 E2=EMN(3)	GAMM	67
C	78 MAIN CODE /TEST ARGS.	GAMM	68
C		GAMM	69
20	100 IF (K2) 110,410,110	GAMM	70
21	110 IF (KAL(6)) 200,400,200	GAMM	71
158		GAMM	72
22	200 LM=KAL(6)	GAMM	73
24	210 KAL(6)=0	GAMM	74

25	220	K=1		GAMM	75
26	230	GO TO 1000		GAMM	76
	C 248		SET OUTPUT	GAMM	77
27	200	THEX(26)=SUCG(1)		GAMM	78
31	210	THEX(30)=SUCG(2)		GAMM	79
33	220	THEX(29)=SUCG(4)		GAMM	80
35	230	THEX(28)=SUCG(5)		GAMM	81
37	240	NAL(8)=L4		GAMM	82
41	250	CALL DOUT (4HGAMM,1)		GAMM	83
	C 298		DIFF. AT EQ.COMP.	GAMM	84
46	400	IF (K1)410,600,410		GAMM	85
47	410	K=2		GAMM	86
51	420	GO TO 1000		GAMM	87
	C 498		SET OUTPUT	GAMM	88
51	500	THEX(22)=SUCG(1)		GAMM	89
53	510	THEX(23)=SUCG(2)		GAMM	90
55	520	THEX(24)=SUCG(3)		GAMM	91
57	530	THEX(25)=SUCG(4)		GAMM	92
61	540	THEX(27)=SUCG(5)		GAMM	93
63	550	CALL DOUT (4HGAMM,1)		GAMM	94
	C 598			GAMM	95
70	600	RETURN		GAMM	96
	C 994			GAMM	97
	C 996		DIFFERENCE SUBROUTINE	GAMM	98
	C 998		DELTA P	GAMM	99
71	1000	P=FER(13)*DER(1)		GAMM	100
73	1010	T=DER(3)		GAMM	101
75	1010	CALL MES		GAMM	102
100	1020	DER(5)=V		GAMM	103
102	1030	P=DER(1)/FOR(13)		GAMM	104
104	1040	CALL MES		GAMM	105
107	1050	DER(6)=V		GAMM	106
111	1060	SUCG(6)=-2.0*ALOG(FCB(13)/ALOG(DER(5)/DER(6)))		GAMM	107
	C1096			GAMM	108
	C1098		DELTA T	GAMM	109
124	1100	P=DER(1)		GAMM	110
125	1104	T=DER(3)*(1.0+FOR(14))		GAMM	111
131	1110	CALL MES		GAMM	112
134	1120	DER(5)=V		GAMM	113
136	1120	DER(7)=T*DER(17)*TEMPN(3)		GAMM	114
141	1130	T=DER(3)*(1.0+FCB(14))		GAMM	115
144	1130	CALL MES		GAMM	116
147	1140	DER(6)=V		GAMM	117
151	1170	DER(8)=T*DER(17)*TEMPN(3)		GAMM	118
154	1180	SUCG(7)=(DER(7)-DER(8))/(2.0*DER(3)*FCB(14)*E2)		GAMM	119
162	1190	SUCG(8)=ALOG(DER(5)/DER(6))/(2.0*DER(3)*FOR(14))		GAMM	120
	C1296			GAMM	121
	C1298		CALC. OUTPUT	GAMM	122
174	1200	I=DER(3)		GAMM	123
176	1202	V=DER(2)		GAMM	124
200	1204	E1=DER(4)*T*SUCG(8)/SUCG(7)		GAMM	125
204	1210	SUCG(1)=SUCG(6)/(1.0-SUCG(6)*E1*T*SUCG(8))		GAMM	126
211	1220	SUCG(3)=1.0/(SUCG(1)*E1)		GAMM	127
214	1230	SUCG(2)=SUCG(1)*SUCG(3)-1.0		GAMM	128
217	1240	SUCG(4)=SQRT(SUCG(1)*DER(1)*DER(2))		GAMM	129
226	1250	SUCG(5)=(V/DE(6))/(SUCG(1)/(SUCG(1)+1.0-DE(2)/DER(1)))		GAMM	130
234	1260	SUCG(5)=SUCG(5)*(-SUCG(1))-1.0		GAMM	131
	C			GAMM	132
242	1400	GO TO (300,500),K		GAMM	133
	C			GAMM	134

250	C	END	GAMM	135
			GAMM	136
		SUBROUTINE PV(ICPY)	PV	2
	C		PV	3
	C	CALCULATE ISOTHERM, ISOCORE, ISENTROPE,	PV	4
	C	OR CONSTANT-ENERGY POINTS	PV	5
	C	AT VALUES OF P IN P1 ARRAY	PV	6
	C	(FIND KAL(8)=1,2,3,4)	PV	7
	C	INPUT	PV	8
	C	SUC(1), (2) = TC, PC (INITIAL POINT)	PV	9
	C	KAL(1), KAL(2) = DIFF SWITCHES	PV	10
	C	KAL(8) = 1,2,3,4 FOR CONSTANT T,V,S,E	PV	11
	C	PT = PRESSURE TABLE	PV	12
	C	OUTPUT	PV	13
	C	PRINTED POINT OUTPUT	PV	14
	C	-----	PV	15
	C	REVISION 1, LEAVE P CORRECT ON EXIT	PV	16
	C	FOR RESTART OPTION	PV	17
	C	W. F. 3/1/66	PV	18
	C		PV	19
	C	PV	PV	20
			PV	21
3		COMMON Z(4000)	PV	22
3		DIMENSION	PV	23
		1 KAL (20) ,KEN (60) ,PT (50)	PV	24
		2,SUC (20) ,THER (50)	PV	25
3		EQUIVALENCE	PV	26
		1 (7(1600),KAL) ,(Z(1620),KEN) ,(Z(1750),PT)	PV	27
		2,(Z(1880),SUC) ,(Z(1920),THER)	PV	28
	C		PV	29
3		EQUIVALENCE (THER(1),P),(THER(3),T)	PV	30
3		EQUIVALENCE (THER(8),V),(THER(9),F),(THER(13),S)	PV	31
	C		PV	32
3		8 KEN(16)=0	PV	33
	C		PV	34
4		12 CALL POUT (1)	PV	35
7		14 T=SUC(1)	PV	36
11		16 F=SUC(2)	PV	37
13		40 CALL MES	PV	38
15		50 CALL POUT(2)	PV	39
21		55 SUC(3)=V	PV	40
22		56 SUC(4)=S	PV	41
24		57 SUC(5)=F	PV	42
26		60 IF (KAL(1)+KAL(2)) 70,112,70	PV	43
30		70 CALL GAMM (KAL(1),KAL(2))	PV	44
34		90 CALL POUT(3)	PV	45
37		112 I=1	PV	46
40		114 IF (PT(I)) 200,200,116	PV	47
42		116 F=PT(I)	PV	48
44		120 CALL MESG (KAL(8),SUC)	PV	49
50		122 CALL POUT(2)	PV	50
53		124 IF (KAL(1)+KAL(2)) 130,140,130	PV	51
55		130 CALL GAMM (KAL(1),KAL(2))	PV	52
61		134 CALL POUT(3)	PV	53
64		140 I=I+1	PV	54
66		142 GO TO 114	PV	55
67		200 RETURN	PV	56
70		END	PV	57

C	SUBROUTINE TEN	TEL	2
C	DETONATION HUGONIOT CONTROL	TEL	3
C	CALCULATE DEL, HUG. POINTS AT P VALUES	TEL	4
C	FOUND IN PT ARRAY	TEL	5
C		TEL	6
C	INPUT	TEL	7
C	KAL(1), KAL(2) - DIFF SWITCHES	TEL	8
C	PT - PRESSURE TABLE	TEL	9
C	OUTPUT	TEL	10
C	PRINTED POINT OUTPUT	TEL	11
C	-----	TEL	12
C		TEL	13
C	REVISION 1. LEAVE P CORRECT ON EXIT	TEL	14
C	FOR RESTART OPTION	TEL	15
C	W. F. 3/1/62	TEL	16
C		TEL	17
C	TEN	TEL	18
C		TEL	19
1	COMMON 7(4000)	TEL	20
1	DIMENSION	TEL	21
	1 KAL (20) ,PT (50)	TEL	22
	2, THER (50)	TEL	23
1	EQUIVALENCE	TEL	24
	1 (7(1600), KAL) , (2(1/50), PT)	TEL	25
	2 , (2(1920), THER)	TEL	26
C		TEL	27
1	EQUIVALENCE (THER(1), P)	TEL	28
C		TEL	29
C	SET GUESS ON FIRST ENTRY	TEL	30
1	12 CALL POUT(1)	TEL	31
3	20 I=1	TEL	32
4	30 IF (PT(I)) 200, 200, 40	TEL	33
6	40 P=PT(I)	TEL	34
10	50 I=I+1	TEL	35
12	60 CALL HUG	TEL	36
13	70 CALL POUT(2)	TEL	37
15	80 IF (KAL(1)+KAL(2)) 100, 30, 100	TEL	38
17	100 CALL GAMM (KAL(1), KAL(2))	TEL	39
22	150 CALL POUT(3)	TEL	40
24	180 GO TO 30	TEL	41
25	200 RETURN	TEL	42
C		TEL	43
26	END	TEL	44
		TEL	45
C	SUBROUTINE C.I	CJ	2
C	CALCULATE CJ LOCUS AT VALUES OF RHO ZERO	CJ	3
C	IN ROT TABLE	CJ	4
C		CJ	5
C	ITERATE ON P ALONG HUGONIOT UNTIL	CJ	6
C	CJ CONDITION IS SATISFIED	CJ	7
C	INPUT	CJ	8
C	KAL(1), KAL(2) - DIFF SWITCHES	CJ	9
C	ROT - INITIAL-DENSITY TABLE	CJ	10
C	OUTPUT	CJ	11
C	PRINTED POINT OUTPUT	CJ	12
C	-----	CJ	13
		CJ	14

C	CONST. V DEL. P CALCD FROM Q, GAMMA	CJ	15
C	* F. 11/21/61	CJ	16
C		CJ	17
C	REVISION 2. SAVE INITIAL E FOR INTEGRAL PDV	CJ	18
C	* F. 1/3/62	CJ	19
C		CJ	20
C		CJ	21
C	CJ	CJ	22
1	COMMON 7(4000)	CJ	23
1	DIMENSION	CJ	24
	1 CAR (10, 8), HE (10), KAL (20)	CJ	25
	2, KON (6, 10), RUT (20), THER (50)	CJ	26
	3, KEN(60)	CJ	27
1	DIMENSION CC(10), KCC(2)	CJ	28
1	EQUIVALENCE	CJ	29
	1 (7(120), CAR) , (2(1590), HE) , (2(1600), KAL)	CJ	30
	2, (7(1690), KON) , (2(1800), RUT) , (2(1920), THER)	CJ	31
	3, (7(1620), KEN)	CJ	32
C		CJ	33
C		CJ	34
1	EQUIVALENCE (CAR(1), CC), (CC(8), KCC)	CJ	35
1	EQUIVALENCE (HE(6), V0), (HE(2), P0), (HE(1), RHO)	CJ	36
1	EQUIVALENCE (THER(1), P), (THER(22), GAM), (THER(26), GAM0)	CJ	37
1	EQUIVALENCE (THER(6), V)	CJ	38
1	EQUIVALENCE (THER(6), Q)	CJ	39
1	6 KEN(15)=0	CJ	40
1	8 KEN(16)=0	CJ	41
2		CJ	42
C	10 Q=Q+E INPUT, OUTPUT LABEL	CJ	43
3	30 CALL POUT(1)	CJ	44
5	40 I=1	CJ	45
C	50 H1+E SET UP FROOTT	CJ	46
6	60 R=0=RQT(1)	CJ	47
10	65 HE(1)=RHO	CJ	48
12	70 V=1./RHO	CJ	49
14	72 IF(P) 80, 74, 80	CJ	50
15	74 P=0.3	CJ	51
17	80 CC(4)=P	CJ	52
21	100 KCC(1)=0	CJ	53
C	110 W(G2, G3, G4, G5) FROOTT	CJ	54
22	120 CALL FROOTT(CC, KON (1,8))	CJ	55
25	130 KEXIT=KCC(2)	CJ	56
27	140 GO TO (365, 200, 180, 160), KEXIT	CJ	57
C	150 H5+0 FROOT ERROR EXIT 1	CJ	58
37	160 CALL DBUG (2H0J, 1)	CJ	59
42	170 GO TO 365	CJ	60
43	180 CALL DBUG (2H0J, 1)	CJ	61
46	190 GO TO 365	CJ	62
47	200 IF (KON(1,8)) 260, 204, 260	CJ	63
50	204 IF (KCC(1)-2) 260, 210, 260	CJ	64
52	210 E1=GAM	CJ	65
54	220 IF (GAP) 240, 230, 240	CJ	66
55	230 E1=GAM0	CJ	67
57	240 E2=V*E1/(E1+1.0-P0/P)	CJ	68
64	250 CC(2)=P*(V/E2)*E1	CJ	69
C		CJ	70
72	260 IF (KCC(1)-2) 280, 280, 262	CJ	71
75	262 E1=GAM	CJ	72
77	284 IF (GAP) 268, 266, 266	CJ	73
100	266 E1=GAM0	CJ	74

Line	Code	Statement	Column	Page
1		DIMENSION	28	
1		HS (40), CASH (10), COUNT (20)	29	
2		EM (20), F (20), F (20)	30	
3		FLAH (12), F (10), ME (10)	31	
4		KAL (20), KIM (10), KUN (10)	32	
5		PT (50), RUT (20), SUC (20)	33	
6		THEM (40)	34	
1		EQUIVALENCE	35	
1		((40), HS) , ((40), CASH) , ((40), COUNT)	36	
2		((10), EM) , ((10), F) , ((10), F)	37	
3		((10), FLAH) , ((10), F) , ((10), ME)	38	
4		((10), KAL) , ((10), KIM) , ((10), KUN)	39	
5		((10), PT) , ((10), RUT) , ((10), SUC)	40	
6		((10), THEM)	41	
C		***** LOCALS *****	42	
1		LOGICAL	43	
1		EM (20), F (12)	44	
2		EQUIVALENCE (KIM(2), KS)	45	
3		EQUIVALENCE (HS(27), BLANK), (HS(38), FURN), (HS(39), HCCN)	46	
4		EQUIVALENCE (HS(21), CPAS), (HS(36), END)	47	
5		EQUIVALENCE (HS(24), HCDRE), (HS(27), HUBUG)	48	
6		EQUIVALENCE (HS(33), DULLAN)	49	
7		EQUIVALENCE (HS(35), HREAN)	50	
8		EQUIVALENCE (E(1), CW1), (E(2), CW)	51	
C			52	
1		EQUIVALENCE (FLAH(1), HUNLH), (FLAH(13), MELAH)	53	
2		EQUIVALENCE (FLAH(26), CURLH), (FLAH(37), SPELH)	54	
C			55	
1		EQUIVALENCE (THEM(1), P), (THEM(3), T)	56	
2		EQUIVALENCE (KON(6), WERHGT)	57	
C			58	
1		DIMENSION R.LAH(12), MELAH(12), CURLH(12), SPELH(12)	59	
C		***** EXECUTE *****	60	
1		IF (ACCN.F. 0) GO TO 70	61	
C		----- 1. SCAN TO REWD -----	62	
4		20 CALL FID (3PIT, 4H(1246), 12, E, 0)	63	
10		IF (ME(CURHEND)) GO TO 20	64	
C		----- 2. BEGIN RUN -----	65	
15		70 CONTINUE	66	
15		WERHGT=1.	67	
16		80 CALL FID (3PIT, 13H(246, 6410, Ad), 9, E, 0)	68	
21		90 CALL FID (3PIT, 14H(1440, 6410, Ad), 9, E, 0)	69	
27		IF (ME(CURHEND))	70	
		1 CALL ERR(3LCON, 14LHAD INPUT PACK, E)	71	
C			72	
C		SEARCH FOR CUN BRANCH	73	
41		8700 GO TO 20 I=1, 76	74	
42		8710 IF (CUN(I)) 8370, 8350, 8320	75	
C			76	
C			77	
45		8720 CONTINUE	78	
47		CALL ERR(3HCON, 13H840 CUN CARD, E)	79	
C			80	
51		8730 GO TO (100, 200, 300, 400, 500, 600	81	
		1, 700, 800, 900, 1000, 1100, 1200	82	
		2, 1300, 1400, 1500, 1600, 1700, 1800	83	
		3, 1900, 2000, 2100, 2200, 2300, 2400	84	
		4, 2500, 2600, 2700, 2800, 2900, 3000	85	
		5, 3100, 3200, 3300, 3400, 3500, 3600), I	86	
C			87	

123	C	100 GO TO H1	CUN	88
124	C	108	CUN	89
	C	PAS	CUN	90
	C	ZERO COMMON	CUN	91
124	C	200 CONTINUE	CUN	92
	C	ZERO COMMON	CUN	93
124	C	210 I=1,2900	CUN	94
131	C	210 CONT(I)=1.0	CUN	95
133	C	CALL HEADIT(F(3))	CUN	96
135	C	CALL HEADIT9LBEIGIN KUN)	CUN	97
	C		CUN	98
141	C	220 GO 222 I=1,96	CUN	99
143	C	222 FLA(I)=0.0	CUN	100
147	C	224 GO 240 I=1,10	CUN	101
151	C	220 SUMLAH(I)=E(1+2)	CUN	102
156	C	GO TO 20	CUN	103
	C		CUN	104
156	C	200 CONTINUE	CUN	105
156	C	CALL HEADIT	CUN	106
	C	1501 DIFF. FX DIFF. GAS, SOLID, MIX, EQ, CU, PV	CUN	107
	C	21 = (2, KE)	CUN	108
162	C	202 GO 208 I=1,12	CUN	109
164	C	204 IF (ISIG(I,KE(1))) 308,306,305	CUN	110
170	C	206 CALL I)=F(I)	CUN	111
172	C	208 CONTINUE	CUN	112
174	C	210 GO TO H1	CUN	113
	C		CUN	114
175	C	400 CALL HEADIT	CUN	115
	C	10L*. FRUIT EPS(CG,CM,CM,CG,CS,C)/ RADIUS/ UP,UT,EPSTN,CUI/ FRUIT	CUN	116
	C	2 BOLDUS	CUN	117
	C	2 F(I)	CUN	118
201	C	410 GO 420 I=1,7	CUN	119
211	C	420 CAH(I)=F(I)	CUN	120
214	C	430 GO TO H1	CUN	121
215	C	500 GO TO H1	CUN	122
	C		CUN	123
216	C	600 KUN(I)=	CUN	124
217	C	610 CALL UIMP1	CUN	125
221	C	620 GO TO H1	CUN	126
	C		CUN	127
222	C	700 CALL HEADIT (.,-7,KE)	CUN	128
224	C	710 GO 720 I=1,7	CUN	129
234	C	720 KUN(I,KE)=KE(I+1)	CUN	130
237	C	730 GO TO H1	CUN	131
	C		CUN	132
240	C	800 CALL HEADIT (.,-1,KE)	CUN	133
244	C	820 KUN(KE,4)=1	CUN	134
246	C	830 CALL HEADIT (0.3,CAH(5,KE))	CUN	135
254	C	840 GO TO H1	CUN	136
	C		CUN	137
255	C	900 GO TO H1	CUN	138
	C		CUN	139
256	C	1000 CALL GEN(1)	CUN	140
261	C	1010 GO TO H1	CUN	141
	C		CUN	142
262	C	1100 CALL SEM(1,1)	CUN	143
266	C	1110 GO TO H1	CUN	144
	C		CUN	145
267	C	1200 CALL TIM(1)	CUN	146
272	C	1210 GO TO H1	CUN	147

	C1298	XIP	CUN	148
273	1300 CALL XI:1 (1,0)		CUN	149
277	1310 GO TO B7		CUN	150
	C1298	EQ	CUN	151
300	1400 CALL EQP		CUN	152
302	1410 GO TO B8		CUN	153
	C1498	EMPTY	CUN	154
303	1500 GO TO B80		CUN	155
	C1598	SAM	CUN	156
304	1400 CALL HEAD(1)LSAM = INPUT PART 2)		CUN	157
306	CALL REAP (33H KS/ RHO, MO, 10, MO+ MFE/ NI S, -1, KS)		CUN	158
311	CALL REAP(0,5,HE)		CUN	159
314	CALL REAP(0,KS,PN)		CUN	160
320	1410 HE(1)=1.1/HE(1)		CUN	161
322	1420 HE(7)=HE(5)PCONT(4)/HE(4)		CUN	162
325	1430 EMN(2)=F(1)		CUN	163
327	1432 EMN(3)=0.1		CUN	164
330	1434 GO 1436 I=1,KS		CUN	165
334	1436 EMN(3)=EMN(1)+FN(I)		CUN	166
337	1440 EMN(1)=FN(7)-EMN(2)		CUN	167
341	1442 EMN(4)=EMN(1)/EMN(3)		CUN	168
343	1444 EMN(5)=FN(2)/EMN(3)		CUN	169
345	1450 GO 1452 I=1,KS		CUN	170
353	1452 EMX(1)=FN(1)/EMN(1)		CUN	171
	C		CUN	172
356	1460 GO 1462 I=1,10		CUN	173
363	1462 MELAB(I)=E(I+2)		CUN	174
365	1470 GO TO B8		CUN	175
	C1498	TEO	CUN	176
376	1700 CALL HEAD(14)TEO = HUGONIUT)		CUN	177
379	CALL REAP (11H P=TABLE S, 0, PT)		CUN	178
	C		CUN	179
374	1710 CALL TEO		CUN	180
376	1720 GO TO B7		CUN	181
	C1798	PV	CUN	182
377	1800 CALL HEAD(ELLOCUS)		CUN	183
401	CALL REAP(CUN	184
	150.1 BR3:CH (1-T,2-V,3-S,4-E) / TC,PC/ P-TABLE S		CUN	185
	2, -2,KAL(2))		CUN	186
404	CALL REAP(0,2,SUC)		CUN	187
407	CALL REAP(0,0,PT)		CUN	188
	C		CUN	189
	C		CUN	190
413	1850 IF(KAL(9)) 1852,1860,1852		CUN	191
414	1852 SUC(1)=T		CUN	192
416	1854 SUC(2)=V		CUN	193
	C		CUN	194
420	1900 CONTINUE		CUN	195
421	CALL PV		CUN	196
422	1970 GO TO B8		CUN	197
	C1898	CJ	CUN	198
423	1900 CALL HEAD(2)LCJ)		CUN	199
425	CALL REAP (16H CJ RHO-TABLE S, 0, RUT)		CUN	200
	C		CUN	201
431	1910 CALL CJ		CUN	202
433	1920 GO TO B1		CUN	203
	C1898	TEST	CUN	204
434	2000 CALL TEST		CUN	205
436	2010 GO TO B8		CUN	206
	C2098	CHEC	CUN	207

437	2100	CALL CHEC		CUN	208
441	2110	GO TO 80		CUN	209
	C2198		EMPTY	CUN	210
442	2200	GO TO 80		CUN	211
	C2298		SPEC	CUN	212
443	2300	CALL SPEC		CUN	213
445	2310	GO TO 80		CUN	214
	C2398		SPEC1	CUN	215
446	2400	CALL SPFC1		CUN	216
450	2410	GO TO 80		CUN	217
	C2498		EMPTYIES	CUN	218
451	2500	GO TO 80		CUN	219
	C		CORE	CUN	220
452	2600	E(2)=E(4)		CUN	221
454	2610	E(1)=E(5)		CUN	222
456	2620	CALL CORE (E(3))		CUN	223
461	2630	GO TO 80		CUN	224
	C2698		DEBUG	CUN	225
462	2700	CALL ERP(4HCONS)		CUN	226
465	2710	GO TO 80		CUN	227
	C2798		LOAD	CUN	228
466	2800	GO TO 80		CUN	229
	C2898		EMPTYIES	CUN	230
467	2900	GO TO 80		CUN	231
470	3000	GO TO 80		CUN	232
471	3100	GO TO 80		CUN	233
472	3200	GO TO 80		CUN	234
473	3300	GO TO 80		CUN	235
	C		FORM	CUN	236
474	3400	CALL FIO (3HWOT,4H(A6),1,E(3),0)		CUN	237
502	3610	POL=E(4)-HLANK		CUN	238
504	3620	IF (POL) 3430,3440,3430		CUN	239
505	3630	CALL FIO (5HPRINT,4H(A6),1,E(3),0)		CUN	240
	C			CUN	241
513	3640	IF (E(6)-DOLLAR) 3470,3450,3470		CUN	242
515	3650	DO 3460 I=1,6		CUN	243
522	3660	SPELAB(I)=E(I+6)		CUN	244
524	3670	GO TO 80		CUN	245
	C			CUN	246
	C			CUN	247
	C		REND - END OF RUN	CUN	248
525	3500	GO TO 80		CUN	249
	C		JEND - END OF JOB	CUN	250
526	3600	CONTINUE		CUN	251
526		CALL MEANE (7HJOHENOS)		CUN	252
530		CALL EXIT		CUN	253
532	4000	RETURN		CUN	254
	C			CUN	255
	C		LOAD BUTTON	CUN	256
	C			CUN	257
	C			CUN	258
	C			CUN	259
533		END		CUN	260
	C	*****		EQPS	2
	C	6. OUT OF PLACE		EQPS	3
	C	*****		EQPS	4
	C	*****		EQPS	5
	C	BRTAKLEY-METHOD EQUILIBRIUM-COMPOSITION PKG.		EQPS	6
	C	TRANSCRIBED TO FORTRAN BY PAUL BIRD, GMX-7,		EQPS	7
	C	FROM TICKETT'S ORIGINAL LONGHAND VERSION.		EQPS	8

C	NOTES -	EQPS	9
C	1. CHANGES WHEN INCORPORATED INTO REVISED MES	EQPS	10
C	(MARKED KERSHNER 3/17/76)	EQPS	11
C	A. MAKE AVECT LOCAL, FILLED FROM ARGUS EPA, EPA1,	EQPS	12
C	IN EQPS	EQPS	13
C	9. EMUL(12) REPLACED BY EMUL(7), IN EDMS	EQPS	14
C	*****	EQPS	15
	SUBROUTINE EQPS(KHP,CSP,QATOM,ALPHA,ALPHA12,EPA,EPA1)	EQPS	16
C		EQPS	17
C		EQPS	18
17	1 ALPT(6,101),KHP(2)	EQPS	19
17	1 ALPT(6,101),KHP(2)	EQPS	20
17	1 ALPT(6,101),KHP(2)	EQPS	21
17	1 ALPT(6,101),KHP(2)	EQPS	22
17	1 ALPT(6,101),KHP(2)	EQPS	23
C	COMMON /E:/QBAR,NAVEC,XNUMAT,XNU,SUMQ,NS,NC,ND,NP,NPHI,ND1,	EQPS	24
17	1 QBAR,NAVEC,XNUMAT,XNU,SUMQ	EQPS	25
C		EQPS	26
C		EQPS	27
C		EQPS	28
C	*****	EQPS	29
C	MAKE AVECT LOCAL. KERSHNER 3/17/76	EQPS	30
C	*****	EQPS	31
17	DO 12 I=1,20	EQPS	32
24	AVECT(I,1)=EPA(I)	EQPS	33
24	AVECT(I,2)=EPA1(I)	EQPS	34
24	12 CONTINUE	EQPS	35
C	DEFINE CONTROL CONSTANTS AND REORDER ALPHA ACCORDING TO A-VECTOR	EQPS	36
33	NC=CSP(1)	EQPS	37
33	NS=CSP(2)	EQPS	38
33	NPHI=CSP(4)	EQPS	39
33	ND=NS-NC	EQPS	40
33	ND)=ND+1	EQPS	41
33	NPHI1=NPHI+1	EQPS	42
45	IF(NPHI1.EQ.1.AND.KHP.EQ.0)GO TO 30	EQPS	43
52	NP=CSP(3)	EQPS	44
54	13 KV=1	EQPS	45
55	14 NCMP=NC-NP	EQPS	46
57	IF(NCMP.LE.0)CALL DBUG(2)	EQPS	47
62	DO 1 I=1,NS	EQPS	48
73	NAVEC(I)=AVECT(I,KV)	EQPS	49
73	NAV=NAVEC(I)	EQPS	50
74	DO 1 J=1,NC	EQPS	51
111	1 ALPHA(NV,J)=ALPHA(I,J)	EQPS	52
122	DO 2 J=1,NC	EQPS	53
131	2 ALPHA(NS+1,J)=QATOM(J)	EQPS	54
133	CALL MATTRA(NS+1,NC,ALPHA,101,ALPT,6)	EQPS	55
C	TRANSPOSE ALPHA MATRIX	EQPS	56
C	SOLVE FOR IN-MATRIX	EQPS	57
141	CALL LSS(NC,ND1,6,ALPT,ALPT(1,NC+1),DET)	EQPS	58
C	TEST FOR ZERO DETERMINANT, EXIT FOR NEW A-VECTOR	EQPS	59
151	IF(DET.EQ.0.0)CALL DBUG(2)	EQPS	60
C	TRANSPOSE FOR NG-MATRIX AND SMALL Q	EQPS	61
157	CALL MATTRA(NC,ND+1,ALPT(1,NC+1),6,XNUMAT,100)	EQPS	62
175	SUMQ=0.0	EQPS	63
175	DO 3 J=1,NCMP	EQPS	64
211	3 SUMQ=SUMQ+XNUMAT(ND+1,J)	EQPS	65
214	DO 4 J=1,NC	EQPS	66

232	4	QBAR(J)=XNUMAT(ND+1,J)/SUMQ	EQPS	67
234		DO 5 I=1,ND	EQPS	68
241		ANU(I)=0.0	FQPS	69
243		DO 5 J=1,NCMP	FQPS	70
252	5	ANU(I)=XNU(I)*XNUMAT(I,J)	EQPS	71
	C	PRINT NU=MATRIX AND QBAR	EQPS	72
263		WRITE(9,6)(QBAR(J),J=1,NCMP)	EQPS	73
271		WRITE(9,7)(XNUMAT(1,J),J=1,NC)	EQPS	74
	6	FORMAT(1H0,5X,4H0,5X,6E15.7)	EQPS	75
	7	FORMAT(1H0,5X,6H0,5X,3X,6E15.7)	FQPS	76
	8	FORMAT(10X,13,2X,6E15.7)	EQPS	77
		IF(ND.LE.1)GO TO 90	FQPS	78
317		DO 9 I=2,ND	EQPS	79
321	9	WRITE(9,8)I,(XNUMAT(I,J),J=1,NC)	FQPS	80
323		GO TO (10,15),NPH11	EQPS	81
352	10	IF(NPH1.EQ.1.AND.NP.EQ.1)GO TO 11	FQPS	82
360		RETURN	FQPS	83
367	11	NP=0	EQPS	84
370		KV=2	EQPS	85
372		GO TO 14	FQPS	86
373	15	GO TO (16,10),KFLAG	EQPS	87
401	16	DO 17 I=1,ND	EQPS	88
403		ANUS(I)=XNU(I)	EQPS	89
405		DO 17 J=1,NC	FQPS	90
415	17	ANUS(I,J)=XNUMAT(I,J)	FQPS	91
425		ANUS(ND1)=NP	FQPS	92
430		DO 18 I=1,NS	EQPS	93
435	18	NAVECS(I)=NAVEC(I)	EQPS	94
437		SUMUS=SUMU	FQPS	95
440		DO 19 J=1,NC	FQPS	96
451	19	QBAR(J)=QBAR(J)	FQPS	97
453		KFLAG=2	EQPS	98
454		GO TO (20,21),NPS	FQPS	99
465	20	NP=0	FQPS	100
465		KV=2	FQPS	101
467		GO TO 22	FQPS	102
470	21	NP=1	EQPS	103
470		KV=1	FQPS	104
472	22	AN.(ND1)=NP	FQPS	105
475		GO TO 14	EQPS	106
475	30	NP=COMP(5)	FQPS	107
475		NPS=NP+1	FQPS	108
501		GO TO (31,33),NPS	FQPS	109
506	31	NP=1	EQPS	110
506		KV=1	EQPS	111
510	32	KFLAG=1	FQPS	112
511		GO TO 14	FQPS	113
512	33	NP=0	FQPS	114
512		KV=2	FQPS	115
514		GO TO 32	EQPS	116
515		END	EQPS	117
		SUBROUTINE EOMS(KBERR,XCOMP,EMOL,PDAG)	FQPS	2
C			EQPS	3
C			EQPS	4
		DATA ITERCYC,EXPLIM,EPSILON/99,600.,.1.0E-10/	EQPS	5
C			EQPS	6
12		DIMENSION XCOMP(100),EMOL(7),PDAG(100)	EQPS	7
		C*****	EQPS	8

C	EMCL(2) REPLACED BY EMCL(7). 2/10/76	FUMS	9
C	*****	FUMS	10
12	DIMENSION XLNKI(100),RXCOMP(100),RFDAG(100),XLNXJ(6),A(6,6),F(6),	EUMS	11
	IM(6)	FUMS	12
12	DIMENSION QBAR(6),NAVEC(100),XNUMAT(100,6),XNU(100),	FUMS	13
	QBARIS(6),NAVECS(100),XNUMATS(100,6),XNUS(100)	EUMS	14
C		EUMS	15
12	EQUIVALENCE (F,M)	FUMS	16
C		FUMS	17
12	COMMON /EQUIH/QBAR,NAVEC,XNUMAT,XNU,SUMQ,NS,NC,ND,NP,NPHI,ND1,	EUMS	18
	QBARIS,NAVECS,XNUMATS,XNUS,SUMQS	FUMS	19
C		FUMS	20
C		FUMS	21
C	SET CONSTANTS	FUMS	22
12	1000 NPHLAG=1	EUMS	23
13	1001 ITERCO=0	FUMS	24
13	NCMP=NC-10	FUMS	25
C	REORDER MOLE FRACTIONS AND FREE ENERGIES	FUMS	26
16	DO 1 I=1,NS	EUMS	27
23	NAV=NAVEC(I)	EUMS	28
23	RXCOMP(NAV)=XCOMP(I)	FUMS	29
23	1 RFDAG(NAV)=FIDAG(I)	EUMS	30
30	IF(NPHI.EQ.1.AND.NP.EQ.0)RFDAG(NS)=EXPLIM	EUMS	31
C	CALCULATE LNKI	FUMS	32
43	DO 2 I=1,ND	EUMS	33
45	XLNKI(I)=-RFDAG(I+NC)	FUMS	34
50	DO 2 J=1,NC	EUMS	35
57	2 XLNKI(I)=XLNKI(I)+XNUMAT(I,J)*RFDAG(J)	FUMS	36
C		EUMS	37
C	CALCULATE LN XJ	EUMS	38
67	3 DO 4 J=1,NCMP	FUMS	39
71	4 XLNXJ(J)=ALOG(RXCOMP(J))	EUMS	40
C	CALCULATE MOLE FRACTIONS OF DEPENDENT SPECIES	EUMS	41
102	DO 4 I=1,ND	EUMS	42
103	XLNXI=XLNKI(I)	FUMS	43
105	DO 5 J=1,NCMP	EUMS	44
115	5 XLNXI=XLNXI+XNUMAT(I,J)*XLNXJ(J)	EUMS	45
120	IF(XLNXT.GT.0.0)XLNXI=0.0	EUMS	46
125	IF(XLNXI.LT.-EXPLIM)XLNXI=-EXPLIM	EUMS	47
131	6 RXCOMP(I+NC)=EXP(XLNXI)	FUMS	48
C	SET UP ITERATION LOOP	FUMS	49
143	IF(ITERCO.EQ.0)GO TO 11	EUMS	50
144	IF(ITERCO.GT.ITERCYC)GO TO 20	EUMS	51
C	TEST FOR CONVERGENCE	FUMS	52
147	DO 7 J=1,NCMP	FUMS	53
150	IF(ABS(H(J)).GT.EPSILON)GO TO 11	FUMS	54
155	7 CONTINUE	EUMS	55
C	PASS TO CONVERGENCE TEST	EUMS	56
C		EUMS	57
C	CALCULATE NUMBER OF MOLES	FUMS	58
157	RNCH=1.0	EUMS	59
163	DO 8 I=1,ND	EUMS	60
170	8 RNCH=RNCH-RXCOMP(I+NC)*(XNU(I)-1.0)	EUMS	61
176	EMOL(1)=5000/RNCH	FUMS	62
C	CALCULATE XC AND MOLES OF SOLID FOR NP=1	EUMS	63
176	EMOL(2)=0.0	FUMS	64
201	IF(NP.NE.1)GO TO 81	FUMS	65
203	XC=QBAR(NC)	EUMS	66
205	DO 80 I=1,NC	FUMS	67
220	80 XC=XC-(XNUMAT(I,NC)-QBAR(NC)*(XNU(I)-1.0))*RXCOMP(I+NC)	EUMS	68

231	RXCOMP(NC)=XC	FUMS	69
231	EMOL(2)=(C*EMOL(1)	EQMS	70
	C RESTORE MOLE FRACTION ORDER	FUMS	71
234	81 DO 9 I=1,NS	FUMS	72
243	NAV=NAVEG(I)	FUMS	73
243	9 XCOMP(I)=XCOMP(NAV)	FUMS	74
247	IF(NPHI.EQ.1)GO TO 42	FUMS	75
	C EXIT WITH COMPUTED EQUILIBRIUM COMPOSITION	FUMS	76
253	10 RETURN	FUMS	77
	C	FUMS	78
	C ENTRY TO CALCULATE CORRECTIONS TO MOLE FRACTIONS	FUMS	79
254	11 DO 13 J=1,NCMP	FUMS	80
256	SUMF=0.0	FUMS	81
257	DO 12 I=1,NC	EQMS	82
272	12 SUMF=SUMF+(XNUMAT(I,J)-GBAR(J)*(XNU(I)-1.0))*RXCOMP(I+NC)	EQMS	83
303	13 F(J)=GBAR(J)-RXCOMP(J)-SUMF	EQMS	84
311	DO 14 J=1,NCMP	FUMS	85
313	DO 14 JP=1,NCMP	EQMS	86
314	A(I,JP)=0.0	FUMS	87
317	IF(J.EQ.JP)A(J,JP)=RXCOMP(J)	EQMS	88
322	DO 14 I=1,NC	FUMS	89
340	14 A(I,JP)=A(J,JP)+(XNUMAT(I,J)-GBAR(J)*(XNU(I)-1.0))*RXCOMP(I+NC)*	EQMS	90
	1XNUMAT(I,JP)	FUMS	91
357	CALL LSS(XCOMP,1.6,A,F,DET)	EQMS	92
363	IF (DET.EQ.0.0)GO TO 20	FUMS	93
367	DO 17 J=1,NCMP	FUMS	94
370	RXCOMP(J)=RXCOMP(J)*(1.0+F(J))	FUMS	95
373	IF (RXCOMP(J).LT.EPSILON)RXCOMP(J)=EPSILON	EQMS	96
377	17 CONTINUE	FUMS	97
402	ITERCC=ITERCC+1	EQMS	98
403	GO TO 3	FUMS	99
404	20 CALL DBUR(1)	FUMS	100
406	GO TO 1000	FUMS	101
	C TEST FOR PREVIOUS SOLUTION FOR PHI = 1	FUMS	102
411	21 IF (NPHI.EQ.2)GO TO 10	FUMS	103
414	IF (NP.EQ.1)GO TO 40	FUMS	104
	C CALIBRATION TEST FOR 1-PHASE SOLUTION	FUMS	105
	C SELECT NON-ZERO ELEMENTS OF 2-PHASE NU	FUMS	106
416	DO 50 I=1,NC	EQMS	107
417	IF (XNUMATS(I,NC).NE.0.0)GO TO 51	FUMS	108
422	50 CONTINUE	FUMS	109
424	CALL DBUR(2)	FUMS	110
	C LOCATED SPECIES FORMED FROM SOLID	FUMS	111
430	51 ISP=1	EQMS	112
432	DO 52 I=1,NS	EQMS	113
437	NAV=NAVEG(I)	FUMS	114
437	RXCOMP(NAV)=XCOMP(I)	EQMS	115
437	52 REFUAG(1)=FIDAG(1)	EQMS	116
444	ZLNK1=-FIDAG(ISP+NC)	FUMS	117
447	DO 53 J=1,NC	EQMS	118
462	53 ZLNK1=ZLNK1+XNUMATS(ISP,J)*REFUAG(J)	EQMS	119
465	ALNS=ALOG(RXCOMP(ISP+NC))-ZLNK1	FUMS	120
472	NCM1=NC-1	EQMS	121
474	DO 54 J=1,NCM1	FUMS	122
500	54 ALNS=XLNS-XNUMATS(ISP,J)*ALOG(RXCOMP(J))	FUMS	123
514	EMOL(7)=XLNS	EQMS	124
	C*****	FUMS	125
	C EMOL(7) SFT 2/10/76	EQMS	126
	C*****	FUMS	127
	C TEST FOR SUPERSATURATION	EQMS	128

515	IF (ALNS.LT.0.0)GO TO 10	FQMS	129
	C EXCHANGE FOR 2-PHASE SOLUTION	FQMS	130
	C	FQMS	131
	C EXCHANGE A-VECTORS, ETC., FOR CHANGE IN NUMBER OF PHASES	FQMS	132
515	30 NPHFLAG=2	FQMS	133
517	DO 31 I=1,NI	FQMS	134
521	DO 31 J=1,NC	FQMS	135
535	XNUMSV=XNUMATS(I,J)	FQMS	136
530	XNUMATS(I,J)=XNUMAT(I,J)	FQMS	137
530	31 XNUMAT(I,J)=XNUMSV	FQMS	138
541	DO 32 J=1,NC	FQMS	139
540	QBARSV=QBARS(J)	FQMS	140
540	QBARS(J)=QBAR(J)	FQMS	141
540	32 QBAR(J)=QBARSV	FQMS	142
551	DO 33 I=1,N3	FQMS	143
561	NAV=NAVECS(I)	FQMS	144
561	NAVECS(I)=NAVEC(I)	FQMS	145
561	33 NAV=NAVEC(I)	FQMS	146
564	DO 34 I=1,NBI	FQMS	147
574	ANHSV=ANHS(I)	FQMS	148
574	ANHS(I)=XNU(I)	FQMS	149
574	34 ANH(I)=ANHSV	FQMS	150
577	SUMDSAV=SUMDS	FQMS	151
577	SUMDS=SUMI	FQMS	152
577	SUMC=SUMDSAV	FQMS	153
577	NP=XNU(N1)	FQMS	154
605	GO TO 1001	FQMS	155
	C TEST FOR SATISFACTORY 2-PHASE SOLUTION	FQMS	156
	C 40 IF(XC.GT.0.0)GO TO 10	FQMS	157
	C SIMPL. 40 REPLACED BY THE FOLLOWING TWO STATEMENTS.	FQMS	158
	C KERSHNER 2/10/76	FQMS	159
610	40 EMOL(7)=XC	FQMS	160
612	IF(XC.GT.0.0)GO TO 10	FQMS	161
	C NO SOLID PHASE. GO TO 1-PHASE SOLUTION	FQMS	162
614	GO TO 30	FQMS	163
614	END	FQMS	164
	 SUBROUTINE MATTRA(N,M,A,IA,B,IB)	MATTRA	2
16	DIMENSION A(IA,M),B(IB,N)	MATTRA	3
16	DO 1 J=1,M	MATTRA	4
17	DO 1 I=1,N	MATTRA	5
20	1 B(J,I)=A(I,J)	MATTRA	6
37	RETURN	MATTRA	7
40	END	MATTRA	8
	 SUBROUTINE LSS (N,M,I,A,B,DET)	LSS	2
	C MODIFIED FOR FORTRAN IV HUG	LSS	3
16	DIMENSION A(I,N), B(I,M)	LSS	4
16	DOUBLE PRECISION S1,S2,CU1PRU	LSS	5
16	NN=N	LSS	6
16	MM=M	LSS	7
16	SN=1.	LSS	8
21	DO 9 J=1,NN	LSS	9
23	L=J-1	LSS	10
24	IF (J.EQ.NN) GO TO 7	LSS	11
31	T=ABS(A(J,J))	LSS	12
31	M1=J	LSS	13
31	M2=J+1	LSS	14

34	DO 1 K=M2,NN	LSS	15
35	A=ABS(A(K,J))	LSS	16
41	IF (X,LE,T) GO TO 1	LSS	17
42	I=X	LSS	18
43	M1=K	LSS	19
46 1	CONTINUE	LSS	20
51	IF (M1,EQ,J) GO TO 4	LSS	21
53	DO 2 K=1,MM	LSS	22
63	I=A(J,K)	LSS	23
63	A(I,K)=A(M1,K)	LSS	24
63 2	A(M1,K)=I	LSS	25
67	SN=-SN	LSS	26
70	IF (MM,LE,0) GO TO 4	LSS	27
76	DO 3 K=1,MM	LSS	28
106	I=B(J,K)	LSS	29
106	B(I,K)=B(M1,K)	LSS	30
106 3	B(M1,K)=I	LSS	31
116 4	IF (A(J,J),EQ,0.) GO TO 13	LSS	32
122	DO 6 K=M2,NN	LSS	33
124	S1=0.	LSS	34
124	S2=0.	LSS	35
127	IF (L,EQ,0) GO TO 5	LSS	36
130	S1=OUTPRD(L,A(J,1),I,A(1,K),1)	LSS	37
150 5	A(J,K)=(A(J,K)-S1)/A(J,J)	LSS	38
177	S2=OUTPRD(J,A(K,1),I,A(1,M2),1)	LSS	39
217 6	A(K,M2)=A(K,M2)-S2	LSS	40
232 7	IF (MM,LE,0) GO TO 9	LSS	41
234	IF (A(J,J),EQ,0.) GO TO 13	LSS	42
240	DO 8 K=1,MM	LSS	43
241	S1=0.	LSS	44
242	IF (L,EQ,0) GO TO 8	LSS	45
243	S1=OUTPRD(L,A(J,1),I,B(1,K),1)	LSS	46
263 8	B(I,K)=(B(I,K)-S1)/A(J,J)	LSS	47
315 9	CONTINUE	LSS	48
320	DET=A(1,1)*SN	LSS	49
321	IF (DET,EQ,0.) GO TO 13	LSS	50
322	IF (N,EG,1) GO TO 15	LSS	51
324	DO 10 J=2,NN	LSS	52
332 10	DET=DET*A(J,J)	LSS	53
335	IF (DET,EQ,0.) GO TO 13	LSS	54
341	IF (NN,EG,0) GO TO 15	LSS	55
342	M3=NN-1	LSS	56
344	DO 12 J=1,MM	LSS	57
346	DO 11 L=1,M3	LSS	58
347	M1=NN-L	LSS	59
347	S1=0.	LSS	60
347	M2=M1+1	LSS	61
347	K=NN-M2+1	LSS	62
355	S1=OUTPRD(K,A(M1,M2),I,B(M2,J),1)	LSS	63
374 11	B(M1,J)=B(M1,J)-S1	LSS	64
407 12	CONTINUE	LSS	65
411	GO TO 15	LSS	66
412 13	DET=0.	LSS	67
413 15	RETURN	LSS	68
414	END	LSS	69

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14 DOUBLE FUNCTION OUTPRO(N,X,IX,Y,IY)
14 DIMENSION X(IX,N),Y(IY,N)
14 DOUBLE OX,DY,SUM

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OUTPRO 2
OUTPRO 3
OUTPRO 4

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14	SUM=J.0	DOIPRO	5
15	DO 1 I=1,N	DOIPRO	6
24	UX=X(1,I)	DOIPRO	7
24	UY=Y(1,I)	DOIPRO	8
24	1 SUM=SUM+UX*UY	DOIPRO	9
46	DOTPRG=SUM	DOIPRO	10
50	RETURN	DOIPRO	11
52	END	DOIPRO	12

	SUBROUTINE REAP(LABEL,N,A)	REAP	2
	C*****	REAP	3
	C THIS ROUTINE IS DESIGNED TO READ AND PRINT SPECIFIED	REAP	4
	C ARRAYS.	REAP	5
	C	REAP	6
	C***** KERSHNER 2/13/76	REAP	7
10	10 DIMENSION LABEL(10),A(N)	REAP	8
	C*****	REAP	9
	C FORMAT STATEMENTS.	REAP	10
	C*****	REAP	11
	10 FORMAT(12T6)	REAP	12
	20 FORMAT(6E12.7)	REAP	13
	30 FORMAT(5X.12I8)	REAP	14
	40 FORMAT(5X.1P6E13.5)	REAP	15
	50 FORMAT(2X.1GA10)	REAP	16
10	CALL PRINT (LABEL,0.0)	REAP	17
	C*****	REAP	18
	C THEN BRANCH ON N TO READ AND PRINT ARRAY A.	REAP	19
	C*****	REAP	20
12	12 IF (N)100,110,120	REAP	21
	C*****	REAP	22
	C NEGATIVE N. USE 12I6 FORMAT.	REAP	23
	C*****	REAP	24
15	100 CONTINUE	REAP	25
15	NP=-N	REAP	26
16	READ (10,10) (A(I),I=1,NP)	REAP	27
26	PRINT 10. (A(I),I=1,NP)	REAP	28
40	RETURN	REAP	29
	C*****	REAP	30
	C ZERO N. STOP AFTER READING BLANK FIELD.	REAP	31
	C*****	REAP	32
41	110 CONTINUE	REAP	33
41	J=1	REAP	34
41	K=6	REAP	35
43	120 READ(10,20) (A(I),I=J,K)	REAP	36
55	DO 130 L=J,K	REAP	37
61	IF (A(L).EQ.0.0) GO TO 140	REAP	38
62	130 CONTINUE	REAP	39
64	PRINT 40. (A(I),I=J,K)	REAP	40
75	J=K+1	REAP	41
76	K=K+5	REAP	42
101	GO TO 120	REAP	43
104	140 A(L)=0.0	REAP	44
106	PRINT 40. (A(I),I=J,L)	REAP	45
120	RETURN	REAP	46
	C*****	REAP	47
	C POSITIVE N. USE E12.7 FORMAT.	REAP	48
	C*****	REAP	49
121	150 CONTINUE	REAP	50
121	READ(10,20) (A(I),I=1,N)	REAP	51

14	SUM=0.0	DOIPRO	5
15	DO 1 I=1,N	DOIPRO	6
24	UX=X(1,I)	DOIPRO	7
24	UY=Y(1,I)	DOIPRO	8
24	1 SUM=SUM+UX*DY	DOIPRO	9
45	DOTPRC=SUM	DOIPRO	10
50	RETURN	DOIPRO	11
52	END	DOIPRO	12

	SUBROUTINE REAP(LABEL,N,A)	REAP	2
	C*****	REAP	3
	C THIS ROUTINE IS DESIGNED TO READ AND PRINT SPECIFIED	REAP	4
	C ARRAYS.	REAP	5
	C	REAP	6
	C*****	REAP	7
10	DIMENSION LABEL(10),A(N)	REAP	8
	C*****	REAP	9
	C FORMAT STATEMENTS.	REAP	10
	C*****	REAP	11
	10 FORMAT(1P16)	REAP	12
	20 FORMAT(AE12.7)	REAP	13
	30 FORMAT(5X,1P18)	REAP	14
	40 FORMAT(5X,1P5E13.5)	REAP	15
	50 FORMAT(2X,10A10)	REAP	16
10	CALL PRIN (LABEL,0,0)	REAP	17
	C*****	REAP	18
	C THEN BRANCH ON N TO READ AND PRINT ARRAY A.	REAP	19
	C*****	REAP	20
12	IF (N)100,110,130	REAP	21
	C*****	REAP	22
	C NEGATIVE N, USE 1216 FORMAT.	REAP	23
	C*****	REAP	24
15	100 CONTINUE	REAP	25
15	NP=-N	REAP	26
16	READ (10,10) (A(I),I=1,NP)	REAP	27
26	PRINT 10, (A(I),I=1,NP)	REAP	28
40	RETURN	REAP	29
	C*****	REAP	30
	C ZERO N, STOP AFTER READING BLANK FIELD.	REAP	31
	C*****	REAP	32
41	110 CONTINUE	REAP	33
41	J=1	REAP	34
41	K=1	REAP	35
43	120 READ(10,20) (A(I),I=J,K)	REAP	36
55	DO 130 L=J,K	REAP	37
51	IF (A(L).EQ.0.0) GO TO 140	REAP	38
52	130 CONTINUE	REAP	39
64	PRINT 40, (A(I),I=J,K)	REAP	40
76	J=K+1	REAP	41
76	K=J+1	REAP	42
101	GO TO 120	REAP	43
104	140 A(I)=0.0	REAP	44
106	PRINT 40, (A(I),I=J,L)	REAP	45
120	RETURN	REAP	46
	C*****	REAP	47
	C POSITIVE N, USE E12.7 FORMAT.	REAP	48
	C*****	REAP	49
121	150 CONTINUE	REAP	50
121	READ(10,20) (A(I),I=1,N)	REAP	51

131		PRINT 40*(A(I),I=1*N)	LEAP	52
143		RETURN	LEAP	53
144		END	LEAP	54
	C	*****	DUMMY	2
	C	7. DUMMIES	DUMMY	3
	C	*****	DUMMY	4
		SUBROUTINE DOUT	DUMMY	5
	C	THIS IS A DUMMY ROUTINE.	DUMMY	6
1		RETURN	DUMMY	7
2		END	DUMMY	8
		SUBROUTINE DIPI	DUMMY	9
	C	THIS IS A DUMMY ROUTINE.	DUMMY	10
1		RETURN	DUMMY	11
2		END	DUMMY	12
		SUBROUTINE TEST	DUMMY	13
	C	THIS IS A DUMMY ROUTINE.	DUMMY	14
1		RETURN	DUMMY	15
2		END	DUMMY	16
		SUBROUTINE CHEC	DUMMY	17
	C	THIS IS A DUMMY ROUTINE.	DUMMY	18
1		RETURN	DUMMY	19
2		END	DUMMY	20
		SUBROUTINE SPEC	DUMMY	21
	C	THIS IS A DUMMY ROUTINE.	DUMMY	22
1		RETURN	DUMMY	23
2		END	DUMMY	24
		SUBROUTINE SPEC1	DUMMY	25
	C	THIS IS A DUMMY ROUTINE.	DUMMY	26
1		RETURN	DUMMY	27
2		END	DUMMY	28
		SUBROUTINE CORE	DUMMY	29
	C	THIS IS A DUMMY ROUTINE.	DUMMY	30
1		RETURN	DUMMY	31
2		END	DUMMY	32
		SUBROUTINE DOM	DUMMY	33
	C	THIS IS A DUMMY ROUTINE.	DUMMY	34
1		RETURN	DUMMY	35
2		END	DUMMY	36
	C	CZZ	CZZ	2

APPENDIX D

COMMON STORE

The contents of the common arrays are listed in Table D-I.

•General Notes

- (1) If there is a principal routine dealing with an array, its name is given in parentheses at the end of the description line.
- (2) A few important equivalent names are given; these are denoted by a preceding equals sign.
- (3) A single subscript indicates a one-dimensional array (for example x_i); a double subscript indicates a two-dimensional array.
- (4) One-dimensional arrays containing species properties or compositions for the entire system list the solid as the first species. The mole fraction of the solid is $x_s = n_s/n$.
- (5) Unless otherwise stated, the units are cm-g- μ s or cm-mol- μ s.
- (6) Unless otherwise stated, all derivatives for the system are at chemical equilibrium.

•Particular Notes

- (1) GM - the prime here denotes imperfection quantities with respect to ideal gas at the same temperature and volume. See Sec. IV.C.
- (2) THER - the subscript o on quantities near the end of the array denotes a frozen-composition derivative.

TABLE D-I
COMMON STORE

CAR - matrix of FROOT arrays (columns)	DER - differentiation (GAMM)
1. CC - CJ	1. p
2. CH - Hugoniot	2. v
3. CM - constant-v, s, e contours	3. T
4. CG - gas EOS	4. v_+
5. CS - solid EOS	5. v_-
	6. H_+
	7. H_-
CONT - constants	
1. 1.98719 R(cal)	EMG - \tilde{F}_i , "free energies" for equilibrium constants (EQMS)
2. 831439×10^{-5} R(Mbar-cm ³ /g)	
3. 1.01325×10^{-6} atm to Mbar	
4. 0.04184 kcal to Mbar-cm ³	
5. $0.426012 (N/\sqrt{2}) \times 10^{-24}$	

EMN - phase mole numbers

1. n_g
2. n_s
3. $n = n_g + n_s$
4. $x_g = n_g/n$
5. $x_s = n_s/n$
6. n/M_0 (moles/gram)
7. $\ln \hat{s}$ (saturation index) or $-n_s$
(all solid evaporated)

EMX - x_i , mole fractions

FMU - μ_i' , imperfection chemical potentials

FN - n_i , mole numbers

FOB - knobs

- 1-6. FROOT ϵ 's
- 7-12. FROOT r 's
13. $\Delta_1 = \Delta \ln p$ (GAMM)
14. $\Delta_2 = \Delta T$ (GAMM)
15. ϵ , equilibrium outer (EQP)
16. ϵ , equilibrium inner (EQP)
- 17,18. ---
- 19-36. FROOT x_{\min}, x_{\max} in pairs

GM - pure-fluid gas state (sub g) (GEM)

1. $\tau = v/v^*$
2. $\theta = T/T^*$
3. $z = pV/RT$
4. E'/RT
5. F'/RT
6. $(z\theta)_\theta$
7. τz_τ
8. C_v/R
9. $z - RT/p$
10. $z-1$
11. S'/R
12. $(\partial p/\partial V)_T$
13. $(\partial p/\partial T)_V$
14. $(\partial V/\partial T)_p$
15. V
16. p
17. H'/RT
18. $(z-1)_\theta = \tau \chi_\tau/\theta$
19. $(E'/RT)_\theta = -\chi/\theta$
20. A'/RT
21. $V_f/V = 2\pi\sqrt{2} g(1)$ (V_f = free volume)
22. $b/2$ (integration limit)
23. ---

24. ---

25. γ
26. $p^{-1} (\partial E/\partial V)_p$
27. $1/\Gamma$
28. $-(\partial \ln p/\partial \ln V)_T$
29. C_p/R
30. $(\partial \ln V/\partial T)_p$

GP - gas EOS (GEM)

1. n
2. m
3. A_n
4. A_m
5. $r^* = RSTA$
6. $T^* = TSTA$
7. $V^* = VSTA$

HE - initial (unreacted) state (CON)

1. ρ_0 (g/cm³)
2. p_0 (Mbar)
3. T_0 (K)
4. M_0 (g/mole)
5. ΔH_{f0} (kcal/mole relative to elements at T_0)
6. $v_0 = 1/\rho_0$
7. $h_0(T_0;T_0) = (n/M_0) \Delta H_{f0}$
8. $e_j = \frac{1}{2} u_j^2$

KAL - option switches, see CON, SWIT

1. equilibrium differentiation
2. fixed composition differentiation
3. gas (0/9/other: ideal/KW/LJD)
4. solid (0 for incompressible)
5. mix 0 no-mix 3 - CS
1 ideal 4 One-Fluid
2 LH
6. composition (0/1 for fixed, equilibrium)
7. CJ (0/1 for equilibrium/frozen)
8. contour (1, 2, 3, 4 for constant-T, v, s, e)
9. T_c, p_c choice (0/1 for input/previous)
10. $z - 1$
11. punch output if $\neq 0$

KEN - entry and iteration counts

KIM - sizes

1. r = KR number of gas species
2. s = KS total number of species
3. c = KC number of elements
4. n = KN degree of ideal-function fit

KON - triggers and diagnostic switches

PT - input pressure table (PV, TED)

ROT - input ρ_0 table (CJ)

SM - solid state (sub s) (SEMS)

1. V
2. E'/RT
3. H'/RT
4. A'/RT
5. F'/RT
6. S'/R
7. $z = pV/RT$
8. p
9. $V/V_0 = \gamma$
10. T
11. T_1

SP - solid EOS (SEMS)

1. Γ
2. C_p/R
3. α
4. V_0
5. T_0
6. E_0/RT_0
7. ---
- 8-12. c_0 - c_4 - Hugoniot fit
- 13-20. working store

SUC - contour initial state (PV)

1. T_c
2. p_c
3. V_c
4. S_c
5. E_c

SUCG - derivatives working store (GAMM)

1. $\gamma-1$
2. $p^{-1} (\partial e / \partial v)_p$
3. $1/\Gamma$
4. c
5. CJ function $j(p)$ [see THER (28)]
6. $-(\partial \ln p / \partial \ln v)_T$

7. C_p/R
8. $(\partial \ln v / \partial \ln T)_p$

THER - system state (COUT)

1. p
 2. v/v_0
 3. T
 4. u
 5. D
 6. q (Mbar - cm^3/g)
 7. q (kcal/g)
 8. v
 9. e
 10. h
 11. a
 12. f
 13. s
 14. $H(T;T_0)/RT$ - relative to elements at T_0
 15. V
 16. E/RT
 17. H/RT
 18. A/RT
 19. F/RT
 20. S/R
 21. $z = pV/RT$
 22. γ
 23. $p^{-1} (\partial e / \partial v)_p$
 24. $1/\Gamma$
 25. c
 26. γ_0 (frozen)
 27. $j(p)$ equilibrium
 28. $j(p)$ frozen
- where $j(p)$ is the CJ function:

$$j(p) = \left\{ v/v_0 \left[(\gamma+1 - p_0/p)/\gamma \right] \right\}^{-\gamma}$$

29. c_0 (frozen)
30. $p^{-1} (\partial e / \partial v)_p$ frozen

TMG - F_i^i - ideal free energies

TMS - ideal functions (super i) (TIMS)

1. E_g/RT
 2. H_g/RT
 3. C_g/R
 4. S_g/R
 5. $\Delta_g(T_0)$
 6. $H_g(T;T_0)/RT$
 7. H_s/RT
 8. C_s/R
 9. S_s/R
 10. F_s/RT
 11. $\Delta_s(T_0)$
 12. $H_s(T;T_0)/RT$
- } relative to
} elements at T_0

TP - CON, TIP strings 3 ..., one row
per species

XMT - gas mixture state (sub g) (XIM)

1. V
2. E'/RT
3. H'/RT
4. A'/RT
5. F'/RT
6. S'/R
7. $z-1$
8. $V-RT/p$
9. $\sum x_i x_j T_{ij}^*/T_r^*$ (for LH mix)
10. $\sum x_i x_j r_{ij}^*/r_r^*$ (for LH mix)
11. r_r^* (for LH mix)
12. T_r^* (for LH mix)
13. n (for One-Fluid mix)
14. m (for One-Fluid mix)
15. V_c^* (for One-Fluid mix)
16. $\bar{r}^* = RSTAT$ (from XIMS)
17. $\bar{T}^* = TSTAT$ (from XIMS)
18. $\bar{V}^* = VSTAT$ (from XIMS)

XMU μ_i'/RT , gas species only (XIM)

XPF - T_{ij}^* (XIM)

XPG - r_{ij}^* (XIM)

XPR - r_i^* (XIM)

XPT - T_i^* (XIM)

REFERENCES

1. W. Fickett, "Calculation of the Detonation Properties of Condensed Explosives," Phys. Fluids 6, 997-1006 (1963).
2. W. Fickett, "Detonation Properties of Condensed Explosives Calculated with an Equation of State Based on Intermolecular Potentials," Los Alamos Scientific Laboratory report LA-2712 (December 1962).
3. S. J. Jacobs, "Energy of Detonation," Naval Ordnance Laboratory report NAVORD 4366 (September 1956).